Guide to Best Practices for Ocean CO_2 Measurements

PICES SPECIAL PUBLICATION 3
IOCCP REPORT No. 8

PICES

Scientific Committee on Oceanic Research

CDIAC

Chapter 1

Introduction to the Guide

The collection of extensive, reliable, oceanic carbon data was a key component of the Joint Global Ocean Flux Study (JGOFS) and World Ocean Circulation Experiment (WOCE) and continues to be a cornerstone of the global climate research effort. This Guide was originally prepared at the request, and with the active participation, of a science team formed by the U.S. Department of Energy (DOE) to carry out the first global survey of carbon dioxide in the oceans (DOE. 1994. Handbook of methods for the analysis of the various parameters of the carbon dioxide system in sea water; version 2, A.G. Dickson and C. Goyet, Eds. ORNL/CDIAC-74). The manual has been updated several times since, and the current version contains the most up-to-date information available on the chemistry of CO_2 in sea water and the methodology of determining carbon system parameters. This revision has been made possible by the generous support of the North Pacific Marine Science Organization (PICES), the Scientific Committee on Ocean Research (SCOR), the Intergovernmental Oceanographic Committee (IOC) and DOE through the Carbon Dioxide Information and Analysis Center (CDIAC). The editors are extremely grateful to Alex Kozyr and Mikhail Krassovski at CDIAC for their hard work in helping us to complete this revised volume. This manual should be cited as Dickson, A.G., Sabine, C.L. and Christian, J.R. (Eds.) 2007. Guide to best practices for ocean CO_2 measurements. PICES Special Publication 3, 191 pp.

The procedures detailed in the following pages have been subjected to open review by the ocean carbon science community and describe well-tested methods. They are intended to provide standard operating procedures (SOPs), together with an appropriate quality control plan. These are not the only measurement techniques in use for the parameters of the oceanic carbon system; however, they do represent the current state-of-the-art for shipboard measurements. In the end, we hope that this manual can serve as a clear and unambiguous guide to other investigators who are setting up to analyze the various parameters of the carbon dioxide system in sea water. We envision it as an evolving document, updated where necessary. The editors welcome comments and suggestions for use in preparing future revisions. The procedures included here are not simply descriptions of a particular method in current use in a single

laboratory, but rather provide standard operating procedures which have been written in a fashion that will—we trust—allow anyone to implement the method successfully. In some cases there is no consensus about the best approach; these areas are identified in the footnotes to the various procedures along with other hints and tips.

In addition to the written procedures, general information about the solution chemistry of the carbon dioxide system in sea water has been provided (Chapter 2) together with recommended values for the physical and thermodynamic data needed for certain computations (Chapter 5). This information is needed to understand certain aspects of the procedures, and users of this Guide are advised to study Chapter 2 carefully. The user is cautioned that equilibrium constants employed in ocean carbon chemistry have specific values for different pH scales, and values in the published literature may be on different scales than the one used here; it is very important to make sure that all constants used in a particular calculation are on the same scale. General advice about appropriate quality control measures has also been included (Chapter 3). The SOPs (Chapter 4) are numbered. Numbers less than 10 are reserved for procedures describing sampling and analysis, numbers 11–20 for procedures for calibration, *etc.*, and numbers 21 and upward for procedures for computations and quality control. This scheme allows for the addition of further SOPs in the future. Each of the procedures has been marked with a date of last revision and a version number. When citing a particular SOP in a report or technical paper, we recommend stating the version number of the procedure used. We envision this Guide being further expanded and updated in the future; thus the version number identifies unambiguously the exact procedure that is being referred to. Any errors in the text or corrections that arise as the methods evolve can be reported to Alex Kozyr at CDIAC (kozyra@ornl.gov).

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Editors

Chapter 2

Solution chemistry of carbon dioxide in sea water

1. Introduction

This chapter outlines the chemistry of carbon dioxide in sea water so as to provide a coherent background for the rest of this Guide. The following sections lay out the thermodynamic framework required for an understanding of the solution chemistry; the thermodynamic data needed to interpret field and laboratory results are presented in Chapter 5.

2. Reactions in solution

The reactions that take place when carbon dioxide dissolves in water can be represented by the following series of equilibria:

$$CO_2(g) \rightleftharpoons CO_2(aq), \tag{1}$$

$$CO_2(aq) + H_2O(l) \rightleftharpoons H_2CO_3(aq), \tag{2}$$

$$H_2CO_3(aq) \rightleftharpoons H^+(aq) + HCO_3^-(aq), \tag{3}$$

$$HCO_3^-(aq) \rightleftharpoons H^+(aq) + CO_3^{2-}(aq); \tag{4}$$

the notations (g), (l), (aq) refer to the state of the species, *i.e.*, a gas, a liquid or in aqueous solution respectively. It is difficult to analytically distinguish between the species CO_2(aq) and H_2CO_3(aq). It is usual to combine the concentrations of CO_2(aq) and H_2CO_3(aq) and to express this sum as the concentration of a hypothetical species, $CO_2^*(aq)$.

Redefining (1), (2), and (3) in terms of this species gives

$$CO_2(g) \rightleftharpoons CO_2^*(aq) \tag{5}$$

$$CO_2^*(aq) + H_2O(l) \rightleftharpoons H^+(aq) + HCO_3^-(aq) \tag{6}$$

The equilibrium relationships between the concentrations of these various species can then be written as

$$K_0 = [\mathrm{CO_2^*}] / f(\mathrm{CO_2}), \tag{7}$$

$$K_1 = [\mathrm{H^+}][\mathrm{HCO_3^-}] / [\mathrm{CO_2^*}], \tag{8}$$

$$K_2 = [\mathrm{H^+}][\mathrm{CO_3^{2-}}] / [\mathrm{HCO_3^-}]. \tag{9}$$

In these equations, $f(\mathrm{CO_2})$ is the fugacity of carbon dioxide in the gas phase and brackets represent total stoichiometric concentrations[1] of the particular chemical species enclosed. These equilibrium constants are functions of the temperature, pressure and salinity of the solution (*e.g.*, sea water) and have been measured in a variety of studies (see Chapter 5).

3. Fugacity

The fugacity of carbon dioxide is not the same as its partial pressure—the product of mole fraction and total pressure, $x(\mathrm{CO_2})\cdot p$—but rather takes account of the non-ideal nature of the gas phase. The fugacity of a gas such as CO_2 can be determined from knowledge of its equation of state:

$$f(\mathrm{CO_2}) = x(\mathrm{CO_2})\cdot p \cdot \exp\left(\frac{1}{RT} \int_0^p \left(V(\mathrm{CO_2}) - RT/p' \right) dp' \right). \tag{10}$$

The equation of state of a real gas such as CO_2, either alone or in a mixture, can be represented by a virial expression:

$$\frac{p\,V(\mathrm{CO_2})}{RT} = 1 + \frac{B(x,T)}{V(\mathrm{CO_2})} + \frac{C(x,T)}{V(\mathrm{CO_2})^2} + \ldots \tag{11}$$

This equation, truncated after the second term, is usually adequate to represent *p*–*V*–*T* properties at pressures up to a few atmospheres (Dymond and Smith, 1980).

It is known from statistical mechanics that the virial coefficients $B(x, T)$, $C(x, T)$, *etc*. relate to pair-wise interactions in the gas phase (Guggenheim, 1967). This property can be used to estimate $B(x, T)$ for particular gas mixtures, such as CO_2 in air, from measurements on binary mixtures or from a model of the intermolecular potential energy function for the molecules concerned. The magnitude of the fugacity coefficient (the ratio of fugacity to partial pressure) is a function both of temperature and of gas phase composition (Fig. 1).

[1] Strictly, equations (7) to (9) should be expressed in terms of activities rather than concentrations. However, as the activity coefficients are approximately constant for small amounts of reacting species in a background medium, these expressions are valid and correspond to "ionic medium" equilibrium constants based on a sea water medium.

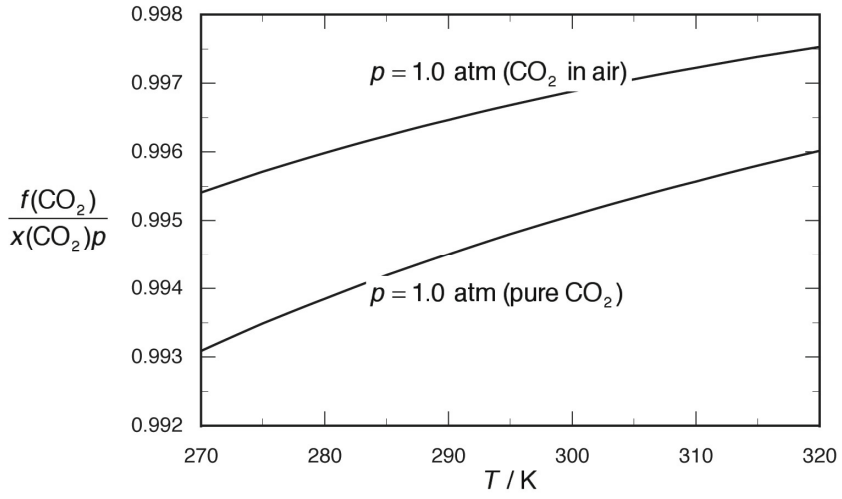

Fig. 1 Variation of the fugacity coefficient with temperature at 1 atm total pressure for pure CO_2 gas and for CO_2 in air: $x(CO_2) = 350 \times 10^{-6}$ (calculated using the procedure described in SOP 24 of this Guide).

4. Analytical parameters of the CO_2 system

Unfortunately, the concentrations of the individual species of the carbon dioxide system in solution can not be measured directly. There are, however, four parameters that can be measured. These are used together with ancillary information to obtain a complete description of the carbon dioxide system in sea water. Methods for determining each of these parameters are detailed in Chapter 4.

4.1 Total dissolved inorganic carbon

The total dissolved inorganic carbon in a sea water sample:

$$C_T = [CO_2^*] + [HCO_3^-] + [CO_3^{2-}] \tag{12}$$

can be measured directly by acidifying the sample, extracting the CO_2 gas that is produced and measuring its amount.

4.2 Total alkalinity

The total alkalinity of a sample of sea water is a form of mass-conservation relationship for hydrogen ion. It is rigorously defined (Dickson, 1981) as ". . . the number of moles of hydrogen ion equivalent to the excess of proton acceptors (bases formed from weak acids with a dissociation constant $K \leq 10^{-4.5}$ at 25°C and zero ionic strength) over proton donors (acids with $K > 10^{-4.5}$) in 1 kilogram of sample." Thus

$$\begin{aligned} A_T = {} & [HCO_3^-] + 2[CO_3^{2-}] + [B(OH)_4^-] + [OH^-] + [HPO_4^{2-}] \\ & + 2[PO_4^{3-}] + [SiO(OH)_3^-] + [NH_3] + [HS^-] + ... \\ & - [H^+]_F - [HSO_4^-] - [HF] - [H_3PO_4] - ... \end{aligned} \tag{13}$$

where the ellipses stand for additional minor acid or base species that are either unidentified or present in such small amounts that they can be safely neglected. $[H^+]_F$ is the *free* concentration of hydrogen ion—see equation (15).

4.3 Fugacity of CO_2 in equilibrium with a sea water sample

This measurement typically requires a gas phase that is in equilibrium with a sea water sample at a known pressure and temperature. The concentration of CO_2 is then determined in the gas phase and the corresponding value of $f(CO_2)$—for that temperature—estimated from equation (10).

4.4 Total hydrogen ion concentration

The hydrogen ion concentration in sea water is usually reported as pH:

$$\mathrm{pH} = -\log[H^+]. \tag{14}$$

Although the concept of a total hydrogen ion concentration is somewhat confusing[2], it is needed to define acid dissociation constants accurately in sea water (Dickson, 1990). Total hydrogen ion concentration is defined as

$$[H^+] = [H^+]_F \cdot (1 + S_T / K_S). \tag{15}$$

$[H^+]_F$ is the *free* hydrogen ion concentration, S_T is the total sulfate concentration ($[SO_4^{2-}] + [HSO_4^-]$) and K_S is the acid dissociation constant for HSO_4^-. At pH values above 4, equation (15) can be approximated as

$$[H^+] = [H^+]_F + [HSO_4^-]. \tag{16}$$

The various equilibrium constants required to describe acid–base chemistry in sea water have been measured in the laboratory (see Chapter 5 for recommended constants). In addition to knowing the carbon parameters, the total concentrations of the various other (non-CO_2) acid–base systems in the sample of interest are needed to fully constrain the carbon dioxide system in sea water. The total concentrations of conservative constituents, such as borate, sulfate, and fluoride, can be estimated from salinity. Those of non-conservative constituents, such as phosphate, silicate, ammonia or hydrogen sulfide, must be measured but approximate "reference" concentrations are adequate for most purposes. Because of the relative consistency of the chemical constituents of sea water, it is generally accepted that only two of the four measurable carbon parameters are needed together with the equilibrium constants, temperature, pressure, and salinity, to have a complete description of the system (see Park (1969), Skirrow (1975), and the Annexe to this chapter).

This practice assumes that our present knowledge of the nature, total concentrations, and thermodynamic properties of all the possible acid–base species in sea water is complete. It is probably better at this stage to over-determine the system whenever possible, *i.e.*, to measure more than two of these parameters on any given sample and to use the redundancy to confirm that the measurements fit with our understanding of the thermodynamics of acid–base processes in sea water.

[2] See Dickson (1984, 1993) for a detailed discussion of the various pH scales that have been used in sea water.

5. Bibliography

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Annexe

Equations that describe the CO_2 system in sea water

It is possible, in theory, to obtain a *complete* description of the carbon dioxide system in a sample of sea water at a particular temperature and pressure provided that the following information is known[3]:

- the solubility constant for CO_2 in sea water, K_0,
- the equilibrium constants for each of the acid–base pairs that are assumed to exist in the solution,
- the total concentrations of all the non-CO_2 acid–base pairs,
- the values of at least two of the CO_2 related parameters: C_T, A_T, $f(CO_2)$, $[H^+]$.

The optimal choice of experimental variables is dictated by the nature of the problem being studied and remains at the discretion of the investigator. Although each of the CO_2 related parameters is linearly independent, they are not orthogonal. For certain combinations there are limits to the accuracy with which the other parameters can be predicted from the measured data. These errors end up being propagated through the equations presented here. Such errors result from all the experimentally derived information, including the various equilibrium constants. As a consequence it is usually better to *measure* a particular parameter directly using one of the methods detailed in Chapter 4 than to calculate it from other measurements.

When more than two of the CO_2-related parameters have been measured on a single sea water sample, it is possible to use the various possible pairs of parameters to compute the other redundant parameters and thus to assess the internal consistency of our knowledge of the system. Again, it is necessary to take all the sources of error into account when doing this. Alternately, one can describe the system independently of one or more of the dissociation constants for carbonic acid. Equations that allow each of these possibilities to be realized are derived here.

[3] The rank of the system of equilibrium equations that describes the acid–base chemistry of sea water—*i.e.*, the number of linearly independent variables—is equal to the number of independent mass-conservation relationships plus the number of acid–base pairs considered (the number of dissociation constants).

Table 1 Equations for the sea water acid–base system.

Mass-conservation equations[4]

$$C_T = [CO_2^*] + [HCO_3^-] + [CO_3^{2-}] \quad (17)$$

$$A_T = [HCO_3^-] + 2[CO_3^{2-}] + [B(OH)_4^-] + [OH^-] + [HPO_4^{2-}] + 2[PO_4^{3-}] + [SiO(OH)_3^-] + [NH_3] + [HS^-] + ... - [H^+]_F - [HSO_4^-] - [HF] - [H_3PO_4] - ... \quad (18)$$

$$B_T = [B(OH)_3] + [B(OH)_4^-] \quad (19)$$

$$S_T = [HSO_4^-] + [SO_4^{2-}] \quad (20)$$

$$F_T = [HF] + [F^-] \quad (21)$$

$$P_T = [H_3PO_4] + [H_2PO_4^-] + [HPO_4^{2-}] + [PO_4^{3-}] \quad (22)$$

$$Si_T = [Si(OH)_4] + [SiO(OH)_3^-] \quad (23)$$

$$NH_{3T} = [NH_4^+] + [NH_3] \quad (24)$$

$$H_2S_T = [H_2S] + [HS^-] \quad (25)$$

Equilibrium constants

$$K_0 = [CO_2^*] / f(CO_2) \quad (26)$$

$$K_1 = [H^+][HCO_3^-] / [CO_2^*] \quad (27)$$

$$K_2 = [H^+][CO_3^{2-}] / [HCO_3^-] \quad (28)$$

$$K_B = [H^+][B(OH)_4^-] / [B(OH)_3] \quad (29)$$

$$K_W = [H^+][OH^-] \quad (30)$$

$$K_S = [H^+][SO_4^{2-}] / [HSO_4^-] \quad (31)$$

$$K_F = [H^+][F^-] / [HF] \quad (32)$$

$$K_{1P} = [H^+][H_2PO_4^-] / [H_3PO_4] \quad (33)$$

$$K_{2P} = [H^+][HPO_4^{2-}] / [H_2PO_4^-] \quad (34)$$

$$K_{3P} = [H^+][PO_4^{3-}] / [HPO_4^{2-}] \quad (35)$$

$$K_{Si} = [H^+][SiO(OH)_3^-] / [Si(OH)_4] \quad (36)$$

$$K_{NH_3} = [H^+][NH_3] / [NH_4^+] \quad (37)$$

$$K_{H_2S} = [H^+][HS^-] / [H_2S] \quad (38)$$

[4] The aqueous chemistry of Si is rather complex, and encompasses more species than are considered here. This approximation is adequate for the present purpose of estimating the silicate contribution to alkalinity.

Table 2 Expressions for the concentrations of the various species in equation (18).

$$[\mathrm{HCO_3^-}] = \frac{C_\mathrm{T} K_1 [\mathrm{H^+}]}{[\mathrm{H^+}]^2 + K_1[\mathrm{H^+}] + K_1 K_2} \tag{39}$$

$$[\mathrm{CO_3^{2-}}] = \frac{C_\mathrm{T} K_1 K_2}{[\mathrm{H^+}]^2 + K_1[\mathrm{H^+}] + K_1 K_2} \tag{40}$$

$$[\mathrm{B(OH)_4^-}] = B_\mathrm{T} / (1 + [\mathrm{H^+}]/K_\mathrm{B}) \tag{41}$$

$$[\mathrm{OH^-}] = K_\mathrm{W} / [\mathrm{H^+}] \tag{42}$$

$$[\mathrm{H_3PO_4}] = \frac{P_\mathrm{T} [\mathrm{H^+}]^3}{[\mathrm{H^+}]^3 + K_{1\mathrm{P}}[\mathrm{H^+}]^2 + K_{1\mathrm{P}}K_{2\mathrm{P}}[\mathrm{H^+}] + K_{1\mathrm{P}}K_{2\mathrm{P}}K_{3\mathrm{P}}} \tag{43}$$

$$[\mathrm{H_2PO_4^-}] = \frac{P_\mathrm{T} K_{1\mathrm{P}} [\mathrm{H^+}]^2}{[\mathrm{H^+}]^3 + K_{1\mathrm{P}}[\mathrm{H^+}]^2 + K_{1\mathrm{P}}K_{2\mathrm{P}}[\mathrm{H^+}] + K_{1\mathrm{P}}K_{2\mathrm{P}}K_{3\mathrm{P}}} \tag{44}$$

$$[\mathrm{HPO_4^{2-}}] = \frac{P_\mathrm{T} K_{1\mathrm{P}} K_{2\mathrm{P}} [\mathrm{H^+}]}{[\mathrm{H^+}]^3 + K_{1\mathrm{P}}[\mathrm{H^+}]^2 + K_{1\mathrm{P}}K_{2\mathrm{P}}[\mathrm{H^+}] + K_{1\mathrm{P}}K_{2\mathrm{P}}K_{3\mathrm{P}}} \tag{45}$$

$$[\mathrm{PO_4^{3-}}] = \frac{P_\mathrm{T} K_{1\mathrm{P}} K_{2\mathrm{P}} K_{3\mathrm{P}}}{[\mathrm{H^+}]^3 + K_{1\mathrm{P}}[\mathrm{H^+}]^2 + K_{1\mathrm{P}}K_{2\mathrm{P}}[\mathrm{H^+}] + K_{1\mathrm{P}}K_{2\mathrm{P}}K_{3\mathrm{P}}} \tag{46}$$

$$[\mathrm{SiO(OH)_3^-}] = Si_\mathrm{T} / (1 + [\mathrm{H^+}]/K_\mathrm{Si}) \tag{47}$$

$$[\mathrm{NH_3}] = NH_{3\mathrm{T}} / (1 + [\mathrm{H^+}]/K_{\mathrm{NH_3}}) \tag{48}$$

$$[\mathrm{HS^-}] = H_2S_\mathrm{T} / (1 + [\mathrm{H^+}]/K_{\mathrm{H_2S}}) \tag{49}$$

$$[\mathrm{H^+}]_\mathrm{F} = [\mathrm{H^+}] / (1 + S_\mathrm{T}/K_\mathrm{S}) \tag{50}$$

$$[\mathrm{HSO_4^-}] = S_\mathrm{T} / (1 + K_\mathrm{S}/[\mathrm{H^+}]_\mathrm{F}) \tag{51}$$

$$[\mathrm{HF}] = F_\mathrm{T} / (1 + K_\mathrm{F}/[\mathrm{H^+}]) \tag{52}$$

$[H^+]$ and A_T

The carbonate alkalinity (*i.e.*, the contribution of carbonate species to the total alkalinity) is defined as

$$A_\mathrm{C} = [\mathrm{HCO_3^-}] + 2[\mathrm{CO_3^{2-}}] . \tag{53}$$

The concentrations of the non-CO_2 species that contribute to A_T are calculated using the expressions given in Table 2, thus

$$\begin{aligned} A_\mathrm{C} = A_\mathrm{T} - \big(& [\mathrm{B(OH)_4^-}] + [\mathrm{OH^-}] + [\mathrm{HPO_4^{2-}}] + 2[\mathrm{PO_4^{3-}}] \\ & + [\mathrm{SiO(OH)_3^-}] + [\mathrm{NH_3}] + [\mathrm{HS^-}] + \ldots \\ & - [\mathrm{H^+}]_\mathrm{F} - [\mathrm{HSO_4^-}] - [\mathrm{HF}] - [\mathrm{H_3PO_4}] - \ldots \big) \end{aligned} \tag{54}$$

Then from (27),

$$[\mathrm{HCO_3^-}] = \frac{[\mathrm{CO_2^*}]K_1}{[\mathrm{H^+}]}, \tag{55}$$

and from (28),

$$[\mathrm{CO_3^{2-}}] = \left(\frac{[\mathrm{CO_2^*}]K_1}{[\mathrm{H^+}]}\right)\frac{K_2}{[\mathrm{H^+}]}. \tag{56}$$

Substituting into (53) and rearranging,

$$[\mathrm{CO_2^*}] = \frac{A_\mathrm{C}[\mathrm{H^+}]^2}{K_1([\mathrm{H^+}] + 2K_2)}, \tag{57}$$

and hence

$$[\mathrm{HCO_3^-}] = \frac{A_\mathrm{C}[\mathrm{H^+}]}{[\mathrm{H^+}] + 2K_2}, \tag{58}$$

$$[\mathrm{CO_3^{2-}}] = \frac{A_\mathrm{C}K_2}{[\mathrm{H^+}] + 2K_2}. \tag{59}$$

C_T is calculated from (17) and $f(\mathrm{CO_2})$ from (26):

$$f(\mathrm{CO_2}) = \frac{[\mathrm{CO_2^*}]}{K_0}. \tag{60}$$

$[H^+]$ and $f(CO_2)$

$[\mathrm{CO_2^*}]$ is given by (26):

$$[\mathrm{CO_2^*}] = K_0 f(\mathrm{CO_2}). \tag{61}$$

Thus, from (27) and (28),

$$[\mathrm{HCO_3^-}] = \frac{K_0K_1f(\mathrm{CO_2})}{[\mathrm{H^+}]}, \tag{62}$$

$$[\mathrm{CO_3^{2-}}] = \frac{K_0K_1K_2f(\mathrm{CO_2})}{[\mathrm{H^+}]^2}. \tag{63}$$

C_T is calculated from (17) and A_T from (18); $[\mathrm{HCO_3^-}]$ and $[\mathrm{CO_3^{2-}}]$ are given by (62) and (63), the remaining terms are calculated from the expressions given in Table 2.

$[H^+]$ and C_T

Equations (27) and (28) are rearranged and substituted into (17) to give

$$C_\mathrm{T} = [\mathrm{CO_2^*}]\left(1 + \frac{K_1}{[\mathrm{H^+}]} + \frac{K_1K_2}{[\mathrm{H^+}]^2}\right). \tag{64}$$

Thus

$$[CO_2^*] = \frac{C_T[H^+]^2}{[H^+]^2 + K_1[H^+] + K_1K_2}, \quad (65)$$

$$[HCO_3^-] = \frac{C_T K_1[H^+]}{[H^+]^2 + K_1[H^+] + K_1K_2}, \quad (66)$$

$$[CO_3^{2-}] = \frac{C_T K_1K_2}{[H^+]^2 + K_1[H^+] + K_1K_2}. \quad (67)$$

$f(CO_2)$ is calculated from (60) and A_T from (18); the various terms needed are calculated from the expressions given in Table 2.

A_T and C_T

The easiest approach to using this pair of parameters is to rewrite (18), the expression for A_T, in terms of total concentrations and $[H^+]$ (see Table 2). The resulting equation is solved for $[H^+]$ using either a Newton–Raphson technique or a simple iterative approach; a suitable initial estimate for calculations involving sea water is: $[H^+] = 10^{-8}$ mol kg^{-1}.

Once $[H^+]$ has been calculated,

$$[HCO_3^-] = \frac{C_T K_1[H^+]}{[H^+]^2 + K_1[H^+] + K_1K_2}, \quad (68)$$

$$[CO_3^{2-}] = \frac{C_T K_1K_2}{[H^+]^2 + K_1[H^+] + K_1K_2}. \quad (69)$$

$[CO_2^*]$ is then calculated from

$$[CO_2^*] = \frac{[H^+][HCO_3^-]}{K_1} \quad (70)$$

and $f(CO_2)$ is calculated from (60).

A_T and $f(CO_2)$

$[CO_2^*]$ is given by (26):

$$[CO_2^*] = K_0 f(CO_2). \quad (71)$$

Equations (27) and (28) are then rewritten as

$$[HCO_3^-] = \frac{K_0K_1 f(CO_2)}{[H^+]}, \quad (72)$$

$$[CO_3^{2-}] = \frac{K_0K_1K_2 f(CO_2)}{[H^+]^2}. \quad (73)$$

These terms are substituted into (18) together with the remaining terms from Table 2. The resulting expression is solved for $[H^+]$ using either a Newton–Raphson technique or a simple iterative approach; a suitable initial estimate for ocean water is: $[H^+] = 10^{-8}$ mol kg^{-1}. Once $[H^+]$ has been calculated, C_T is calculated from (17) using the final values obtained for $[HCO_3^-]$ and $[CO_3^{2-}]$.

C_T and $f(CO_2)$

For this calculation, it is convenient to define the constant

$$K = K_1/K_2 = \frac{[HCO_3^-]^2}{[CO_2^*][CO_3^{2-}]}. \tag{74}$$

For the equilibrium process,

$$CO_2^*(aq) + CO_3^{2-}(aq) + H_2O(l) = 2\,HCO_3^-. \tag{75}$$

$[CO_2^*]$ is given by (26):

$$[CO_2^*] = K_0 f(CO_2) \tag{76}$$

and combining (17) and (74) gives

$$C_T = K_0 f(CO_2) + [HCO_3^-] + \frac{[HCO_3^-]^2}{K K_0 f(CO_2)}. \tag{77}$$

Rearranging,

$$\begin{aligned}[HCO_3^-]^2 + K K_0 f(CO_2)[HCO_3^-] \\ + K K_0 f(CO_2)\left(K_0 f(CO_2) - C_T\right) = 0.\end{aligned} \tag{78}$$

The solution is

$$\begin{aligned}[HCO_3^-] = \frac{1}{2}\Big[-K K_0 f(CO_2) + \Big(\left(K K_0 f(CO_2)\right)^2 \\ - 4\left(K K_0 f(CO_2)\right)\left(K_0 f(CO_2) - C_T\right)\Big)^{1/2}\Big]\end{aligned} \tag{79}$$

and

$$[CO_3^{2-}] = C_T - [CO_2^*] - [HCO_3^-]. \tag{80}$$

$[H^+]$ is calculated from (27):

$$[H^+] = \frac{K_1[CO_2^*]}{[HCO_3^-]}; \tag{81}$$

A_T from (18): the various terms needed are calculated from the expressions given in Table 2.

$[H^+]$, A_T and C_T

The concentrations of the non-CO_2 species that contribute to A_T are calculated using the expressions given in Table 2. The carbonate alkalinity, A_C, is then calculated from (54). Equations (17), (27), and (53) can then be combined to give

$$2C_T - A_C = [CO_2^*]\left(2 + \frac{K_1}{[H^+]}\right). \tag{82}$$

Hence

$$[CO_2^*] = \frac{[H^+](2C_T - A_C)}{2[H^+] + K_1}, \tag{83}$$

$$[HCO_3^-] = \frac{K_1(2C_T - A_C)}{2[H^+] + K_1}, \tag{84}$$

$$\begin{aligned}[CO_3^{2-}] &= A_C - C_T + [CO_2^*] \\ &= \frac{[H^+]A_C + K_1(A_C - C_T)}{2[H^+] + K_1}.\end{aligned} \tag{85}$$

An expression for $[CO_2^*]$ can also be derived in terms of K_2:

$$[CO_2^*] = C_T - [HCO_3^-] - [CO_3^{2-}] \tag{86}$$

and $[HCO_3^-]$ and $[CO_3^{2-}]$ are given by (58) and (59), thus

$$[CO_2^*] = C_T - \frac{A_C([H^+] + K_2)}{[H^+] + 2K_2}. \tag{87}$$

$f(CO_2)$ is then calculated from (60).

$[H^+]$, A_T and $f(CO_2)$

The concentrations of the contributions of the various non-CO_2 species to A_T are calculated using the expressions given in Table 2. A_C is calculated from (54). Then, from (26),

$$[CO_2^*] = K_0 f(CO_2) \tag{88}$$

and from (27),

$$[HCO_3^-] = \frac{K_0 K_1 f(CO_2)}{[H^+]}, \tag{89}$$

Then, from (28) and (53),

$$[CO_3^{2-}] = \frac{A_C[H^+] - K_0 K_1 f(CO_2)}{2[H^+]}. \tag{90}$$

There are no equations that can be used to calculate these independently of K_1. C_T is calculated from (17).

$[H^+]$, C_T and $f(CO_2)$

From (26),

$$[CO_2^*] = K_0 f(CO_2)\,. \tag{91}$$

$[HCO_3^-]$ is given either by

$$[HCO_3^-] = \frac{K_0 K_1 f(CO_2)}{[H^+]}, \tag{92}$$

or can be obtained from (17) and (28):

$$\begin{aligned}[HCO_3^-] &= C_T - [CO_2^*] - \frac{[HCO_3^-]K_2}{[H^+]} \\ &= \frac{[H^+]\left(C_T - K_0 f(CO_2)\right)}{[H^+] + K_2}.\end{aligned} \tag{93}$$

$[CO_3^{2-}]$ can be obtained either from $[H^+]$ and $f(CO_2)$:

$$\begin{aligned}[CO_3^{2-}] &= C_T - [CO2^*] - [HCO_3^-] \\ &= C_T - K_0 f(CO_2)\left(1 + K_1/[H^+]\right)\end{aligned} \tag{94}$$

or from the equation for $[HCO_3^-]$ above, (93):

$$[CO_3^{2-}] = \frac{\left(C_T - K_0 f(CO_2)\right)K_2}{[H^+] + K_2}\,. \tag{95}$$

A_T is then calculated from (18), the terms for $[HCO_3^-]$ and $[CO_3^{2-}]$ are given by either (92) and (94), in terms of K_1, or (93) and (95), in terms of K_2. The remaining terms are calculated from the expressions given in Table 2.

$[H^+]$, A_T, C_T and $f(CO_2)$

The following sets of equations have the property that they do not embody directly either of the dissociation constants functions K_1 or K_2. The carbonate alkalinity, A_C, is first calculated from A_T and $[H^+]$ using (54) and the expressions in Table 2.

$[CO_2^*]$ is calculated from (26):

$$[CO_2^*] = K_0 f(CO_2) \tag{96}$$

and then

$$[HCO_3^-] = 2C_T - A_C - 2K_0 f(CO_2)\,, \tag{97}$$

$$[CO_3^{2-}] = A_C - C_T + K_0 f(CO_2)\,. \tag{98}$$

The dissociation constants for carbonic acid can then be calculated from (27) and (28).

Chapter 3

Quality assurance

1. Introduction

This chapter is intended to indicate some general principles of analytical quality assurance appropriate to the measurement of oceanic CO_2 parameters. Specific applications of analytical quality control are detailed as part of the individual standard operating procedures (Chapter 4).

Quality assurance constitutes the system by which an analytical laboratory can assure outside users that the analytical results they produce are of proven and known quality (Dux, 1990). In the past, the quality of most oceanic carbon data has depended on the skill and dedication of individual analysts. A formal quality assurance program is required for the development of a global ocean carbon data set, which depends on the consistency between measurements made by a variety of laboratories over an extended period of time[1]. Such a program was initiated during the World Ocean Circulation Experiment (WOCE) and Joint Global Ocean Flux Study (JGOFS) as described in the first (1994) edition of this manual. A quality assurance program consists of two separate related activities, quality control and quality assessment (Taylor, 1987):

Quality control — The overall system of activities whose purpose is to control the quality of a measurement so that it meets the needs of users. The aim is to ensure that data generated are of known accuracy to some stated, quantitative degree of probability, and thus provides quality that is satisfactory, dependable, and economic.

Quality assessment — The overall system of activities whose purpose is to provide assurance that quality control is being done effectively. It provides a continuing evaluation of the quality of the analyses and of the performance of the analytical system.

[1] An outline of how to go about establishing a formal quality assurance program for an analytical laboratory has been described by Dux (1990), additional useful information can be found in the book by Taylor (1987).

2. Quality control

The aim of quality control is to provide a stable measurement system whose properties can be treated statistically, *i.e.*, the measurement is "in control". Anything that can influence the measurement process must be optimized and stabilized to the extent necessary and possible if reproducible measurements are to be obtained. Measurement quality can be influenced by a variety of factors that are classified into three main categories (Taylor and Oppermann, 1986): management practices, personnel training and technical operations.

Although emphasis on quality by laboratory management, together with competence and training of individual analysts, is essential to the production of data of high quality (see Taylor and Oppermann, 1986; Taylor, 1987; Vijverberg and Cofino, 1987; Dux, 1990), these aspects are not discussed further here. The emphasis in this Guide is on documenting various standard procedures so that all technical operations are carried out in a reliable and consistent manner.

The first requirement of quality control is for the use of suitable and properly maintained equipment and facilities. These are complemented by the use of documented Good Laboratory Practices (GLPs), Good Measurement Practices (GMPs) and Standard Operating Procedures (SOPs).

GLPs refer to general practices that relate to many of the measurements in a laboratory such as maintenance of equipment and facilities, records, sample management and handling, reagent control and storage, and cleaning of laboratory glassware. GMPs are essentially technique specific. Both GLPs and GMPs should be developed and documented by each laboratory so as to identify critical operations that can cause variance or bias.

SOPs describe the way specific operations or analytical methods should be carried out. They comprise written instructions which define completely the procedure to be adopted by an analyst to obtain the required result. Well written SOPs include tolerances for all critical parameters that must be observed to obtain results of a specified accuracy. This Guide contains a number of such SOPs, many of which have been in use since the early 1990s, and have been revised with accumulated experience and improved technology.

3. Quality assessment

A key part of any quality assurance program is the statistical evaluation of the quality of the data output (see SOPs 22 and 23). There are both internal and external techniques for quality assessment (Table 1). Most of these are self evident; some are discussed in more detail below.

Table 1 Quality assessment techniques (after Taylor, 1987).

Internal techniques
Repetitive measurements
Internal test samples
Control charts
Interchange of operators
Interchange of equipment
Independent measurements
Measurements using a definitive method
Audits
External techniques
Collaborative tests
Exchange of samples
External reference materials
Certified reference materials
Audits

3.1 Internal techniques

Duplicate measurements of an appropriate number of samples provide an evaluation of precision that is needed while minimizing the level of pre-cruise preparation involved and eliminates all question of the appropriateness of the samples. At least 12 pairs distributed across the time and space scales of each measurement campaign (*i.e.*, each leg of a cruise) are needed to estimate a standard deviation with reasonable confidence. Ideally, if resources allow, one would like to collect and analyze duplicate samples from approximately 10% of the sample locations (*e.g.*, 3 sets of duplicates from a 36 position rosette). In cases where multiple instruments are used to increase sample throughput, replicate samples analyzed on each instrument provide useful cross-calibration documentation.

An internal test solution of reasonable stability can also be used to monitor precision (and bias, if the test solution value is known with sufficient accuracy). For example, the analysis of sub-samples from a large container of deep ocean water is frequently used to monitor the reproducibility of total alkalinity measurements. Historical data on a laboratory's own test solution can be used to develop a control chart and thus monitor and assess measurement precision[2].

[2] Considerable confusion exists between the terms *precision* and *accuracy*. Precision is a measure of how *reproducible* a particular experimental procedure is. It can refer either to a particular stage of the procedure, *e.g.*, the final analysis, or to the entire procedure including sampling and sample handling. It is estimated by performing replicate measurements and estimating a mean and standard deviation from the results obtained. Accuracy, however, is a measure of the degree of agreement of a measured value with the "true" value. An accurate method provides unbiased results. It is a much more difficult quantity to estimate and can only be inferred by careful attention to possible sources of systematic error.

A laboratory should also conduct regular audits to ensure that its quality assurance program is indeed being carried out appropriately and that the necessary documentation is being maintained.

3.2 External techniques

External evidence for the quality of the measurement process is important for several reasons. First, it provides the most straightforward approach for assuring the compatibility of the measurements with other laboratories. Second, errors can arise over time that internal evaluations can not detect. External quality assessment techniques, however, should supplement, but not replace, a laboratory's ongoing internal quality assessment program.

Collaborative test exercises provide the opportunity to compare an individual laboratory's performance with that of others. If the results for the test samples are known accurately, biases can be evaluated. Such exercises were organized as part of the WOCE/JGOFS CO_2 survey and provided a useful tool for estimating overall data quality (Dickson, 2001; Feely *et al.*, 2001). Exchange of samples, or of internal test solutions with other laboratories can provide similar evidence of the level of agreement or possible biases in particular laboratories.

The use of reference materials to evaluate measurement capability is the procedure of choice whenever suitable reference materials are available. Reference materials are stable substances for which one or more properties are established sufficiently well to calibrate a chemical analyzer, or to validate a measurement process (Taylor, 1987). Ideally, such materials are based on a matrix similar to that of the samples of interest, in this case, sea water. The most useful reference materials are those for which one or more properties have been *certified* as accurate, preferably by the use of a definitive method in the hands of two or more analysts. Reference materials test the full measurement process (though not the sampling).

The U.S. National Science Foundation funded the development of certified reference materials (CRMs) for the measurement of oceanic CO_2 parameters (Dickson, 2001); the U.S. Department of Energy promoted the widespread use of CRMs by providing to participants (both from the U.S. and from other nations) in the WOCE/JGOFS CO_2 survey, the time-series stations at Hawaii and Bermuda and to other JGOFS investigations (Feely *et al.*, 2001). The Scripps Institution of Oceanography CRMs have proven to be a valuable quality assessment tool over the last decade and are currently widely used by the international ocean carbon community[3]. We recommend their use in the individual SOPs (see Table 2 for their certification status). Ideally, CRMs should be analyzed on each instrument any time a component of the system is changed (*e.g.*, with each new coulometer cell for C_T) or at least once per day. If resources are limited, a minimum of 12 CRMs, spread evenly over the timeframe of the expedition, should be analyzed to give reasonable confidence in the average value.

[3] Available from Dr. Andrew G. Dickson, Marine Physical Laboratory, Scripps Institution of Oceanography, University of California, San Diego, 9500 Gilman Drive, La Jolla, CA 92093-0244, U.S.A. (fax: 1-858-822-2919; e-mail: co2crms@ucsd.edu; http://andrew.ucsd.edu/co2qc/).

Table 2 Present status (2007) of certified reference materials for the quality control of oceanic carbon dioxide measurements.

Analytical Measurement	Desired Accuracy[a]	Certification
total dissolved inorganic carbon	± 1 μmol kg^{-1}	since 1991
total alkalinity	± 1 μmol kg^{-1}	since 1996[b]
pH	± 0.002	—[c]
$f(CO_2)$	± 0.05 Pa (0.5 μatm)	—[d]

[a] Based on considerations outlined in the report of SCOR Working Group 75 (SCOR, 1985). They reflect the desire to measure changes in the CO_2 content of sea water that allow the increases due to the burning of fossil fuels to be observed.

[b] Representative samples of earlier batches were also certified for alkalinity at that time.

[c] The pH of a reference material can be calculated from the measurements of total dissolved inorganic carbon and total alkalinity. Also, buffer solutions based on TRIS in synthetic sea water can be certified for pH, but—as yet—this is not done regularly.

[d] CO_2 in air reference materials are presently available through a variety of sources. However, it is desirable to use a sterilized sea water sample as a reference material for a discrete $f(CO_2)$ measurement. Although the thermodynamics of the sea water system suggest that, since the CRMs are certified stable for C_T, A_T, and pH, they should be stable for $f(CO_2)$, a reliable technique for independently determining $f(CO_2)$ to allow proper certification has not yet been developed.

4. Calibration of temperature measurements

The accurate measurement of temperature is central to many of the SOPs included in this Guide, yet, on a number of occasions, it has been apparent that the calibration of the various temperature probes that have been used has not received the attention it should. To be accurate, all temperature sensors must be calibrated against a known standard. However, only short-term stability is checked during calibration. Long-term stability should be monitored and determined by the user through periodic regular comparisons with standards of higher accuracy. The frequency of such checks should be governed by experience, recognizing the potential fragility of many temperature probes.

The official temperature scale presently in use is the International Temperature Scale of 1990 (ITS-90)[4]. Although this is intended to represent closely *thermodynamic temperature* over a wide range of temperatures, it is first and foremost a temperature scale that can be realized in practice. It achieves this by assigning temperatures to particular fixed points such as the triple point of water: 273.16 K (0.01°C), or the triple point of gallium: 302.9146 K (29.7646°C), as well as defining appropriate interpolating equations based (for the oceanographic temperature range) on the properties of a standard platinum resistance thermometer.

Typically, working thermometer probes[5] are calibrated (at a number of different temperatures over the desired range of use) by placing them in a stable

[4] For additional information, see http://www.its-90.com.

[5] For high-quality measurements it is appropriate to recognize that what is typically needed is not just a calibration of the thermometer probe, but rather of the entire temperature measuring system (probe and readout).

temperature environment (*e.g.*, a temperature-controlled water bath) where their reading can be compared with the temperature value obtained using a reference thermometer whose own calibration is traceable to ITS-90. A good rule-of-thumb is that the uncertainty of this reference thermometer should be about 4 times smaller than the uncertainty desired for the thermometer being calibrated. Usually the reference thermometer is itself calibrated annually at an accredited calibration facility. The stability of a probe can be ascertained by monitoring its performance at a single temperature. (As is noted in the next section, it is important—for quality assurance purposes—to document the calibration of any thermometer used in the measurements described in this Guide.)

5. Documentation

One aspect of quality assurance that merits emphasis is that of documentation. All data must be technically sound and supported by evidence of unquestionable reliability. While the correct use of tested and reliable procedures such as those described in Chapter 4 is, without doubt, the most important part of quality control, inadequate documentation can cast doubt on the technical merits and defensibility of the results produced. Accordingly, adequate and accurate records must be kept of:

- when the measurement was made (date and time of taking the sample as well as date and time of processing the sample; in special cases, geological age of sample);
- where the measurement was made (latitude, longitude of the sampling from the official station list);
- what was measured (variables/parameters, units);
- how the measurement was made (equipment, calibration, methodology *etc.*, with references to literature, if available);
- who measured it (name and institution of the Principal Investigator);
- publications associated (in preparation or submitted);
- data obtained;
- calculations;
- quality assurance support;
- relevant data reports.

Although good analysts have historically kept such documentation, typically in bound laboratory notebooks, current practices of data sharing and archiving of data at national and world data centers require that this documentation (known as metadata) be maintained in electronic format with the data. Without an accompanying electronic version of the metadata to document methods and QA/QC protocols, archived data are of limited use. The challenge of documenting changes in the Earth system that have been ongoing since before any measurements were done makes it particularly important that data collected at different times and places be comparable, and that archived data be sufficiently well documented to be usable for decades or longer.

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Chapter 4

Recommended standard operating procedures

Standard operating procedures (SOPs) describe the way specific operations or analytical methods should be carried out. They comprise written instructions which define completely the procedure to be adopted by an analyst to obtain the required result. This Guide contains SOPs that fall under three categories. SOPs with numbers 1–10 are procedures for sampling and analysis. SOPs with numbers 11–20 are procedures related to calibrations. SOPs with numbers 21 and higher are for computations and quality control. These procedures have been in use since the early 1990s and have been revised with accumulated experience and improved technology. These are the recommended standard procedures for those participating in the CLIVAR/CO_2 repeat hydrography program. Each SOP has a revision date and version number that should be cited when referencing a procedure in scientific publications. Procedures for reporting errors are given in Chapter 1.

Many of the SOPs contain example calculations. Our philosophy on the precision given in these is that the answers should be correct whether the later steps are done from the partially rounded intermediate values shown, or all steps are done directly from the input data without rounding. However, there may be a few cases where the final result will be different depending on which of these two approaches is used.

1. Procedures for sampling and analysis

- SOP 1 Water sampling for the parameters of the oceanic carbon dioxide system
- SOP 2 Determination of total dissolved inorganic carbon in sea water
- SOP 3a Determination of total alkalinity in sea water using a closed-cell titration
- SOP 3b Determination of total alkalinity in sea water using an open-cell titration
- SOP 4 Determination of $p(CO_2)$ in air that is in equilibrium with a discrete sample of sea water
- SOP 5 Determination of $p(CO_2)$ in air that is in equilibrium with a continuous stream of sea water

SOP 6a Determination of the pH of sea water using a glass/reference electrode cell
SOP 6b Determination of the pH of sea water using the indicator dye *m*-cresol purple
SOP 7 Determination of dissolved organic carbon and total dissolved nitrogen in sea water

2. Procedures for calibrations, *etc*.

SOP 11 Gravimetric calibration of the volume of a gas loop using water
SOP 12 Gravimetric calibration of volume delivered using water
SOP 13 Gravimetric calibration of volume contained using water
SOP 14 Procedure for preparing sodium carbonate solutions for the calibration of coulometric C_T measurements

3. Procedures for computations, quality control, *etc.*

SOP 21 Applying air buoyancy corrections
SOP 22 Preparation of control charts
SOP 23 Statistical techniques used in quality assessment
SOP 24 Calculation of the fugacity of carbon dioxide in pure carbon dioxide gas or in air

Chapter 5

Physical and thermodynamic data

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1. Values for various fundamental constants

R = 8.314472(15) J K^{-1} mol^{-1},
F = 96485.3399(24) C mol^{-1},
0°C = 273.15 K (defined),
1 atm = 101325 Pa (defined)

(from http://physics.nist.gov/cuu/Constants/index.html). For each constant, the standard uncertainty in the least significant digits is given in parentheses.

2. Atomic weights

Atomic weights are quoted here (Table 1) to 5 significant figures unless the dependable accuracy is more limited by either the combined uncertainties of the best published atomic weight determinations, or by the variability of isotopic composition in normal terrestrial occurrences (elements **annotated r**). The last significant figure of each tabulated value is considered reliable to at least ±1 except when a larger single-digit uncertainty is inserted in parentheses following the atomic weight. In many cases the "official" values (IUPAC, 2006) have more than five significant figures and the precision is considerably better than ±1 at the precision shown here. In a few cases the truncation to five significant figures will mean that the true confidence interval is strongly asymmetric relative to the values shown here. Neither the highest nor the lowest actual atomic weight of any normal sample is thought likely to differ from the tabulated value by more than the assigned uncertainty. However, the tabulated values do not apply either to samples of highly exceptional isotopic composition arising from most geological occurrences (elements **annotated g**) or to those whose isotopic composition has been artificially altered. Such might even be found in commerce without disclosure of that modification (elements **annotated m**). Elements that have no stable isotope are excluded from this table except for Th, Pa, and U which do have a characteristic terrestrial isotope composition.

Table 1 IUPAC (2006) table of standard atomic weights abridged to five significant figures. Scaled to the relative atomic mass $A(^{12}C) = 12$ (includes 2007 revisions).

	Name	Symbol	Atomic weight	Annotations
1	Hydrogen	H	1.0079	g m
2	Helium	He	4.0026	
3	Lithium	Li	6.941(2)	g m r
4	Beryllium	Be	9.0122	
5	Boron	B	10.811(7)	g m r
6	Carbon	C	12.011	g r
7	Nitrogen	N	14.007	
8	Oxygen	O	15.999	
9	Fluorine	F	18.998	
10	Neon	Ne	20.180	m
11	Sodium (Natrium)	Na	22.990	
12	Magnesium	Mg	24.305	

Table 1 Continued.

	Name	Symbol	Atomic weight	Annotations
13	Aluminium	Al	26.982	
14	Silicon	Si	28.086	
15	Phosphorus	P	30.974	
16	Sulfur	S	32.065(5)	g r
17	Chlorine	Cl	35.453(2)	m
18	Argon	Ar	39.948	g r
19	Potassium (Kalium)	K	39.098	g
20	Calcium	Ca	40.078(4)	g
21	Scandium	Sc	44.956	
22	Titanium	Ti	47.867	
23	Vanadium	V	50.942	
24	Chromium	Cr	51.996	
25	Manganese	Mn	54.938	
26	Iron	Fe	55.845(2)	
27	Cobalt	Co	58.933	
28	Nickel	Ni	58.693	
29	Copper	Cu	63.546(3)	r
30	Zinc	Zn	65.38(2)	
31	Gallium	Ga	69.723	
32	Germanium	Ge	72.64	
33	Arsenic	As	74.922	
34	Selenium	Se	78.96(3)	
35	Bromine	Br	79.904	
36	Krypton	Kr	83.798(2)	g m
37	Rubidium	Rb	85.468	
38	Strontium	Sr	87.62	
39	Yttrium	Y	88.906	
40	Zirconium	Zr	91.224(2)	g
41	Niobium	Nb	92.906	
42	Molybdenum	Mo	95.96(2)	g
44	Ruthenium	Ru	101.07(2)	g
45	Rhodium	Rh	102.91	
46	Palladium	Pd	106.42	g
47	Silver	Ag	107.87	
48	Cadmium	Cd	112.41	
49	Indium	In	114.82	
50	Tin	Sn	118.71	
51	Antimony (Stibium)	Sb	121.76	g
52	Tellurium	Te	127.60(3)	g
53	Iodine	I	126.90	
54	Xenon	Xe	131.29	g m
55	Caesium	Cs	132.91	
56	Barium	Ba	137.33	
57	Lanthanum	La	138.91	

Table 1 Continued.

	Name	Symbol	Atomic weight	Annotations
58	Cerium	Ce	140.12	g
59	Praesodymium	Pr	140.91	
60	Neodymium	Nd	144.24	g
62	Samarium	Sm	150.36(2)	g
63	Europium	Eu	151.96	g
64	Gadolinium	Gd	157.25(3)	g
65	Terbium	Tb	158.93	
66	Dysprosium	Dy	162.50	g
67	Holmium	Ho	164.93	
68	Erbium	Er	167.26	g
69	Thulium	Tm	168.93	
70	Ytterbium	Yb	173.05	
71	Lutetium	Lu	174.97	g
72	Hafnium	Hf	178.49(2)	
73	Tantalum	Ta	180.95	
74	Tungsten (Wolfram)	W	183.84	
75	Rhenium	Re	186.21	
76	Osmium	Os	190.23(3)	g
77	Iridium	Ir	192.22	
78	Platinum	Pt	195.08	
79	Gold	Au	196.97	
80	Mercury	Hg	200.59(2)	
81	Thallium	Tl	204.38	
82	Lead	Pb	207.2	g r
83	Bismuth	Bi	208.98	
90	Thorium*	Th	232.04	g
91	Protoactinium*	Pa	231.04	
92	Uranium*	U	238.03	g m

* These elements have no stable isotope.

3. Vapor pressure of water

3.1 Pure water

The vapor pressure of pure water (p_σ) over the temperature range 273 to 647 K (*i.e.*, from the triple point to the critical point of water) is represented by the polynomial (Wagner and Pruß, 2002)

$$\ln\left(\frac{p_\sigma}{p_c}\right) = \frac{T_c}{T}\left(a_1\vartheta + a_2\vartheta^{1.5} + a_3\vartheta^3 + a_4\vartheta^{3.5} + a_5\vartheta 4 + a_6\vartheta^{7.5}\right) \qquad (1)$$

where $\vartheta = (1 - T/T_c)$, T_c = 647.096 K and p_c = 22.064 MPa. The coefficients are:

$$\begin{aligned} a_1 &= -7.859\,517\,83, & a_4 &= 22.680\,741\,1, \\ a_2 &= 1.844\,082\,59, & a_5 &= -15.961\,871\,9, \\ a_3 &= -11.786\,649\,7, & a_6 &= 1.801\,225\,02. \end{aligned}$$

At 25°C (298.15 K), $p_\sigma = 3.1698$ kPa.

3.2 Sea water

For sea water, the vapor pressure is related to that of pure water,

$$p_\sigma\ (\mathrm{s/w}) \approx p_\sigma \exp\left(-0.018\phi \sum_{\mathrm{B}} m_{\mathrm{B}}/m^\circ\right) \tag{2}$$

where

p_σ is the vapor pressure of pure water (1),
$\sum_{\mathrm{B}} m_{\mathrm{B}}$ is the total molality of dissolved species (3),
ϕ is the osmotic coefficient of sea water (4),
$m^\circ = 1$ mol kg-H_2O^{-1}.

For sea water (of the composition detailed in section 6.1),

$$\sum_{\mathrm{B}} m_{\mathrm{B}}/m^\circ = \frac{31.998S}{10^3 - 1.005S} \tag{3}$$

and the osmotic coefficient at 25°C is given by (Millero, 1974)

$$\begin{aligned} \phi = 0.90799 - 0.08992\left(\frac{\frac{1}{2}\sum_{\mathrm{B}} m_{\mathrm{B}}}{m^\circ}\right) + 0.18458\left(\frac{\frac{1}{2}\sum_{\mathrm{B}} m_{\mathrm{B}}}{m^\circ}\right)^2 \\ - 0.07395\left(\frac{\frac{1}{2}\sum_{\mathrm{B}} m_{\mathrm{B}}}{m^\circ}\right)^3 - 0.00221\left(\frac{\frac{1}{2}\sum_{\mathrm{B}} m_{\mathrm{B}}}{m^\circ}\right)^4 \end{aligned} \tag{4}$$

for $I = 0.3 - 0.8$ mol kg-H_2O^{-1} ($S = 16$–40). (Although strictly speaking, ϕ is a function of temperature as well as of I, the change between 0 and 40°C is typically about 1% and can be ignored here.)

At 25°C and $S = 35$, $p_\sigma\,(\mathrm{s/w}) = 3.1106$ kPa.

4. Densities of various substances

4.1 Air-saturated water

The density of air-saturated water in the temperature range 5 to 40°C—*i.e.*, avoiding the temperature of maximum density—is given by the expression (Jones and Harris, 1992)

$$\begin{aligned} \rho_{\mathrm{W}}/(\mathrm{kg\ m^{-3}}) = 999.84847 + 6.337563\times10^{-2}(t/^\circ\mathrm{C}) - 8.523829\times10^{-3}(t/^\circ\mathrm{C})^2 \\ + 6.943248\times10^{-5}(t/^\circ\mathrm{C})^3 - 3.821216\times10^{-7}(t/^\circ\mathrm{C})^4\,. \end{aligned} \tag{5}$$

At 25°C, $\rho_{\mathrm{W}} = 997.041$ kg m^{-3} = 0.997041 g cm^{-3}.

4.2 Sea water

The density of sea water in the temperature range 0 to 40°C (IPTS 68[1]) and the salinity range 0 to 42 is given by the expression (Millero and Poisson, 1981)

$$\rho_{SW}/(\text{kg m}^{-3}) = \rho_{SMOW}/(\text{kg m}^{-3}) + AS + BS^{1.5} + CS^2 \qquad (6)$$

where[2]

$$\begin{aligned}\rho_{SMOW}/(\text{kg m}^{-3}) = {} & 999.842594 + 6.793952\times10^{-2}(t/°\text{C}) \\ & - 9.095290\times10^{-3}(t/°\text{C})^2 + 1.001685\times10^{-4}(t/°\text{C})^3 \\ & - 1.120083\times10^{-6}(t/°\text{C})^4 + 6.536332\times10^{-9}(t/°\text{C})^5 , \end{aligned} \qquad (7)$$

$$\begin{aligned}A = {} & 8.24493\times10^{-1} - 4.0899\times10^{-3}(t/°\text{C}) \\ & + 7.6438\times10^{-5}(t/°\text{C})^2 - 8.2467\times10^{-7}(t/°\text{C})^3 + 5.3875\times10^{-9}(t/°\text{C})^4 , \end{aligned} \qquad (8)$$

$$B = -5.72466\times10^{-3} + 1.0227\times10^{-4}(t/°\text{C}) - 1.6546\times10^{-6}(t/°\text{C})^2 , \qquad (9)$$

$$C = 4.8314\times10^{-4} , \qquad (10)$$

t is on IPTS 68 and S is the salinity.

At 25°C (IPTS 68) and $S = 35$, $\rho_{SW} = 1023.343$ kg m^{-3}.

4.3 Sodium chloride solutions

The density of a solution of sodium chloride in water in the temperature range 0 to 50°C (see Footnote 1) and the concentration range 0.1 mol kg-H_2O^{-1} to saturation can be calculated from the expression (Lo Surdo *et al.*, 1982)

$$\begin{aligned}\frac{10^3(\rho(\text{NaCl}) - \rho_{SMOW})}{\text{g cm}^{-3}} = {} & \left(\frac{m}{m°}\right)\left[45.5655 - 0.2341\left(\frac{t}{°\text{C}}\right)\right. \\ & \left. + 3.4128\times10^{-3}\left(\frac{t}{°\text{C}}\right)^2 - 2.7030\times10^{-5}\left(\frac{t}{°\text{C}}\right)^3 + 1.4037\times10^{-7}\left(\frac{t}{°\text{C}}\right)^4\right] \\ & + \left(\frac{m}{m°}\right)^{3/2}\left[-1.8527 + 5.3956\times10^{-2}\left(\frac{t}{°\text{C}}\right) - 6.2635\times10^{-4}\left(\frac{t}{°\text{C}}\right)^2\right] \\ & + \left(\frac{m}{m°}\right)^{2}\left[-1.6368 - 9.5653\times10^{-4}\left(\frac{t}{°\text{C}}\right) + 5.2829\times10^{-5}\left(\frac{t}{°\text{C}}\right)^2\right] \\ & + 0.2274\left(\frac{m}{m°}\right)^{5/2} \end{aligned} \qquad (11)$$

---

[1] The International Practical Temperature Scale of 1968 (IPTS 68) has been superseded by the International Temperature Scale of 1990 (ITS 90). A simple equation can be used to relate the two over the oceanographic temperature range 0 to 40°C (Jones and Harris, 1992):

$$t_{90}/°\text{C} = 0.0002 + 0.99975\ t_{68}/°\text{C} .$$

[2] SMOW—Standard Mean Ocean Water (Craig, 1961)—is pure water with a specified isotopic composition and free of dissolved gases.

where t is the temperature (IPTS 68), m the molality of the sodium chloride solution, and m° = 1 mol kg-H_2O^{-1}. ρ_{SMOW} is calculated using equation (7)—see Footnote 3.

To convert the concentration of sodium chloride expressed in mol kg-soln^{-1}—C(NaCl)—to mol kg-H_2O^{-1}, use the expression

$$\frac{m(\mathrm{NaCl})}{m^\circ} = \frac{10^3 C(\mathrm{NaCl})}{10^3 - 58.443 C(\mathrm{NaCl})}. \tag{12}$$

At 25°C and m = 0.725 mol kg-H_2O^{-1}, ρ (NaCl) = 1.02581 g cm^{-3}.

4.4 A mixture of NaCl and HCl at 25°C

An expression based on Young's rule has been developed for the density of a mixture of NaCl and HCl at a temperature of 25°C[4] (Millero, personal communication):

$$\rho_{\mathrm{mix}}(25\,^\circ\mathrm{C}) = \frac{\rho_{\mathrm{W}}(25\,^\circ\mathrm{C})\left[10^3 + m_{\mathrm{T}}\left(m(\mathrm{HCl}) + m(\mathrm{NaCl})\right)\right]}{10^3 + \varphi_{\mathrm{mix}}\left(m(\mathrm{HCl}) + m(\mathrm{NaCl})\right)\left(\rho_{\mathrm{W}}(25\,^\circ\mathrm{C})\right)} \tag{13}$$

where ρ_W(25°C) = 0.99704 g cm^{-3},

$$m_{\mathrm{T}} = \frac{36.46 m(\mathrm{HCl}) + 58.44 m(\mathrm{NaCl})}{m(\mathrm{HCl}) + m(\mathrm{NaCl})}, \tag{14}$$

$$\varphi_{\mathrm{mix}} = \frac{m(\mathrm{HCl})\varphi_{\mathrm{HCl}} + m(\mathrm{NaCl})\varphi_{\mathrm{NaCl}}}{m(\mathrm{HCl}) + m(\mathrm{NaCl})}, \tag{15}$$

and the apparent molar volumes at 25°C,

$$\varphi_{\mathrm{HCl}} = 17.854 + 1.460\sqrt{m} - 0.307m, \tag{16}$$

$$\varphi_{\mathrm{NaCl}} = 16.613 + 1.811\sqrt{m} + 0.094m \tag{17}$$

where $m = m$(HCl) + m(NaCl). The concentrations m(HCl) and m(NaCl) are in mol kg-H_2O^{-1}.

At m(HCl) = 0.2 mol kg-H_2O^{-1} and m(NaCl) = 0.5 mol kg-H_2O^{-1}, ρ_{mix}(25°C) = 1.02056 g cm^{-3}.

4.5 Various solids

From data of Weast (1975),

Potassium chloride: ρ (KCl) = 1.984 g cm^{-3} (18)

[3] In the original paper of Lo Surdo *et al.* (1982) an alternate formulation based on the work of Kell (1975) was used for the density of pure water. The difference is < 10^{-5} over the temperature range 0–50°C.

[4] At temperatures other than 25°C, equation (13) is not reliable.

Sodium chloride: $\rho(\mathrm{NaCl}) = 2.165\ \mathrm{g\ cm^{-3}}$ (19)

Sodium carbonate: $\rho(\mathrm{Na_2CO_3}) = 2.532\ \mathrm{g\ cm^{-3}}$ (20)

Sodium sulfate: $\rho(\mathrm{Na_2SO_4}) = 2.68\ \mathrm{g\ cm^{-3}}$ (21)

Sodium tetraborate decahydrate (borax):

$$\rho(\mathrm{Na_2B_4O_7{\cdot}10H_2O}) = 1.73\ \mathrm{g\ cm^{-3}} \quad (22)$$

2-amino-2-hydroxymethyl-1,3-propanediol ("TRIS"):

$$\rho(\mathrm{H_2NC(CH_2OH)_3}) = 1.35\ \mathrm{g\ cm^{-3}} \quad (23)$$

2-aminopyridine: $\rho(\mathrm{C_5H_6N_2}) = 1.24\ \mathrm{g\ cm^{-3}}$ (24)

5. Virial coefficients for carbon dioxide

5.1 Pure carbon dioxide gas

The first virial coefficient of CO_2 is given by the expression (Weiss, 1974)

$$\frac{B(\mathrm{CO_2}, T)}{\mathrm{cm^3\ mol^{-1}}} = -1636.75 + 12.0408\left(\frac{T}{\mathrm{K}}\right) - 3.27957\times10^{-2}\left(\frac{T}{\mathrm{K}}\right)^2 + 3.16528\times10^{-5}\left(\frac{T}{\mathrm{K}}\right)^3 \quad (25)$$

where $265 < T/\mathrm{K} < 320$.

At 25°C (298.15 K), $B(\mathrm{CO_2}, 298.15\ \mathrm{K}) = -123.2\ \mathrm{cm^3\ mol^{-1}}$.

5.2 Carbon dioxide in air

For a binary mixture (B–C), it is possible to define a cross-virial coefficient:

$$\delta_{\mathrm{B-C}} = B_{\mathrm{BC}} - \tfrac{1}{2}(B_{\mathrm{BB}} - B_{\mathrm{CC}})\ . \quad (26)$$

Weiss (1974) used the Lennard–Jones (6–12) potential to calculate values for the cross-virial coefficient δ for the binary mixture: CO_2–air (see also SOP 24). He found that the temperature dependence of this parameter could be represented by the equation

$$\frac{\delta(\mathrm{CO_2 - air})}{\mathrm{cm^3\ mol^{-1}}} = 57.7 - 0.118\left(\frac{T}{\mathrm{K}}\right) \quad (27)$$

where $273 < T/\mathrm{K} < 313$.

At 25°C (298.15 K), $\delta(\mathrm{CO_2}\text{–air}) = 22.5\ \mathrm{cm^3\ mol^{-1}}$.

6. Salinity and the composition of sea water

6.1 The major ion composition of sea water

Traditionally the parameter salinity, *S*, has been used to give a measure of the total dissolved solids in sea water. Originally this was intended to be an analytical parameter with the units g kg^{-1}, but this direct approach was quickly superseded by the practice of estimating salinity from alternative, simpler procedures (*e.g.*, the measurement of chlorinity or conductivity ratio). The concept of a "constant composition of sea water" is then invoked to relate these parameters to salinity (UNESCO, 1966).

Although the idea of "constant composition of sea water" is recognized as being not strictly accurate, it is a useful device in simplifying the study of the various physicochemical properties of sea water. One example of this is the treatment of sea water as a two-component system—water and sea-salt—to represent its thermodynamic properties (*e.g.*, osmotic coefficient or density—see sections 3.2 and 4.2).

Another is the treatment of sea water as a constant ionic medium in which the thermodynamics of various chemical processes involving minor constituents can be studied (*e.g.*, gas solubility or acid–base equilibria).

Analytical results for the other major components of sea water are usually expressed relative to chlorinity (Table 2) and a standard mean chemical composition of sea water (Table 3) can be calculated using the equilibrium constants for the dissociation of water, carbonic and boric acids.

Table 2 Standard mean analytical composition of sea water with S = 35 and chlorinity = 19.374.

Component	Relative concentration[a]	mol kg-soln^{-1}	Reference
Chloride	0.99889	0.54586	calculated from chlorinity
Sulfate	0.1400	0.02824	Morris and Riley (1966)
Bromide	0.003473	0.00084	Morris and Riley (1966)
Fluoride	0.000067	0.00007	Riley (1965)
Sodium	0.55661	0.46906	from charge balance
Magnesium	0.06626	0.05282	Carpenter and Manella (1973)
Calcium	0.02127	0.01028	Riley and Tongudai (1967)
Potassium	0.0206	0.01021	Riley and Tongudai (1967)
Strontium	0.00041	0.00009	Riley and Tongudai (1967)
Boron	0.000232	0.000416	Uppström (1974)
Total alkalinity	–	0.002400	average surface water
pH = 8.1	–	$10^{-8.1}$	average surface water

[a] Expressed relative to the chlorinity (= S/1.80655). Thus the total sulfate (molar mass 96.062 g) at a salinity, S, is given by

$$S_T = \left(\frac{0.1400}{96.062}\right) \times \left(\frac{S}{1.80655}\right) \text{ mol kg-soln}^{-1}.$$

Table 3 Standard mean chemical composition of sea water ($S = 35$).

Species	mol kg-soln^{-1}	g kg-soln^{-1}	mol kg-H_2O^{-1}	g kg-H_2O^{-1}
Cl^-	0.54586	19.3524	0.56576	20.0579
SO_4^{2-}	0.02824	2.7123	0.02927	2.8117
Br^-	0.00084	0.0673	0.00087	0.0695
F^-	0.00007	0.0013	0.00007	0.0013
Na^+	0.46906	10.7837	0.48616	11.1768
Mg^{2+}	0.05282	1.2837	0.05475	1.3307
Ca^{2+}	0.01028	0.4121	0.01065	0.4268
K^+	0.01021	0.3991	0.01058	0.4137
Sr^{2+}	0.00009	0.0079	0.00009	0.0079
$B(OH)_3$	0.00032	0.0198	0.00033	0.0204
$B(OH)_4^-$	0.00010	0.0079	0.00010	0.0079
CO_2^*	0.00001	0.0004	0.00001	0.0004
HCO_3^-	0.00177	0.1080	0.00183	0.1117
CO_3^{2-}	0.00026	0.0156	0.00027	0.0162
OH^-	0.00001	0.0002	0.00001	0.0002
sum of column	1.11994	35.1717	1.16075	36.4531
ionic strength	0.69734	–	0.72275	–

6.2 A simplified synthetic sea water recipe

A simplified synthetic sea water recipe can be obtained from the recipe in Table 2 as follows: replace bromide, fluoride, and total alkalinity with chloride and replace strontium with calcium. The resultant composition (Table 4) is the basis of the synthetic sea water that has been used to determine a variety of equilibrium constants for use in sea water (*e.g.*, Dickson, 1990; Roy *et al.*, 1993).

Table 4 Simplified synthetic sea water composition ($S = 35$)[a].

Species	mol kg-soln^{-1}	g kg-soln^{-1}	mol kg-H_2O^{-1}	g kg-H_2O^{-1}
Cl^-	0.54922	19.4715	0.56918	20.1791
SO_4^{2-}	0.02824	2.7128	0.02927	2.8117
Na^+	0.46911	10.7848	0.48616	11.1768
Mg^{2+}	0.05283	1.2840	0.05475	1.3307
Ca^{2+}	0.01036	0.4152	0.01074	0.4304
K^+	0.01021	0.3992	0.01058	0.4137
sum of column	1.11997	35.0675	1.16068	36.3424
ionic strength	0.69713	–	0.72248	–

[a] The composition here is very slightly different from that used by Dickson (1990) or Roy *et al.* (1993). This is the result of minor changes in the molar masses used to compute the various concentrations.

7. Equilibrium constants

All the equations for the equilibrium constants presented here use concentrations expressed in moles per kilogram of solution. In addition, with the exception of that for bisulfate ion, all acid dissociation constants are expressed in terms of "total" hydrogen ion concentration (see Chapter 2).

7.1 Solubility of carbon dioxide in sea water

The equilibrium constant for the process

$$\mathrm{CO_2(g) \rightleftharpoons CO_2^*(aq)}, \tag{28}$$

i.e.,

$$K_0 = [\mathrm{CO_2^*}] / f(\mathrm{CO_2}), \tag{29}$$

is given by the expression (Weiss, 1974)

$$\ln(K/k^\circ) = 93.4517\left(\frac{100}{T/\mathrm{K}}\right) - 60.2409 + 23.3585\ln\left(\frac{T/\mathrm{K}}{100}\right) + S\left[0.023517 - 0.023656\left(\frac{T/K}{100}\right) + 0.0047036\left(\frac{T/K}{100}\right)^2\right]. \tag{30}$$

The fugacity of CO_2 gas (see Chapter 2) is expressed in atm; $k^\circ = 1$ mol kg-soln^{-1}.

At $S = 35$ and $t = 25$°C (298.15 K), $\ln(K_0/k^\circ) = -3.5617$.

7.2 Acid–base reactions in sea water

7.2.1 Bisulfate ion

The equilibrium constant for the reaction

$$\mathrm{HSO_4^- \rightleftharpoons H^+ + SO_4^-}, \tag{31}$$

i.e.,

$$K_S = [\mathrm{H^+}]_F [\mathrm{SO_4^{2-}}] / [\mathrm{HSO_4^-}], \tag{32}$$

is given by the expression (Dickson, 1990a)

$$\ln(K_S/k^\circ) = \frac{-4276.1}{(T/\mathrm{K})} + 141.328 - 23.093\ln(T/\mathrm{K}) + \left(\frac{-13856}{(T/\mathrm{K})} + 324.57 - 47.986\ln(T/\mathrm{K})\right)\times\left(\frac{I}{m^\circ}\right)^{1/2} + \left(\frac{35474}{(T/\mathrm{K})} - 771.54 + 114.723\ln(T/\mathrm{K})\right)\times\left(\frac{I}{m^\circ}\right) - \frac{2698}{(T/\mathrm{K})}\left(\frac{I}{m^\circ}\right)^{3/2} + \frac{1776}{(T/\mathrm{K})}\left(\frac{I}{m^\circ}\right)^2 + \ln(1 - 0.001005S) \tag{33}$$

where $k° = 1$ mol kg-soln^{-1} and hydrogen ion concentration is expressed on the "free" scale. The ionic strength is calculated from the expression

$$I / m° = \frac{19.924S}{1000 - 1.005S}. \tag{34}$$

The term $\ln(1 - 0.001005S)$ converts the value of K_S from mol kg-H_2O^{-1} (used in Dickson, 1990a) to mol kg-soln^{-1}.

At $S = 35$ and $t = 25°C$ (298.15K), $\ln(K_S/k°) = -2.30$.

7.2.2 Boric acid

The equilibrium constant for the reaction

$$B(OH)_3 + H_2O \rightleftharpoons H^+ + B(OH)_4^-, \tag{35}$$

i.e.,

$$K_B = [H^+][B(OH)_4^-] / [B(OH)_3] \tag{36}$$

is given by the expression (Dickson, 1990b)

$$\begin{aligned} \ln\left(\frac{K_B}{k°}\right) = {} & \frac{-8966.90 - 2890.53S^{1/2} - 77.942S + 1.728S^{3/2} - 0.0996S^2}{(T/\mathrm{K})} \\ & + (148.0248 + 137.1942S^{1/2} + 1.62142S) \\ & + (-24.4344 - 25.085S^{1/2} - 0.2474S)\ln(T/\mathrm{K}) \\ & + 0.053105S^{1/2}(T/\mathrm{K}) \end{aligned} \tag{37}$$

where $k° = 1$ mol kg-soln^{-1}. This equation is in excellent agreement with the measurements made by Roy *et al.* (1993a); it is also in reasonable agreement with the results of Hansson (1973a).

At $S = 35$ and $t = 25°C$ (298.15 K), $\ln(K_B/k°) = -19.7964$.

7.2.3 Carbonic acid

The equilibrium constants used here are based on the measurements of Mehrbach *et al*. (1973) and have been converted to the total hydrogen ion pH scale by Lueker *et al.* (2000) who also showed them to be in good agreement with direct measurements of $p(CO_2)$, C_T, and A_T. These constants are in reasonable agreement with those measured by Roy *et al.* (1993b), Goyet and Poisson (1989), and Hansson (1973b).

The equilibrium constant for the reaction

$$CO_2^*(aq) + H_2O(l) \rightleftharpoons H^+(aq) + HCO_3^-(aq), \tag{38}$$

i.e.,

$$K_1 = [H^+][HCO_3^-] / [CO_2^*] \tag{39}$$

is given by the expression (Lueker *et al.*, 2000)

$$\log_{10}(K_1/k°) = \frac{-3633.86}{(T/\mathrm{K})} + 61.2172 - 9.67770\ln(T/\mathrm{K}) + 0.011555S - 0.0001152S^2 \quad (40)$$

where $k°$ = 1 mol kg-soln^{-1}.

At S = 35 and t = 25°C (298.15 K), $\log_{10}(K_1/k°) = -5.8472$.

The equilibrium constant for the reaction

$$\mathrm{HCO_3^-(aq) \rightleftharpoons H^+(aq) + CO_3^{2-}(aq)}, \quad (41)$$

i.e.,

$$K_2 = [\mathrm{H^+}][\mathrm{CO_3^{2-}}]/[\mathrm{HCO_3^-}], \quad (42)$$

is given by the expression (Lueker *et al.,* 2000)

$$\log_{10}(K_2/k°) = \frac{-471.78}{(T/\mathrm{K})} - 25.9290 + 3.16967\ln(T/\mathrm{K}) + 0.01781S - 0.0001122S^2 \quad (43)$$

where $k°$ = 1 mol kg-soln^{-1}.

At S = 35 and t = 25°C (298.15 K), $\log_{10}(K_2/k°) = -8.9660$.

7.2.4 Hydrogen fluoride

The equilibrium constant for the reaction

$$\mathrm{HF(aq) \rightleftharpoons H^+(aq) + F^-(aq)}, \quad (44)$$

i.e.,

$$K_\mathrm{F} = [\mathrm{H^+}][\mathrm{F^-}]/[\mathrm{HF}], \quad (45)$$

is given by the expression (Perez and Fraga, 1987)

$$\ln(K_\mathrm{F}/k°) = \frac{874}{(T/\mathrm{K})} - 9.68 + 0.111S^{1/2} \quad (46)$$

where $k°$ = 1 mol kg-soln^{-1}. This equation gives values that are in reasonable agreement with those suggested by Dickson and Riley (1979a).

At S = 35 and t = 25°C (298.15K), $\ln(K_\mathrm{F}/k°) = -6.09$.

7.2.5 Phosphoric acid

The expressions below are from Millero (1995)[5] and are a composite of measurements by Kester and Pytkowicz (1967), Dickson and Riley (1979b), and Johansson and Wedborg (1979).

[5] 0.015 has been subtracted from the constant term in each of these expressions: (49), (52), (55) to convert—approximately—from the SWS pH scale (including HF) used by Millero (1995) to the "total" hydrogen ion scale used here.

The equilibrium constant for the reaction

$$H_3PO_4(aq) \rightleftharpoons H^+(aq) + H_2PO_4^-(aq), \tag{47}$$

i.e.,

$$K_{1P} = [H^+][H_2PO_4^-]/[H_3PO_4], \tag{48}$$

is given by the expression

$$\ln(K_{1P}/k^\circ) = \frac{-4576.752}{T/K} + 115.525 - 18.453\ln(T/\mathrm{K}) + \left(\frac{-106.736}{(T/\mathrm{K})} + 0.69171\right)S^{1/2} + \left(-\frac{0.65643}{(T/\mathrm{K})} - 0.01844\right)S \tag{49}$$

where k° = 1 mol kg-soln^{-1}.

At S = 35 and t = 25°C (298.15 K), $\ln(K_{1P}/k^\circ) = -3.71$.

The equilibrium constant for the reaction

$$H_2PO_4^-(aq) \rightleftharpoons H^+(aq) + HPO_4^{2-}(aq), \tag{50}$$

i.e.,

$$K_{2P} = [H^+][HPO_4^{2-}]/[H_2PO_4^-], \tag{51}$$

is given by the expression

$$\ln(K_{2P}/k^\circ) = \frac{-8814.715}{T/\mathrm{K}} + 172.0883 - 27.927\ln(T/\mathrm{K}) + \left(\frac{-160.340}{(T/\mathrm{K})} + 1.3566\right)S^{1/2} + \left(\frac{0.37335}{(T/\mathrm{K})} - 0.05778\right)S \tag{52}$$

where k° = 1 mol kg-soln^{-1}.

At S = 35 and t = 25°C (298.15 K), $\ln(K_{2P}/k^\circ) = -13.727$.

The equilibrium constant for the reaction

$$HPO_4^{2-}(aq) \rightleftharpoons H^+(aq) + PO_4^{3-}(aq), \tag{53}$$

i.e.,

$$K_{3P} = [H^+][PO_4^{3-}]/[HPO_4^{2-}], \tag{54}$$

is given by the expression

$$\ln(K_{3P}/k^\circ) = \frac{-3070.75}{(T/\mathrm{K})} - 18.141 + \left(\frac{17.27039}{(T/\mathrm{K})} + 2.81197\right)S^{1/2} + \left(\frac{-44.99486}{(T/\mathrm{K})} - 0.09984\right)S \tag{55}$$

where k° = 1 mol kg-soln^{-1}.

At S = 35 and t = 25°C (298.15 K), $\ln(K_{3P}/k^\circ) = -20.24$.

7.2.6 Silicic acid

The equilibrium constant for the reaction

$$\mathrm{Si(OH)_4(aq) \rightleftharpoons H^+(aq) + SiO(OH)_3^-(aq)}, \tag{56}$$

i.e.,

$$K_{\mathrm{Si}} = [\mathrm{H^+}][\mathrm{SiO(OH)_3^-}]/[\mathrm{Si(OH)_4}], \tag{57}$$

is given by the expression (Millero, 1995)

$$\begin{aligned}\ln(K_{\mathrm{Si}}/k^\circ) = {} & \frac{-8904.2}{(T/\mathrm{K})} + 117.385 - 19.334\ln(T/\mathrm{K}) \\ & + \left(\frac{-458.79}{(T/\mathrm{K})} + 3.5913\right)(I/m^\circ)^{1/2} + \left(\frac{188.74}{(T/\mathrm{K})} - 1.5998\right)(I/m^\circ) \\ & + \left(\frac{-12.1652}{(T/\mathrm{K})} + 0.07871\right)(I/m^\circ)^2 + \ln(1 - 0.001005S)\end{aligned} \tag{58}$$

where k° = 1 mol kg-soln^{-1}. This expression is based on the results of Sjöberg *et al.* (1981) and the review by Baes and Mesmer (1976); 0.015 has been subtracted from the constant (see Footnote 5).

The ionic strength is calculated from the expression

$$I/m^\circ = \frac{19.924S}{1000 - 1.005S} \approx 0.02S\,. \tag{59}$$

The term $\ln(1 - 0.001005S)$ converts the value of K_{Si} from mol kg-H_2O^{-1} to mol kg-soln^{-1}; m° is as in equation (11).

At S = 35 and t = 25°C (298.15 K), $\ln(K_{\mathrm{Si}}/k^\circ) = -21.61$.

7.2.7 Water

The equilibrium constant for the reaction

$$\mathrm{H_2O(l) \rightleftharpoons H^+(aq) + OH^-(aq)}, \tag{60}$$

i.e.,

$$K_{\mathrm{W}} = [\mathrm{H^+}][\mathrm{OH^-}], \tag{61}$$

is given by the expression (Millero, 1995)

$$\begin{aligned}\ln\left(K_{\mathrm{W}}/(k^\circ)^2\right) = {} & \frac{-13847.26}{(T/\mathrm{K})} + 148.9652 - 23.6521\ln(T/\mathrm{K}) \\ & + \left(\frac{118.67}{(T/\mathrm{K})} - 5.977 + 1.0495\ln(T/\mathrm{K})\right)S^{1/2} - 0.01615S\end{aligned} \tag{62}$$

where k° = 1 mol kg-soln^{-1}. This expression is based on results published by Hansson (1973a), Culberson and Pytkowicz (1973), and Dickson and Riley (1979a). Note that 0.015 has been subtracted from the constant term (see Footnote 5).

At S = 35 and t = 25°C (298.15 K), $\ln(K_{\mathrm{W}}/(k^\circ)^2) = -30.434$.

7.3 Acid–base reactions in sodium chloride media

The values given here are appropriate to a background medium with C(NaCl) = 0.7 mol kg-soln^{-1} and at a temperature of 25°C.

7.3.1 Carbonic acid

The values given here are from Dyrssen and Hansson (1973).

The equilibrium constant for the reaction

$$CO_2^*(aq) + H_2O(l) \rightleftharpoons H^+(aq) + HCO_3^-(aq), \quad (63)$$

i.e.,

$$K_1 = [H^+][HCO_3^-]/[CO_2^*], \quad (64)$$

at C(NaCl) = 0.7 mol kg-soln^{-1} and t = 25°C is

$$\ln(K_1/k^\circ) = -13.82. \quad (65)$$

The equilibrium constant for the reaction

$$HCO_3^-(aq) \rightleftharpoons H^+(aq) + CO_3^{2-}(aq), \quad (66)$$

i.e.,

$$K_2 = [H^+][CO_3^{2-}]/[HCO_3^-], \quad (67)$$

at C(NaCl) = 0.7 mol kg-soln^{-1} and t = 25°C is

$$\ln(K_2/k^\circ) = -21.97. \quad (68)$$

7.3.2 2-amino-2-hydroxymethyl-1,3-propanediol ("TRIS")

The equilibrium constant for the reaction

$$H_3NC(CH_2OH)_3^+(aq) \rightleftharpoons H^+(aq) + H_2NC(CH_2OH)_3(aq), \quad (69)$$

i e.,

$$K_{tris} = [H^+][H_2NC(CH_2OH)_3]/[H_3NC(CH_2OH)_3^+], \quad (70)$$

at C(NaCl) = 0.7 mol kg-soln^{-1} and t = 25°C is

$$\ln(K_{TRIS}/k^\circ) = -18.90 \quad (71)$$

(Millero *et al.*, 1987).

7.3.3 Water

The equilibrium constant for the reaction

$$H_2O(l) \rightleftharpoons H^+(aq) + OH^-(aq), \quad (72)$$

i.e.,

$$K_W = [H^+][OH^-], \quad (73)$$

at C(NaCl) = 0.7 mol kg-soln^{-1} and t = 25°C is

$$\ln\left(K_W/(k°)^2\right) = -31.71 \quad (74)$$

(Dyrssen and Hansson, 1973).

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SOP 1

Water sampling for the parameters of the oceanic carbon dioxide system

1. Scope and field of application

This SOP describes how to collect discrete samples, from a Niskin or other water sampler, that are suitable for the analysis of the four measurable inorganic carbon parameters: total dissolved inorganic carbon, total alkalinity, pH and CO_2 fugacity.

2. Principle

A sample of sea water is collected in a clean glass container in a manner designed to minimize gas exchange with the atmosphere (note: CO_2 exchange affects the various carbon parameters to differing degrees ranging from the very sensitive CO_2 fugacity, $f(CO_2)$, to alkalinity which is not affected by gas exchange). The sample may be treated with a mercuric chloride solution to prevent biological activity, and then the container is closed to prevent exchange of carbon dioxide or water vapor with the atmosphere.

3. Apparatus

The sample containers are somewhat different depending on which parameter is being collected, but the basic concept is similar for the four possible inorganic carbon samples. In general, one needs a flexible plastic drawing tube, a clean[1] glass sample container with stoppers, a container and dispenser for the mercuric chloride solution (if it is being used) and a sampling log to record when and where each of the samples were collected.

3.1 Drawing tube

Tygon® tubing is normally used to transfer the sample from the Niskin to the sample container; however, if dissolved organic carbon samples are being collected from the same Niskins, then it may be necessary to use silicone tubing to prevent contamination from the Tygon®. The drawing tube can be pre-treated

[1] Cleaning sample containers by precombustion in a muffle furnace will remove any organic carbon and associated microorganisms. Some groups soak the bottles in 1 N HCl; however, care must be taken to remove all residual acid during rinsing.

by soaking in clean sea water for at least one day. This minimizes the amount of bubble formation in the tube when drawing a sample.

3.2 Sample container

The sample container depends on the parameter being measured. Typically, the $f(CO_2)$ samples are analyzed directly from the sample container so they are collected in 500 cm^3 volumetric flasks that have been pre-calibrated for a documented volume and sealed with screw caps that have internal plastic conical liners. Samples for pH are also typically analyzed directly from the sample containers. For spectrophotometric pH measurements, the samples are collected directly into 10 cm path-length optical cells and sealed with polytetrafluoroethylene (Teflon®) caps ensuring that there is no headspace. For C_T and A_T, high quality borosilicate glass bottles, such as Schott Duran (l.c.e. 32×10^{-7} K^{-1}), are recommended for both temporary and longer term storage. The bottles should be sealed using greased ground glass stoppers held in place with some form of positive closure, or in some alternate gas-tight fashion[2].

3.3 Mercury dispenser

The $f(CO_2)$ and C_T samples should be poisoned with a mercuric chloride solution at the time of sampling. The A_T samples have historically been poisoned as well, but tests have suggested that poisoning may not be required if open ocean samples are kept in the dark at room temperature and are analyzed within 12 hours. Samples for pH are typically not poisoned because the sample size is relatively small and the samples are usually analyzed very quickly after sampling. Although any appropriately sized Eppendorf pipette can be used to add the mercuric chloride solution, it may be more convenient to use a repipetter that can be mounted near the sample collection area. All equipment should be properly labeled for safety.

4. Reagents

4.1 Mercuric chloride solution

Samples collected for $f(CO_2)$, C_T, and, in some cases, A_T, should be poisoned with a mercuric chloride solution to stop biological activity from altering the carbon distributions in the sample container before analysis. A typical solution is saturated mercuric chloride in deionized water. However, saturated solutions have been known to clog the pipette in very cold weather, so some investigators use twice the volume of a 50% saturated solution. Standard volumes used for saturated solutions are 0.05–0.02% of the total sample volume.

[2] Some groups use screw-cap bottles with apparent success, but this method has not been thoroughly tested and should not be used if samples are to be stored for extended periods.

4.2 Stopper grease

C_T and A_T samples are typically collected in borosilicate glass bottles with ground glass stoppers. To form an airtight seal, the stoppers should be greased. Apiezon® L grease has been found to be suitable for this purpose; other greases may also work. Care should be taken not to transfer the grease onto the Niskin bottle as this could interfere with other analyses.

5. Procedure

5.1 Introduction

Collection of water at sea from the Niskin bottle (or other sampler) must be done soon after opening the sampler and before much other water has been removed from it. This is necessary to minimize exchange of CO_2 with the air space in the sampler which affects all carbon parameters except A_T. Other gas samples (*e.g.*, He, CFCs, O_2) have faster exchange rates than CO_2 and are usually sampled before carbon, but it is desirable that the carbon samples be collected before the Niskin bottle is half empty and within 10 minutes of it being first opened. A typical sampling order for carbon is $f(CO_2)$, pH, C_T, then A_T.

5.2 Filling procedure

Rinse the sample bottle — If the bottle is not already clean, rinse it twice with 30–50 cm^3 of sample to remove any traces of a previous sample.

Fill the sample bottle — Fill the bottle smoothly from the bottom using a drawing tube which extends from the Niskin drain to the bottom of the glass sample bottle. For $f(CO_2)$, pH, and C_T, it is critical to remove any bubbles from the draw tube before filling. Overflow the water by at least a half, and preferably by a full, bottle volume[3].

Adjust the headspace — A headspace of 1% of the bottle volume is left to allow for water expansion (see Annexe to this procedure), *i.e.*, 2.5 cm^3 for a 250 cm^3 bottle. This can be achieved by pinching off the draw tube before removing it from the sample bottle or removing excess water using a plastic pipette with a bulb. pH samples should not have a headspace.

Add mercuric chloride — Mercuric chloride is added to poison the sample; the recommended minimum amount is about 0.02% by volume of a saturated aqueous solution. Thus to poison a 250 cm^3 sample requires 0.05 cm^3 (50 μl) of saturated mercuric chloride (or 0.10 cm^3 of a 50% saturated solution). Maximum amount is 0.1% by volume of a saturated aqueous solution, or a smaller percentage than measurement precision of C_T and $f(CO_2)$.

[3] The amount of overflow water can be estimated by measuring how long it takes to fill a sample bottle, and allowing the water to flow for a period of 1.5 times that.

Close the bottle — Seal the bottle carefully to ensure that it remains gas-tight. If it is to be sealed using a greased ground glass stopper[4], first wipe the excess water from the ground glass in the bottle neck, then insert the stopper completely, and finally twist the stopper to squeeze the air out of the grease to make a good seal.

Finally, secure the lid — Use a rubber band or other positive closure, then invert the bottle several times to disperse the mercuric chloride solution thoroughly.

5.3 Sample storage

The samples should be stored in a cool, dark, location (preferably refrigerated but not frozen) until use.

5.4 Sample documentation

The following information must be recorded in the sampling logbook at the time of sampling:

- Time and date when taken;
- Full name of person who took sample;
- Location: an unambiguous designation of the station, cast, and bottle number from which the sample was taken;
- Container designation: a number or alphanumeric symbol unique to the sample container;
- Comments: additional information such as conditions when sampling, problems with sample collection, *etc.*

6. Quality assurance

Some duplicate sampling is recommended, both from the same sampler (*e.g.*, Niskin bottle) and, if possible, from two samplers tripped together at the same depth, to assess the quality of the sampling procedures.

[4] The recommended procedure for re-greasing (or greasing) a stopper is as follows: (a) wipe the stopper with a tissue to remove as much grease as possible and (b) grease the stopper with 4 strips of grease, each strip extending two thirds of the way from the top towards the bottom of the ground portion of the stopper. This provides a path for air to escape when the stopper is inserted into the neck of the bottle.

Annexe

How large a headspace should be left in a sample bottle?

The volume of the headspace is chosen so as to leave room for expansion of the sea water on warming, while being sufficiently small to minimize the amount of gas exchange between the headspace and the bulk of the sample. The closure system must be adequate to retain the pressure exerted by the expansion.

The apparent change in the volume of a fixed mass of sea water can be calculated by allowing for the change in the density of the sea water and the expansion of the glass container. The total change over the temperature range 0–40°C is about 1%. (The effect of expansion on the volume of the borosilicate glass bottle is only 0.04% over this range.) One third of this expansion occurs on heating the sea water from 0 to 20°C, the remaining two thirds on heating it from 20 to 40°C.

The pressure in the headspace of a container heated from a temperature t_1 to t_2 can be estimated, allowing for the following:

- the expansion of the sea water in the bottle,
- the change in solubility of gases such as N_2, O_2, Ar,
- the thermal expansion of the gas phase,
- the change in the vapor pressure of H_2O in the gas phase.

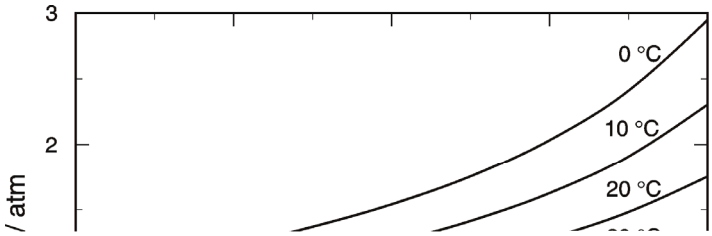

Fig. 1 Pressure in headspace with $r = 0.01$ as a function of temperature for various initial temperatures. In calculating this, it was assumed that the gases—N_2, O_2, Ar, H_2O—were initially at solubility equilibrium with sea water at the starting temperature, that they behaved ideally and that the initial pressure in the bottle at the indicated temperature was 1 atm.

sample bottle, securing it with the metal clamp. Pressurize the bottle, and flush the tubing with about 20 cm^3 of sample (discard to waste).

6.2.2 Fill a 125 cm^3 plastic bottle with sample, cap tightly, and weigh; record the weight to 0.01 g.

6.2.3 Carefully pour the sample into the clean 250 cm^3 jacketed beaker containing a 1½ inch (~ 4 cm) stir bar.

6.2.4 Recap the plastic bottle, and record the empty weight. The sample weight is obtained by difference in the two.

6.2.5 Begin stirring.

6.2.6 Position the holder assembly over the beaker so the four parts are well into the sample without interfering with the stir bar.

6.3 Titration procedure

6.3.1 With slow stirring, dispense enough hydrochloric acid to bring the sample to a pH just above 3.5 (~ 3 cm^3).[7]

6.3.2 Increase the stirring rate until it is vigorous but not splashing. Turn on air flow through the solution.

6.3.3 Leave the acidified sample stirring for at least 6 minutes to allow for CO_2 degassing.

6.3.4 Titrate the sample using 0.05 cm^3 increments to a final pH of *ca*. 3.0 (~ 20 increments). After each addition, record the total dispensed volume to 0.001 cm^3, the e.m.f. to 0.00001 V and the sample temperature to 0.01°C.

6.4 Cleanup after each titration

6.4.1 Once the titration is complete, remove the holder assembly from the beaker, and position it over the waste basin.

6.4.2 Purge the remaining acid in the burette (from the previous titration) into the waste basin, and refill the burette[8]. (To prevent bubbles from forming in the burette and tubing, vent the acid bottle during each filling of the burette.)

6.4.3 Record the hydrochloric acid solution temperature to 0.1°C.

6.4.4 Rinse the acid tip, electrode, and thermometer thoroughly with water from the wash bottle. Gently touch-dry with Kimwipes®.

6.4.5 Pour the spent sample into the waste basin. Use the wash bottle to rinse the beaker and stir bar three times. Thoroughly dry the beaker and stir bar with Kimwipes®, and return the stir bar to the beaker.

---

[7] The amount of acid added will depend on the approximate alkalinity of the sample. Typically, this is known well enough to allow estimation of the initial acid addition.

[8] Purging the burette is a precautionary measure that is not universally used. It is intended to prevent contamination of the acid in the burette tip.

6.5 Cleanup for system storage

If the apparatus will be left out overnight, leave the burette tip, thermometer, and electrode in the last solution titrated. If no more samples will be run for 2 days or longer, clean up the apparatus in the following manner:

6.5.1 Cover the clean, dry beaker and stir bar to protect them from dust.

6.5.2 Disconnect the acid bottle, and seal it with a lightly greased, ground glass stopper[9].

6.5.3 Use Milli-Q® water to thoroughly rinse the glass piece from the acid bottle and the thermometers, then set it out to dry in a place protected from dust.

6.5.4 Refill the burette with air.

6.5.5 Remove the burette and plunger, and thoroughly rinse with Milli-Q® water.

6.5.6 Replace the burette, and dispense 5 cm^3 to purge any acid remaining in the tubing.

6.5.7 As the burette refills, submerge the flexible tubing end (goes to the acid bottle) in a beaker of Milli-Q® water so that the burette is filled with Milli-Q® water.

6.5.8 Again, dispense 5 cm^3 and fill the burette with Milli-Q® water to flush out all the acid.

6.5.9 Finally, refill the burette with air, and purge the tubing of all remaining liquid.

6.5.10 Disconnect the burette, and set it to dry protected from dust.

6.5.11 Rinse the outside of the acid tip, and place it in the test tube holder.

6.5.12 Cover the Dosimat® valve and all tubing with a plastic bag.

6.5.13 Rinse the electrode, cover the filling hole, and place it in a suitable storage solution in an airtight container.

6.5.14 Turn off all instruments.

7. Calculation and expression of results

7.1 Introduction

The titration data can be processed using an Excel® spreadsheet program. Points from the pH region 3.0 to 3.5 are treated using an approach in which the equivalence point is determined using a non-linear least-squares fit of the results. To process sea water samples, the total dissolved inorganic carbon is assumed to be zero, and corrections are made for sulfuric acid and hydrogen fluoride formation.

[9] A screw cap with a Teflon® liner, as is provided with Dosimat® bottles, may also be used.

7.2 Derivation of basic equations

The defining equation for total alkalinity is used to specify a proton condition corresponding to this equivalence point:

$$\begin{aligned}[\mathrm{H^+}]_\mathrm{F} + [\mathrm{HSO_4^-}] + [\mathrm{HF}] + [\mathrm{H_3PO_4}] \\ = [\mathrm{HCO_3^-}] + 2[\mathrm{CO_3^{2-}}] + [\mathrm{B(OH)_4^-}] + [\mathrm{OH^-}] + [\mathrm{HPO_4^{2-}}] \\ + 2[\mathrm{PO_4^{3-}}] + [\mathrm{SiO(OH)_3^-}] + [\mathrm{NH_3}] + [\mathrm{HS^-}].\end{aligned} \tag{2}$$

(Note that the existence of minor, unidentified species has been ignored in this expression.) At each point in the titration, the analytical total concentration of hydrogen ion (relative to this proton condition) is given by

$$\begin{aligned}C_\mathrm{H} = [\mathrm{H^+}]_\mathrm{F} + [\mathrm{HSO_4^-}] + [\mathrm{HF}] + [\mathrm{H_3PO_4}] - [\mathrm{HCO_3^-}] \\ - 2[\mathrm{CO_3^{2-}}] - [\mathrm{B(OH)_4^-}] - [\mathrm{OH^-}] - [\mathrm{HPO_4^{2-}}] \\ - 2[\mathrm{PO_4^{3-}}] - [\mathrm{SiO(OH)_3^-}] - [\mathrm{NH_3}] - [\mathrm{HS^-}].\end{aligned} \tag{3}$$

The initial analytical concentration of hydrogen ion in the solution is thus the negative of the total alkalinity. After a mass m of acid[10] with concentration C (mol kg-soln^{-1}) has been added to a mass m_0 of sample,

$$C_\mathrm{H} = \frac{-m_0 A_\mathrm{T} + m C}{m_0 + m}. \tag{4}$$

This expression can be equated to the previous expression for C_H:

$$\begin{aligned}\frac{-m_0 A_\mathrm{T} + m C}{m_0 + m} = [\mathrm{H^+}]_\mathrm{F} + [\mathrm{HSO_4^-}] + [\mathrm{HF}] + [\mathrm{H_3PO_4}] - [\mathrm{HCO_3^-}] \\ - 2[\mathrm{CO_3^{2-}}] - [\mathrm{B(OH)_4^-}] - [\mathrm{OH^-}] - [\mathrm{HPO_4^{2-}}] \\ - 2[\mathrm{PO_4^{3-}}] - [\mathrm{SiO(OH)_3^-}] - [\mathrm{NH_3}] - [\mathrm{HS^-}].\end{aligned} \tag{5}$$

Equation (5) is the basis of the computations involved in this procedure; however, as only pH data in the range 3.0–3.5 are used, and as the CO_2 generated by the reaction with the acid titrant is lost to the atmosphere, the majority of these terms can be ignored (Dickson *et al.*, 2003). Hence, (5) can be reduced to

$$\frac{-m_0 A_\mathrm{T} + m C}{m_0 + m} \approx [\mathrm{H^+}]_\mathrm{F} + [\mathrm{HSO_4^-}] + [\mathrm{HF}]. \tag{6}$$

7.3 Computational procedures[11]

Equation (6) is used to estimate A_T from titration data by means of a non-linear least-squares procedure. First, it is necessary to start with reasonable estimates

[10] Typically, acid is added by volume, and its density is known accurately. In this procedure, the acid temperature is monitored carefully, and the appropriate density is estimated from laboratory measurements of the acid density as a function of temperature.

[11] The values used for R and F, the functions used for the acid dissociation constants, K_S and K_F, and the expressions for the total concentrations, S_T and F_T, are given in Chapters 2 and 5.

for A_T and $E°$ so as to ensure convergence. A simple Gran approach is used for this. Equation (6) is approximated by

$$\frac{-m_0 A_\mathrm{T} + m C}{m_0 + m} \approx [\mathrm{H}^+] = \exp\left(\frac{E - E°}{RT/F}\right) = k \exp\left(\frac{E}{RT/F}\right) \tag{7}$$

where $[\mathrm{H}^+]$ is the "total" hydrogen ion concentration defined as[12]

$$[\mathrm{H}^+] = [\mathrm{H}^+]_\mathrm{F}\left(1 + S_\mathrm{T}/K_\mathrm{S}\right) \approx [\mathrm{H}^+]_\mathrm{F} + [\mathrm{HSO}_4^-]. \tag{8}$$

In this expression, S_T is the total sulfate concentration, and K_S is the acid dissociation constant of $[\mathrm{HSO}_4^-]$. Equation (7) is rearranged to give the Gran function

$$F_1 = (m_0 + m)\exp\left(\frac{E}{RT/F}\right). \tag{9}$$

This function is linear in m and has a zero at $A_\mathrm{T} = mC/m_0$ that can be estimated from a linear least-squares fit of F_1 against m.

Once the A_T estimate has been obtained, (7) is rearranged to calculate an estimate of $E°$ at each titration point:

$$E° = E - \left(\frac{RT}{F}\right)\ln\left(\frac{-m_0 A_T + m C}{m_0 + m}\right). \tag{10}$$

These values are averaged to obtain an initial estimate of $E°$.

A non-linear least-squares calculation is then used to refine these values of A_T and $E°$. However, rather than adjusting $E°$ directly, it is convenient to define a multiplier

$$f = [\mathrm{H}^+]/[\mathrm{H}'] \tag{11}$$

where estimates of $[\mathrm{H}^+]$ ($[\mathrm{H}']$) are computed from the initial estimate of $E°$:

$$[\mathrm{H}'] = \exp\left(\frac{E - E°}{RT/F}\right), \tag{12}$$

i.e., the error in $E°$ (the difference between this initial estimate and the *true* value) appears as a multiplicative factor in the hydrogen ion concentration (f) that can then be adjusted in the least-squares procedure (rather than adjusting the value of $E°$ directly).

Equation (6) is thus rewritten as

$$A_\mathrm{T} + \left(\frac{S_\mathrm{T}}{1 + K_\mathrm{S}Z/(f\,[\mathrm{H}'])}\right) + \left(\frac{F_\mathrm{T}}{1 + K_\mathrm{F}Z/(f\,[\mathrm{H}'])}\right) + \left(\frac{m_0 + m}{m_0}\right)\left(\frac{f\,[\mathrm{H}']}{Z}\right) - \left(\frac{m}{m_0}\right)C = 0 \tag{13}$$

[12] A comparison of (7) and (8) with (6) shows that the term [HF] has been neglected for this initial stage of the calculation. It is, however, included in the non-linear least-squares evaluation.

where F_T is the total sulfate concentration, and K_F is the acid dissociation constant of [HF]. In this equation, the product, $f\,[H']$, represents the total hydrogen ion concentration and $f\,[H']/Z$ the free hydrogen ion concentration, where $Z = (1 + S_T / K_S)$, and thus

$$[H^+]_F = [H^+]/Z = [H^+]/(1 + S_T / K_S). \quad (14)$$

This approach (though seemingly cumbersome) renders the calculation essentially independent of likely errors in K_S.

The actual data fitting is performed using a non-linear least-squares routine. Equation (13) is used to define a vector of residuals (*i.e.*, the extent to which the left hand side differs from 0), and the software then minimizes the sum-of-squares of these residuals by adjusting the parameters, f and A_T. During this procedure, care is taken to ensure that the initial and final titration points of the data set processed are those for which the calculated pH lies the closest to the values 3.5 and 3.0, respectively. Points that lie outside this region are excluded from the calculation.

The choice of pH range is appropriate for the following reasons. If there is some bicarbonate present, it will be a negligible amount (< 0.5 μmol kg^{-1}) even at the highest pH used (3.5) and will be still less at the lower pH. Furthermore, at pH lower than 3.0, the simple Nernst equation no longer holds true, as the liquid junction potential for a pH cell is a function of hydrogen ion concentration (~ 30 mV/mol-H$^+$ kg^{-1}); in addition, the effect of uncertainties in K_S becomes more problematic at low pHs.

7.4 Example calculation

An example of a complete set of titration data for a sea water sample, together with the resulting calculated values for A_T and $E°$, is given.

Sample information

Mass of sea water 140.32 g
Salinity 33.923

Hydrochloric acid titrant information

Concentration 0.10046 mol kg-soln^{-1}
Density 1.02393 g cm^{-3}

Titration temperature

24.25°C

Titration values

V / cm^{-3}	E / V
3.500	0.18607
3.550	0.18893
3.600	0.19150
3.650	0.19384
3.700	0.19601
3.750	0.19800
3.800	0.19986
3.850	0.20159
3.900	0.20321
3.950	0.20473
4.000	0.20617
4.050	0.20753
4.100	0.20880
4.150	0.21002
4.200	0.21120
4.250	0.21233
4.300	0.21341
4.350	0.21446
4.400	0.21545
4.450	0.21641
4.500	0.21732
4.550	0.21820*

Titration results

A_T = 2260.06 μmol kg-soln^{-1}
$E°$ = 0.394401 V

The point marked with an asterisk was excluded from the final processing as the calculated pH is outside the range 3.0–3.5.

For the most accurate work, a further minor correction may need to be made to compute the total alkalinity in the original sea water sample: for the dilution by mercuric chloride when the sample was collected[13],

$$A_T = 1.0002 \times A_T' . \quad (15)$$

8. Quality assurance

For general principles of analytical quality control, see Chapter 3.

8.1 Target control limits

8.1.1 Introduction

The various control limits outlined below are necessary to ensure that the accuracy and precision of the results are adequate for the purpose of certifying

[13] The value 1.0002 assumes that saturated mercuric chloride was used (0.02% by volume—SOP 1. If a 50% saturated solution was used to preserve the sample, the appropriate correction factor is 1.0004.

reference materials. The targets specified to meet these requirements are a precision (1 SD) of better than 1 μmol kg^{-1} and an overall bias of less than 2 μmol kg^{-1}.

8.1.2 Quality of individual titrations

For each titration, quality can be assessed by examining the standard deviation of the final $E°$ value ($s(E°)$). This is typically less than 0.04 mV for the apparatus used here (*i.e.*, measuring E to within 0.01 mV).

8.1.3 Analysis of a sea water reference material

A certified reference material should be analyzed regularly[14]. Plot the results obtained on a property control chart (see SOP 22). Expect a standard deviation on the order of 1 μmol kg-soln^{-1} or less[15].

8.1.4 Duplicate analyses

A duplicate analysis should be made on each sample (including the certified reference material). Plot the difference between each pair of analyses on a range control chart (see SOP 22). Expect a standard deviation on the order of 0.5 μmol kg-soln^{-1}.

8.2 Instrument calibration

Ensure that the calibrations of the various instruments used in this procedure are confirmed at least once a year, though the effects of sudden changes should show up on the control charts described above.

9. Bibliography

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Dickson, A.G., Afghan, J.D. and Anderson, G.C. 2003. Reference materials for oceanic CO_2 analysis: a method for the certification of total alkalinity. *Mar. Chem.* **80**: 185–197.

Gran, G. 1952. Determination of the equivalence point in potentiometric titrations. Part II. *Analyst* **77**: 661–670.

Jones, F.E. and Harris, G.L. 1992. ITS-90 density of water formulation for volumetric standards calibration. *J. Res. Natl. Inst. Stand. Technol.* **97**: 335–340.

[14] Suitable reference materials are available from Dr. Andrew G. Dickson, Marine Physical Laboratory, Scripps Institution of Oceanography, University of California, San Diego, 9500 Gilman Drive, La Jolla, CA 92093-0244, U.S.A. (fax: 1-858-822-2919; e-mail: co2crms@ucsd.edu).

[15] If the analyses on a particular day are problematic, the electrode behavior is the usual suspect.

Annexe

Dosimat® burette calibration procedure

1. Scope and field of application

The goal of this procedure is to calibrate a Metrohm Dosimat® burette accurately so that it can be used in the open-cell, alkalinity titration procedure (see procedure).

2. Principle

The burette is filled with deionized water whose temperature is equilibrated to that of the surrounding room and measured accurately. Aliquots of the water are dispensed into pre-weighed vials that are capped and reweighed. The true volumes dispensed are then calculated from a knowledge of the density of the deionized water and a "calibration function" is prepared for the burette under consideration.

3. Apparatus

- Metrohm Dosimat® burette base unit,
- Metrohm Dosimat® exchangeable burette (5 cm^3 capacity),
- 15 × 5 cm^3 capacity screw-capped glass bottles[16],
- Analytical balance readable to 0.0001 g,
- Calibrated thermometer readable to 0.1°C,
- Waste container.

4. Reagents

- Deionized water (Milli-Q® quality).

5. Procedure

5.1 Fill the Dosimat® reservoir with deionized water and allow to equilibrate to room temperature.

[16] Although glass containers are superior, excellent results can be obtained with plastic containers provided that appropriate anti-static precautions are taken when weighing.

5.2 Assemble the Dosimat® as usual except remove the anti-diffusion portion of the dispensing tip.

5.3 Submerge the thermometer in a reservoir bottle.

5.4 Fill and empty the Dosimat® burette several times; check to be sure that there are no bubbles in the burette and delivery tubing.

5.5 Weigh a dry, screw-capped glass bottle.

5.6 Dispense the water in the burette into a waste container. Make sure that the delivery tip is below the surface of the water. After dispensing, slowly withdraw the tip from the water.

5.7 Record the temperature as burette refills.

5.8 Dispense between 0.05 and 5.00 cm^3 of water into a weighed glass bottle[17]. Ensure that the delivery tip is immersed in dispensed solution.

5.9 Withdraw the tip slowly, cap the bottle and reweigh.

5.10 Repeat, varying the amount of water dispensed; repeat the measurement at least twice for each volume dispensed.

6. Calculation and expression of results

6.1 Principle

Compute the weight of the water delivered from the difference between the filled and empty container volumes:

$$w(\mathrm{H_2O}) = w(\text{filled container}) - w(\text{empty container})\,. \tag{16}$$

Compute the mass of water contained, correcting for air buoyancy (see SOP 21):

$$m(\mathrm{H_2O}) = w(\mathrm{H_2O})\left[1 + 0.0012\left(\frac{1}{\rho(\mathrm{H_2O}, t)} - \frac{1}{\rho(\text{weights})}\right)\right]. \tag{17}$$

The volume dispensed at the temperature noted (t) is

$$V(t) = m(\mathrm{H_2O}) / \rho(\mathrm{H_2O}, t)\,. \tag{18}$$

The density of air-saturated water in the temperature range 5 to 40°C is given by the expression (Jones and Harris, 1992)

$$\begin{aligned}\rho_W / (\mathrm{kg\ m^{-3}}) = {} & 999.84847 + 6.337563\times10^{-2}(t/°\mathrm{C}) \\ & - 8.523829\times10^{-3}(t/°\mathrm{C})^2 + 6.943248\times10^{-5}(t/°\mathrm{C})^3 \\ & - 3.821216\times10^{-7}(t/°\mathrm{C})^4\end{aligned} \tag{19}$$

where t is the temperature on ITS 90[18]. To achieve an accuracy of 1 part in 10^4, t must be known to within 0.5°C.

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[17] This procedure is designed to provide a series of calibration points corresponding to dispensing from 0.000 cm^3 on the burette.

[18] The distinction between the temperature scales ITS90 and IPTS68 is not important for this procedure.

The volumes measured are then compared to the nominal volumes indicated by the burette display so as to develop a "calibration function" for the particular burette system being calibrated.

6.2 Sample calculation

The following table contains a set of calibration results for a Metrohm Dosimat® system used in our laboratory.

Table 1 Calibration results for titration system 1 (December 12, 1996).

Nominal volume, V^* / cm^3	Dispensing temperature, t / °C	Weight dispensed, w / g	Volume dispensed, V / cm^3	Volume correction, ΔV / cm^3
1.000	20.9	0.9971	1.0001	0.0001
1.000	20.9	0.9957	0.9987	–0.0013
1.000	20.9	0.9971	1.0001	0.0001
2.000	20.9	1.9936	1.9997	–0.0003
2.000	20.9	1.9937	1.9998	–0.0002
3.000	20.9	2.9906	2.9997	–0.0003
3.000	21.0	2.9915	3.0007	0.0007
3.000	21.1	2.9912	3.0004	0.0004
4.000	21.1	3.9865	3.9988	–0.0012
4.000	21.1	3.9877	4.0000	0.0000
4.000	21.1	3.9877	4.0000	0.0000
4.000	21.2	3.9872	3.9996	–0.0004
5.000	21.2	4.9833	4.9988	–0.0012
5.000	21.3	4.9834	4.9990	–0.0010
3.050	21.3	3.0400	3.0495	–0.0005
0.050	21.3	0.0511	0.0513	0.0013
0.050	21.4	0.0499	0.0501	0.0001

The measured values of ΔV obtained are plotted against the nominal volume (see Figure 2)*, and* are fitted to provide a "calibration" function—typically a polynomial in V(nominal):

$$V = V^* [1 + aV^* + b(V^*)^2] . \quad (20)$$

For the measurements given in Table 1, and shown in Figure 2, the calibration function is not significantly different from

$$V = V^* , \quad (21)$$

which is the function that is used for this burette. The volume uncertainty at any point in this calibration is ± 0.0007 cm^3 (r.m.s. deviation).

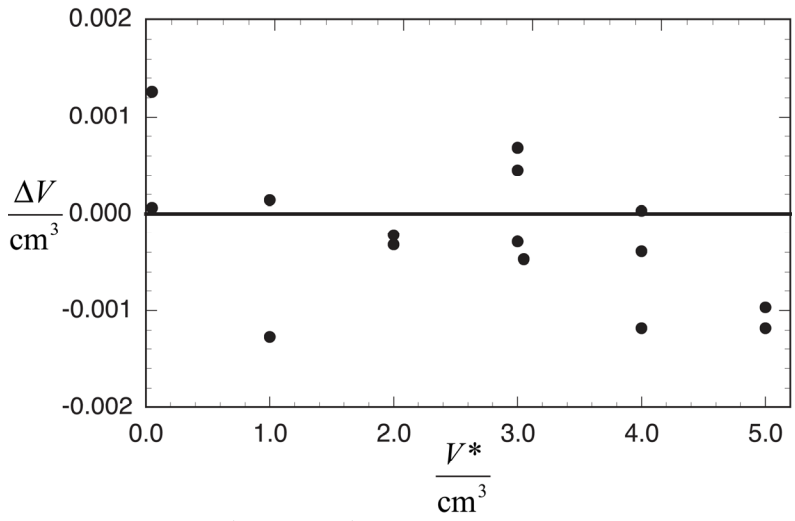

Fig. 2 Plot of $\Delta V = V - V^*$ against V^* for the calibration results for titration system 1 (December 12, 1996).

7. Quality Assurance

It is essential to identify a complete burette system as a coherent unit for the purpose of calibration and subsequent use. If it is necessary to change any of the parts (particularly the burette assembly or the base unit), it is essential to recalibrate the burette.

A new burette system should be calibrated a number of times initially to ensure that the calibration is stable. After that, it should be recalibrated yearly (or if a possible problem is identified).

SOP 4

Determination of $p(CO_2)$ in air that is in equilibrium with a discrete sample of sea water

1. Scope and field of application

This procedure describes a method for the determination of the partial pressure of carbon dioxide in air that is in equilibrium with a discrete sample of sea water. The partial pressure of carbon dioxide is expressed in microatmospheres. The method determines the dry mole fraction of air in equilibrium with oceanic water samples (250–2000 μatm at 20°C).

2. Definition

The partial pressure of carbon dioxide in air that is in equilibrium with a sample of sea water is defined as the product of the mole fraction of CO_2 in the equilibrated gas phase and the total pressure of equilibration:

$$p(\mathrm{CO_2}) = x(\mathrm{CO_2}) \cdot p \,. \tag{1}$$

The partial pressure of CO_2 is a temperature-dependent property of the sea water sample; thus it is important to record the temperature at equilibrium.

3. Principle

A known amount of sea water is isolated in a closed system containing a small known volume of air (containing a known initial amount of carbon dioxide) and maintained at a constant, known temperature and pressure. Once the water and air are in equilibrium[1] a sample of the air is analyzed for carbon dioxide content using a gas chromatograph or infrared CO_2 detector which is capable of integrating a constant volume of CO_2.[2] The partial pressure, $p(CO_2)$, is calculated from (1).

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[1] Typically the gas and liquid phases are mixed thoroughly to speed this process up. The approach commonly used is to recirculate the air through a frit immersed in the sea water sample. The circulation of small air bubbles through the volume of water acts to not only equilibrate the water, but also stir it. The frit should be close to the surface.

[2] A non-dispersive infrared detector can also be used to quantify the amount of CO_2 and can be used to assess the rate of approach to equilibrium (see *e.g.*, Wanninkhof and Thoning, 1993). However, such a detector requires a larger air/water ratio—and thus

4. Apparatus[3]

4.1 Gas analyzer system

There are several ways to measure equilibrated headspace gas. This procedure focuses on the measurement of a constant volume of headspace gas which, once equilibrated with the sample water, is carried with CO_2-free gas (for flame ionization detection the carrier gas will need to be hydrocarbon free N_2).

4.1.1 Gas analyzer that is capable of accurately integrating the total amount of CO_2 in a sample loop

For best results using a gas chromatographic technique, the following are recommended:

- A 2.0 m chromatographic column and 0.2 m precolumn packed with porous polystyrene (60–80 mesh) (Chromosorb 102 or Porapak Q);
- A catalytic system to convert carbon dioxide to methane (Ruthenium on Chromosorb W support);
- A flame-ionization detector for methane quantification.

4.1.2 Computer-controlled 10-port 2-position valve with two 1 cm^3 sample loops for sample injection and column switching

This 10-port, 2-position valve should be contained in a temperature controlled box so that loops with known volume can be carefully temperature controlled and monitored. In this configuration one loop will always have the carrier gas flowing through it while the other loop will be in line with a selected sample equilibrator. Before the valve is switched, the flow of sample headspace gas must stop to allow the sample to be pressure and temperature equilibrated with the temperature controlled system.

4.1.3 Analog to digital integrator

Unless one can ensure that there is a predictable relationship between CO_2 concentration and the peak height of CO_2 passing through the analyzer, it is important to integrate the full area under the curve to account for peak broadening and carrier gas flow rate changes.

4.2 CO_2 equilibration system

The ideal equilibration system will be contained in a single temperature controlled water bath in close proximity to the selection valve and CO_2 gas analyzer to ensure minimal length of tubing in which the sample will be circulated. To avoid transferring samples from one container to another, each

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involves a larger and less reliable correction for CO_2 exchange (see section 8.2)— also infrared detectors are non-linear and thus require more elaborate calibration for use over such a wide range of CO_2 concentrations. In addition, it is important to take account of the effect of H_2O vapor on the infrared performance of the instrument.

[3] The system described here is based on that used at the Lamont-Doherty Earth Observatory. A schematic diagram of that apparatus is provided in the Annexe to this procedure.

sample will be analyzed in the same sample container that it was collected. This can be done by recirculating headspace through a 0.5 L sample using a small air pump.

4.2.1 Constant-temperature bath

Because the partial pressure of CO_2 has a large sensitivity to changes in temperature, it is necessary to control the temperature and measure sample water temperature to less than 0.05 K at hourly time intervals. Because it may take up to an hour for the sample temperature to reach the bath temperature, and the air pumps used to circulate headspace air through the sample container are a source of heat, care must be taken to measure and record the sample temperature directly. Alternatively, with a good understanding of the temperature equilibration time of your system and the offset between bath temperature and sample temperature, given a typical air flow through the sample flask, corrections can be derived.

4.2.2 Air pumps for re-circulating headspace gas

It is important that the air pump does not pump more than 1.0 L min^{-1} at full speed and that the pump speed can be controlled to reduce the amount of aerosols and heat that are circulated through the headspace plumbing.

4.2.3 Thermometer (± 0.02°C)

Accurate temperature measurements are essential and should be recorded continuously throughout the measurement period.

4.2.4 Borosilicate glass flask (0.5 L) with 0.10 m extensions or long-neck sampling flasks (e.g., volumetric flask)

To provide adequate room for bubbles and froth from incoming air rising up through the sample, it is useful to have a long neck or extension on the sampling bottle. It should also be noted that the thinner walled flasks will equilibrate with the thermostat bath more quickly.

4.2.5 Three-hole stopper, nylon tubing and frit to carry headspace gas through equilibrators

The equilibration is done in a closed loop by pushing air from the pump to just below the water level of each sample flask through a nylon tube and frit. Air passes out of the sample cell through a second nylon tube flush with the stopper. A third tube provides an opening to ensure that the samples are at ambient pressure. The longer the tube, the less likely it is that the headspace will be contaminated by room air. A net flow of gas into or out of the third opening is an indication of a leak in the system.

4.2.6 0.5 μm syringe filters

Filters are used to capture aerosols and water droplets on the downstream side of the equilibrator.

4.3 Calibration system

- Remotely operated valve allowing selection between the three calibration gases,
- Normally closed solenoid shut-off valve used to control the flow of calibration gas,
- Barometer, accurate to ± 50 Pa (0.5 mbar), with computer interface.

4.4 System control

- Microcomputer for data logging,
- Digital interface board to control valves, *etc*.

5. Reagents

5.1 Compressed gases

- Carrier gas: hydrocarbon-free nitrogen,
- FID gases: hydrocarbon-free hydrogen (*e.g.*, from a hydrogen generator) and air (*e.g.*, from a pure air generator),
- Three calibration gas mixtures of CO_2 in air: well-known CO_2 concentrations chosen to span the range of measured values: $x(CO_2) = 250–2000 \times 10^{-6}$.

6. Sampling

It is essential that samples are collected, poisoned and stored according to the procedure detailed in SOP 1. However, for this analysis the sample bottles are 500 cm^3 volumetric flasks. Samples are equilibrated in the same bottles in which they are collected, eliminating one transfer operation.

7. Procedure

7.1 Introduction

This procedure has been designed to maximize the sample analysis while accounting for drifts in the system and allowing for both temperature and head space equilibration of CO_2 in each sample. The normal sequence of analysis accounts for changes in the response of the detector with time by running a set of standards (typically three) through the analyzer before and after a set of four samples has been run. To ensure full air–water equilibration of CO_2 in headspace volumes of ~ 0.04 L with 0.5 L of sea water with flow rates of ~ 0.2 L min^{-1}, it is necessary to circulate the air for 8 minutes. In extreme conditions, it may take an hour to equilibrate sample temperatures to bath temperatures. To ensure temperature equilibration, samples should be stored near measurement temperatures, and the sample in the temperature-controlled bath replaced immediately after the previous sample has been analyzed.

7.2 System start-up

To begin a sample analysis run it is important to ensure that the system is stable. To save standards it is possible to run laboratory air samples as follows:

7.2.1 Disconnect the lines leading to and from the equilibrators, so that the pumps will fill the sample loop with ambient air rather than equilibrated air.

7.2.2 Run these analyses without the use of calibration gases, thus conserving the calibration gases (this can be achieved by using a separate subroutine in the operating program).

Calculation of $p(CO_2)$ for a set of samples requires knowledge of the concentration of CO_2 in the headspace gas prior to starting the equilibration. This is estimated—in part—from the $p(CO_2)$ of the previous sample analysis. Thus, after reconnecting the lines to the equilibrators (see above), analyze two dummy (or practice) samples prior to running the main suite of analyses. Subsequently, the final samples from an analysis session can be left in place until the next set of analyses begins (see section 7.5).

7.3 Loading of new samples

As each sample analysis is completed (see section 7.4), replace the previous sample flask with a fresh sample as described below. The immediate replacement of a recently analyzed sample will ensure that the headspace has a known CO_2 concentration at the start of the equilibration time period.

7.3.1 Bring the next sample to the equilibration temperature prior to analysis (*e.g.*, by placing it in the same thermostat bath used to maintain the analysis temperature). As mentioned above, it is important to pre-equilibrate the sample temperature to ensure that the sample is at the thermostat bath temperature when the headspace gas is analyzed.

7.3.2 Turn off the recirculation pump for the equilibrator. This minimizes the exchange of laboratory air with the air currently in the pump and tubing, and prevents sample water from being forced into the return line leading to the gas analyzer.

7.3.3 Open the drain valve for the equilibrator and insert the stopper with gas disperser, return line and drain line into the next sample flask (see diagram).

7.3.4 Force sample water out from the flask through the drain line using air of known CO_2 concentration admitted to the flask through the return line.

7.3.5 Stop the flow of air once the water level reaches the bottom end of the drain tube and close the drain valve.

7.3.6 Turn the recirculation air pump back on.

7.4 Equilibration of sample

Full equilibration with the headspace can take as long as 8 minutes, depending on the total headspace and loop size. It is therefore necessary to ensure that air being captured in the sample gas loop has circulated for an adequate amount of time before capturing the sample and moving on to the next sample.

7.5 Acceptance criterion

Analyze each sample in duplicate (two consecutive equilibrations of the same water sample). Compare the integrated detector peak areas for the CO_2 from the two analyses; if the difference between the two areas is less than 0.25% of the mean of the two areas, accept the results and replace the sample flask by a fresh sample, as described in section 7.3.

If the two analyses differ by more than this amount, do not replace the flask, but re-analyze it as part of the next sequence. After any sample has been analyzed a third and fourth time, it is replaced whether or not it has attained the acceptance criterion.

Repeated failure of samples to attain this criterion on a particular equilibrator suggests that is necessary to clean the system, as aerosol particles of salt or water may be restricting the air flows or interfering with the action of the recirculation pump.

7.6 Termination of analytical session

Following the analysis of the final samples of a given session (including the final set of calibration analyses), the two flasks are left in place connected to the two equilibrators. This serves to prevent drying of the gas dispersers and to provide start-up samples to establish the concentration of CO_2 in the pumps and gas lines before the analysis of fresh samples. In addition, use of such samples—with known $p(CO_2)$—provides a check on the system prior to the analysis of fresh samples.

8. Calculation and expression of results

8.1 Calculation of gas chromatograph response

The response of a flame ionization detector is almost linear over a large dynamic range. However, the response varies with changes in ambient temperature and with the flow rates of the hydrogen and oxygen reaching the flame. A quadratic curve will fit the actual response closely at any given time. With an infrared analyzer, which is not as linear, it will be necessary to run more than three standards to reduce the potential errors for concentrations not well represented by standards.

The detector peak area (A_x) corresponds to the dry CO_2 content—$x(CO_2)$—of each of the three calibration gases. The peak area is linearly interpolated in time

between a pair of measurements (made at times t_1 and t_2) to estimate the response of the system at the time (t) of measurement of each unknown:

$$A_x(t) = A_x(t_1) + \frac{t - t_1}{t_2 - t_1}[A_x(t_2) - A_x(t_1)]. \quad (2)$$

A separate response curve of peak area versus concentration is then calculated at the time of measurement of each unknown (t):

$$x(\mathrm{CO}_2) \cdot p = a_0 + a_1 \cdot A_x(t) + a_2 \cdot [A_x(t)]^2 \quad (3)$$

where p is the measured atmospheric pressure[4].

8.2 Corrections for sample perturbation during equilibration

Some CO_2 will be exchanged between the sea water sample and the air of the headspace during the process of equilibration. This process will alter the total dissolved inorganic carbon (C_T) in the sea water sample while leaving the total alkalinity (A_T) constant. The measured partial pressure will be in equilibrium with this modified sample. A mass balance approach is used to estimate the partial pressure of carbon dioxide in air that would have been in equilibrium with the original, unchanged sample. Although it is useful to have measurements of C_T, rough estimates will suffice for this calculation.

8.2.1 Calculation of ΔC_T

The change in the number of moles of CO_2—$\Delta n(CO_2)$—in the equilibrator headspace can be calculated (assuming ideal behavior),

$$\Delta n(\mathrm{CO}_2) = \frac{[p(\mathrm{CO}_2)_1 - p(\mathrm{CO}_2)_2]V_H}{RT} \quad (4)$$

where V_H is the volume of air in the headspace and the subscripts 1 and 2 refer to values measured before and after the equilibration process, respectively. Note that the temperature of the system and the headspace volume are assumed to remain constant throughout. The change in C_T can then be calculated,

$$\Delta C_T = \frac{\Delta n(\mathrm{CO}_2)}{\rho \cdot V_S} \quad (5)$$

where V_S is the volume of sea water of density ρ that was equilibrated with the headspace gas.

8.2.2 Calculation of corrected $p(CO_2)$

If the C_T of the unperturbed sample is known:

[4] The pressure in the loop is controlled at atmospheric pressure which is measured at the time of injection. The calibration gases are vented directly to the atmosphere to achieve this; air in equilibrium with the sample is in pressure equilibrium with the atmosphere through a flexible rubber diaphragm. Thus, the measured response curve relates partial pressure of CO_2 (rather than concentration) to peak area.

- Calculate the C_T of the perturbed water sample and use this together with $p(CO_2)$ to calculate the value of A_T for the sea water sample (see Annexe to Chapter 2)[5]. The equilibrium constants used should be appropriate to the equilibration temperature and the salinity of the sample being equilibrated[6].
- Calculate $p(CO_2)$ ($\approx f(CO_2)$) for the unperturbed sea water from the knowledge of A_T and C_T (see Annexe to Chapter 2).

If the A_T of the original sample is known:

- Use $p(CO_2)$ together with A_T to calculate the C_T of the perturbed water sample (see Annexe to Chapter 2)[5]. The equilibrium constants used should be appropriate to the equilibration temperature and the salinity of the sample being equilibrated[6].
- Use equation (5) to estimate C_T in the unperturbed sample.
- Calculate $p(CO_2)$ ($\approx f(CO_2)$) for the unperturbed sea water from the knowledge of A_T and C_T (see Annexe to Chapter 2).

8.3 Correction for water vapor pressure

If the equilibrated air is injected into the gas chromatograph without removal of water vapor, the calculation outlined in section 8.2 will give the final value of $p(CO_2)$ at equilibration pressure.

If water vapor was removed from the equilibrated air prior to injection into the gas chromatograph, it is necessary to correct for this. The partial pressure of CO_2 in the dried air must be reduced by a factor which accounts for the increase in concentration of CO_2 in the air resulting from the removal of the water vapor.

$$p(CO_2) = p(CO_2 \text{ in dry air}) \times [1 - p_\sigma(H_2O)] \quad (6)$$

where $p_\sigma(H_2O)$ is the water vapor pressure over a sea water sample of a given salinity at the temperature of equilibration[7]—see Chapter 5, section 3.

8.4 Calculation of $f(CO_2)$ from corrected $p(CO_2)$

See SOP 24.

8.5 Example calculation

Flask volume = 525 cm^3,
Flask headspace = 45 cm^3,
Residual system volume (lines and pump) = 13 cm^3,

[5] If desired it can be assumed that $f(CO_2) \approx p(CO_2)$ for this calculation. Assuming that CO_2 behaves ideally will not make a significant difference to the final result as long as the same assumption is made in both the forward and back calculations.

[6] As the same equilibrium constants (see Chapter 5) are used for the forward and back calculations, errors due to uncertainties in these will be small.

[7] Equation (6) assumes that the water vapor behaves ideally.

Fill gas (used to displace headspace), $x(CO_2) = 750 \times 10^{-6}$,
Residual gas (lines and pump), $x(CO_2) = 535 \times 10^{-6}$,
Temperature of gas in headspace = 25°C,
Salinity of sample = 35,
C_T of sample (before equilibration) = 2050 μmol kg-soln^{-1},
Equilibration pressure = 995 mbar (99.5 kPa),
Equilibration temperature = 20°C,
Measured $x(CO_2)$ for sample = 350×10^{-6}.

From equation (4), for the headspace,

$$\Delta n(CO_2) = \frac{(750\times10^{-6} - 350\times10^{-6})\times 45\times10^{-6}\times 99500}{8.31447\times 298.15}$$
$$= 7.225\times10^{-7}\,\text{mol},$$

and for the residual gas in the lines and pump,

$$\Delta n(CO_2) = \frac{(535\times10^{-6} - 350\times10^{-6})\times 13\times10^{-6}\times 99500}{8.31447\times 298.15}$$
$$= 9.653\times10^{-8}\,\text{mol}.$$

Then at $S = 35$ and $T = 20$°C, $\rho_{SW} = 1024.76$ kg m^{-3} and from equation (5)

$$\Delta C_T = \frac{7.225\times10^{-7} + 9.653\times10^{-8}}{1024.76\times(525-45)\times10^{-6}} = 1.665\times10^{-6}\,\text{mol kg}^{-1},$$

thus

C_T (after equilibration) = 2050 + 1.665 = 2051.67 μmol kg^{-1}.

Total alkalinity (A_T) in the sample is calculated from this together with the post-equilibration values of $p(CO_2)$ (see Footnote 5).

As $p(CO_2) = (350 \times 10^{-6}) \times (99.5/101.325) = 343.7$ μatm and $C_T = 2051.67$ μmol kg^{-1}, using the equations in the Annexe to Chapter 2 together with the thermodynamic data in Chapter 5[8],

$A_T = 2348.21$ μmol kg^{-1}.

The $p(CO_2)$ of the sample before equilibration is then estimated from this value for A_T and $C_T = 2050$ μmol kg^{-1} (again, using the equations in the Annexe to Chapter 2 together with the thermodynamic data in Chapter 5) to give

$p(CO_2) = 341.0$ μatm.

9. Quality assurance

For general principles of analytical quality control see Chapter 3.

[8] If $f(CO_2)$ is assumed ≈ $p(CO_2)$, the calculated $A_T = 2347.35$ μmol kg^{-1}.

9.1 Stability of the response of the gas chromatograph

The performance of the gas chromatograph can be monitored by means of control charts (SOP 22) which give a visual indication of any significant change in the response of the instrument to injections of nearly constant amounts of CO_2 calibration gases.

The absolute peak areas for the three calibration gases (normalized to a constant pressure and temperature) should be plotted against time and deviations of more than 2% should be investigated. As a rapid check on the functioning of the instrument, the values of the response function coefficients a_0, a_1, and a_2 can be printed with the calculated value of $p(CO_2)$ for each analysis.

9.2 Reproducibility of equilibrated samples

Replicate samples should agree within 0.25% (see section 7.5); this test will give a rapid indication of deteriorating performance of the equilibration system. The fraction of analyses from each analytical session that fails to meet the criterion should be entered on a control chart, and any significant increase in these fractions investigated. As a further check on the functioning of the two equilibrators of the system, occasional duplicate samples should be taken from the same water sampler and run as a pair on the two equilibrators. Differences of greater than 0.5% in the corrected values should be cause for concern.

10. Bibliography

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Wanninkhof, R. and Thoning, K. 1993. Measurement of fugacity of CO_2 in surface water using continuous and discrete methods. *Mar. Chem.* **44**: 189–204.

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Annexe

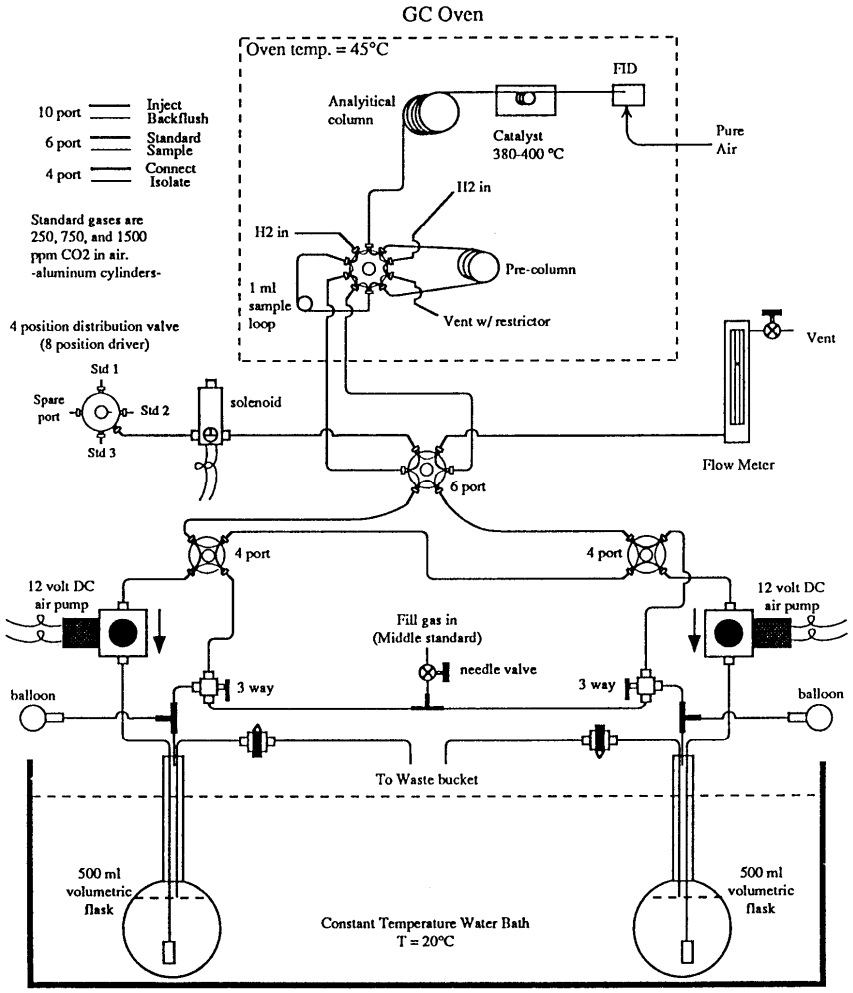

Fig. 1 Schematic showing the gas–water equilibrator and gas chromatographic system for the equilibration of $p(CO_2)$ in discrete samples (Chipman *et al.*, 1992).

SOP 5

Determination of $p(CO_2)$ in air that is in equilibrium with a continuous stream of sea water

1. Scope and field of application

This procedure describes a method for the determination of the partial pressure of carbon dioxide in air that is in equilibrium with a flowing stream of sea water, *e.g.*, that obtained by pumping surface sea water from the bow of a ship for underway analysis. The partial pressure of carbon dioxide is expressed as microatmospheres. The method is suitable for the assay of air in equilibrium with oceanic water samples (250–550 μatm).

2. Definition

The partial pressure of carbon dioxide in air that is in equilibrium with a sample of sea water is defined as the product of the mole fraction of CO_2, $x(CO_2)$, in the equilibrated gas phase and the total pressure (p) of equilibration:

$$p(CO_2) = x(CO_2) \cdot p \; . \tag{1}$$

It is a temperature-dependent property of the sea water sample; thus it is important to record the *in situ* water temperature as well as the water temperature in the equilibrator at the time of measurement.

3. Principle

A fixed volume of air is equilibrated with a stream of sea water that flows through an equilibrator[1]. As the volume of sea water that flows through the equilibrator is essentially infinite compared to the volume of air, the CO_2 content of the air adjusts to equilibrium with the sea water without altering the CO_2 content of the sea water appreciably. The air is circulated through a non-

[1] A number of effective designs exist for such an equilibrator. The most common is that designed by Dr. Ray Weiss at the Scripps Institution of Oceanography and described in a report by Butler *et al.* (1988). The apparatus described in this SOP also uses a rain type equilibrator, but it has approximately one tenth of the volume (~1.3 dm^3) of the original Weiss design.

dispersive infra-red analyzer to measure its CO_2 content[2]. The analyzer is calibrated using gases of known CO_2 concentration (mole fraction).

The partial pressure, $p(CO_2)$, is then calculated from (1). To use this measurement together with other parameters of the carbon dioxide system in sea water, it is necessary to convert the mole fraction to fugacity, $f(CO_2)$, to account for the fact that CO_2 does not strictly follow Henry's Law for ideal gases:

$$f(\mathrm{CO_2}) = x(\mathrm{CO_2})\frac{p}{RT}\exp\left(\int_0^p V(\mathrm{CO_2}) - RT/p'\,dp'\right) \qquad (2)$$

(see Chapter 2). The calculations required are outlined in SOP 24.

4. Apparatus

The apparatus described here is intended to serve as an example of a commonly used system. It is based on a standardized design that is currently used on over a dozen ships at the time of writing[3]. Some of the details of flow rates and timing are "tuned" to this system and may need to be adjusted for systems with different components.

4.1 Outside air intake

A tube, typically Synflex® (formerly Dekoron®) type "1300", is run from the measurement system to a location where uncontaminated outside air can be sampled. If the measurement system is located on board a ship, this line will typically be led to the bow of the ship[4]. The air is continually pumped at a rate of 2–3 $dm^3\ min^{-1}$ to ensure constant flushing of the tubing. During sampling, a fraction (60–80 $cm^3\ min^{-1}$) of the air stream is diverted through a dryer to the analyzer.

4.2 Equilibrator

The most common type of equilibrator involves a chamber where sea water is exposed to a headspace of air maintained at the ambient atmospheric pressure[5].

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[2] A gas chromatographic system can be used successfully for this measurement (see *e.g.*, Weiss, 1981; Weiss *et al.,* 1982; Robertson *et al.,* 1993; Weiss *et al.*, 1992). Although the gas chromatograph approach has a number of advantages in that it requires smaller amounts of both sample and calibration gas and is not sensitive to the O_2/N_2 ratio of the gas being measured, the infrared approach is recommended here as being potentially more rugged and simpler to implement.

[3] A schematic of the layout described here is given in the Annexe to this procedure.

[4] It is important to record the relative wind speed and direction to confirm that the air being sampled represents uncontaminated marine air and does not contain any stack gas from the ship. Some investigators have reported that they believe that this air intake line can, in time, become contaminated with sea salt aerosols and then bleed CO_2 slowly into the gas stream.

[5] Some equilibrator designs (*e.g.*, bubble or membrane type equilibrators) equilibrate at pressures different from ambient atmospheric pressure. These systems either need to

Rapid exchange of CO_2 is facilitated by enhancing the surface area of water exposed to the headspace air (*e.g.*, raining sea water droplets through the headspace into a sea water reservoir at the bottom of the equilibrator). The water flow rate is 2–5 dm^3 min^{-1} and can be dispersed using a standard gardening spray head. The sea water is removed from the reservoir using a gravity drain and a series of water traps to minimize air exchange between the lab and the equilibrator headspace. Ambient air pressure is maintained in the headspace with a vent tube that is open to the outside air. The vent tube should have a volume of at least 10% of the headspace volume so small high-frequency pressure fluctuations just move the headspace air in and out of the vent tube but do not draw in outside air. This can be accomplished by attaching a long tube to the vent that extends outside the ship. This also provides fresh air for the headspace rather than high-CO_2 lab air. A better option for ensuring that the uptake of air through the vent line does not significantly affect the headspace gas is to include a pre-equilibration chamber on the vent line. This is particularly important for equilibrators with a small headspace volume (< 2 dm^3). The pre-equilibration chamber is a small chamber with sea water raining through it so any air brought into the headspace is already close to equilibrium with the sea water. During sampling, the headspace air is pumped through a dryer and the infrared detector at a rate of 60–80 cm^3 min^{-1}. After passing through the detector, the equilibrated air is returned to the headspace to minimize the need for replacement air from the vent. It is important to keep track of temperature and pressure in the equilibrator at all times.

4.3 Drying system

It is desirable to dry all of the air streams going to the detector[6]. The drying system should be placed on the low-pressure side of any pump. Drying the air eliminates the possibility of condensation in the tubing leading to the analyzer; it also improves the sensitivity and the accuracy of the infrared analysis as it eliminates the need to correct for the pressure broadening of the CO_2 band resulting from the presence of water. Also, the calibration gases are typically dry air, so it is preferable to also analyze the unknown samples under the same dry air conditions.

A number of approaches can be used to dry the air:

- Cooling the air to a specified dew point using a refrigeration unit (*e.g.*, Peltier cooler). This necessitates emptying the traps of the accumulated water (or ice) on a regular basis.
- Using a chemical drying agent, *e.g.*, Aquasorb®—a solid support impregnated with P_2O_5 and containing a colored indicator (dew point –96°C). This drying agent will need to be replaced on a regular basis.
- Passing the wet sample gas through water permeable tubing (*e.g.*, Nafion®) with drying gas on the outside of the tubing to carry away the water vapor

use a second-stage equilibrator maintained at ambient pressure or apply a pressure correction term to adjust the values to ambient conditions.

[6] Some systems do not dry the gas streams. Instead, they use a two-channel infrared detector (*e.g.*, the LI-COR® Model 7000) to measure both the water and CO_2 content, then correct for the water vapor in the final calculations. The advantage of these systems is the elimination of a complicated and potentially labor-intensive gas drying procedure.

and maintain a humidity gradient between the inside and the outside of the tubing.

The system described here combines a Peltier cooler and Nafion® tubing to dry the gases, but the analyses are made with a LI-COR® analyzer containing a water channel to ensure a complete accounting of any remaining water vapor.

4.4 Calibration system

Because the infrared detector has a non-linear response to changing CO_2 concentrations, it is recommended that multiple standards (3–6) be analyzed for the most accurate characterization of the response curve. Depending on whether the analyzer is run in absolute mode (*i.e.*, the reference cell is circulated with a closed loop of zero CO_2 air) or in differential mode (*i.e.*, the reference cell is flushed with a known standard gas), it may be desirable to run the reference gas through the sample cell to "zero" the instrument. High-purity two-stage gas cylinder pressure regulators are needed for each of the standard gases, as well as a remotely operable valve for selecting between the different gas sources.

4.5 Detector system

High quality infrared detectors can be purchased commercially. For operation on a ship, it is essential that the instrument not be sensitive to motion or vibration[7]. It is important to keep track of the temperature and pressure of the gas in the infrared absorption cells at the time of the measurements. If a water vapor correction is to be applied, then a detector with a water channel must be used.

4.6 System control

Since the system is intended to operate in "underway" mode, there should be a program for autonomously controlling valve switching, monitoring flow rates and logging the necessary data. This program will require a microcomputer as well as digital and analog interface boards for controlling valves, solenoids and necessary sensors.

5. Reagents

5.1 Compressed gases

The standards should be mixtures of CO_2 in natural air (*i.e.*, containing N_2, O_2, and trace gases) that bracket the expected concentrations of the samples as closely as possible (typically 250–550 × 10^{-6} for open ocean applications). CO_2 concentrations have been found to be most stable in aluminum cylinders. The gases must be calibrated to better than the desired accuracy of the final measurements (*i.e.*, typically beyond the accuracy offered by commercial gas suppliers) and should be traceable to the World Meteorological Organization scale.

[7] Suitable instruments are available from LI-COR Environmental, 4647 Superior Street, P.O. Box 4425, Lincoln, NE 68504-0425, U.S.A.

5.2 Drying agents

Chemical drying agents are the most reliable way to ensure that the sample gas is dry. Even if condensing systems or drying tubes are used to primarily dry the gas, many systems also run the sample gas through a chemical drying agent as a final confirmation that the sample is dry. Some common drying agents are Aquasorb®, magnesium perchlorate or silica gel.

6. Sampling

As this procedure is for underway measurements, the sampling is done as part of the analysis. The important features are to ensure that the air line samples uncontaminated marine air (see section 4.1) and that the equilibrator samples uncontaminated surface sea water. As the $p(CO_2)$ is very dependent on the water temperature, it is important that the water in the equilibrator be as close to sea surface temperature as possible. One should strive to set the system up in such a way that the difference in the temperature observed in the equilibrator and that observed in the surrounding sea water is less than 0.5°C. This is achieved by using a high flow rate of sea water to reduce the extent of the inevitable warming or cooling that occurs during passage from the water intake to the equilibrator. It is important to record the water intake temperature and salinity, *e.g.*, using a thermosalinograph system as well as the equilibrator temperature. The sea water temperature should be monitored with a sensor in the equilibrator and a sensor at the ship's sea water intake (outboard of any pumps or flow restrictors) so any temperature differences can be accounted for (see section 8.3) in the data reduction sequence. Because $p(CO_2)$ is very sensitive to temperature, it is important to use high-quality sensors with confirmed accuracy by comparison with a National Institute of Standards ITS-90 traceable temperature sensor (confirmed calibration ± 0.0001 across the range)[8]. Comparison of the equilibrator and the sea surface temperature sensor readings can be done in a well stirred and insulated water bath either on the ship or in the laboratory, ideally over a range of temperatures with all sensors measuring at the same time. If the sensors vary from the traceable standard, then an offset can be applied.

7. Procedure

7.1 Introduction

The sequence of analyses outlined below is designed to measure both the marine air and the equilibrator in a cycle together with the calibration gases. The exact sequence is not critical and can be optimized for the particular location and desired objectives of the study. In general, the frequency of analysis is determined by the length-scale of the phenomena that are being observed (compared to the ship's speed), and by the desire to conserve calibration gases.

[8] To prove temperature traceability, a continuous path of calibrated measurements must be "traced" back to a fixed point of reference. This path consists of comparison measurements between "transfer standards" to ensure a temperature indication is an accurate reflection of the ITS-90 definition of temperature (see Chapter 3).

7.2 System calibration

A full set of standards should be run every 2.5 to 3 hours. Each standard takes approximately 4.5 minutes to analyze. After the gas selector valve is switched to a new standard, the system is allowed to flush through the detector for approximately 4 minutes with flow rates similar to the sample flow rates (60–80 $cm^3\ min^{-1}$). After the lines are flushed, the flow is stopped at a point before the detector (*i.e.*, the detector is still vented to the atmosphere). After a delay of 6 seconds to allow for pressure equilibration in the detector, a 1-second averaged reading is taken. The gas selector valve is then switched to the next standard.

7.3 Cycle of analyses

Once the system has been calibrated, it alternates between marine air and equilibrated air readings. In the open ocean, sea water $p(CO_2)$ generally has much larger variations than the marine air, so systems usually collect 5 to 10 times more equilibrator readings than marine air readings. Each time the gas selector valve is switched to a new gas, the air lines need to be thoroughly flushed with the new sample. After switching the gas selector valve to marine air, the detector is allowed to flush for 4 minutes. After flushing, the flow is stopped for 6 seconds and a 1-second averaged reading is taken. Flow is started again and the system is allowed to flush for 30 seconds before the flow is stopped for another reading. After 10 marine air readings are collected, the gas selector valve switches to equilibrator air and is allowed to flush for 4 minutes. After flushing, the flow is stopped for 6 seconds and the reading is taken. Flow is started again and the system is allowed to flush for 1 minute before the flow is stopped again for another reading. After 60 equilibrator readings, the system switches back to marine air. The sequence continues until it is time to standardize the system again.

8. Calculation and expression of results

8.1 Calculation of infrared detector response

The response of a non-dispersive infrared absorption detector is appreciably non-linear, even over the restricted range of CO_2 concentrations that apply here. Furthermore, the detector signal depends in part on the number of moles of CO_2 in the cell, not on the mole fraction. This is given by the gas law

$$n(\mathrm{CO_2}) = \frac{x(\mathrm{CO_2}) \cdot p \cdot V(\mathrm{cell})}{RT} \cdot \phi \tag{3}$$

where ϕ is an approximately constant term[9] that accounts for the non-ideality of the gas phase and p and T are the pressure and temperature of the gas, respectively, in the absorption cell, which has a volume V(cell)[10].

[9] Provided that the temperature, pressure and composition remain approximately constant. This is typically the case for this procedure.

[10] Absorption per mole of CO_2 also increases with pressure and it has been found empirically (LI-COR, 1992) that (at a constant temperature) the pressure affects the signal voltage in a linear fashion.

Two approaches are commonly used to evaluate the mole fraction of an unknown sample, based on standards with a known mole fraction. The first approach is based on a factory-calibrated response curve for the instrument. The LI-COR® instruments come from the factory with a built-in response function. This response function is tuned for the particular environmental conditions by setting the "zero" and "span" parameters using standard gases (see LI-COR, 1992 for details). While this approach gives reasonable values over a very wide range of conditions, more accurate values can be achieved over the limited range of conditions observed in the open ocean.

The approach described here starts with the output mole fraction determined by the internal functions provided by the LI-COR® instruments as described in the first approach, then modifies the output based on a series of calibration standards analyzed as part of the sampling sequence. This approach is recommended for those using LI-COR® instruments because:

1) the $x(CO_2)$ signal from RS-232 has better averaging (*i.e.*, the mV signal for the newer LI-COR® instruments is a converted digital signal that is not filtered or averaged);
2) the $x(CO_2)$ signal is internally corrected for band broadening;
3) the $x(CO_2)$ signal automatically takes cell pressure and temperature changes into account[11].

Ideally, the instrument should be calibrated using the built-in zero and span functions at least once at the beginning of the cruise. Additional calibrations during the cruise should be bracketed by analyses of the full set of standards to document the change in nominal $x(CO_2)$ output.

Following the analysis sequence outlined in section 7 provides nominal $x(CO_2)$ values for the unknown samples bracketed in time by the analysis of a series of known standards. The proposed measurement cycle necessarily performs the measurements on each calibration gas, and on each sample of air, at different times. To ensure the highest measurement quality, it is necessary to interpolate the measurements on calibration gases so as to infer the appropriate calibration function at the exact time of the measurement of a sample of air (either atmospheric or from the equilibrator). This is achieved using a piecewise linear interpolation in time. The measured nominal $x(CO_2)$ appropriate to a particular time t is estimated for each of the standard gases from values measured at times t_0 and t_1 that bracket time t:

$$C_0 + (C_1 - C_0)\frac{(t - t_0)}{(t_1 - t_0)}. \qquad (4)$$

C_0 is the nominal concentration of the particular standard gas measured at time t_0, and C_1 that measured at time t_1. This set of values is then used, together with the associated set of assigned $x(CO_2)$ values for the standard gases, to estimate the coefficients of a linear calibration function appropriate to time t. This information is then used to calculate the nominal value of $x(CO_2)$ for the air sample measured at time t:

[11] This requires an internal pressure transducer which some LI-COR® models may not have. In this case the pressure is a pre-set value.

$$y_s = A + Bx_s \tag{5}$$

where x_s and y_s are, respectively, the nominal value of $x(CO_2)$ for the air sample and "true" value calculated from the calibration curve, and A and B are regression coefficients determined by a linear least-squares fit of the standards.

If the partial pressure of CO_2 in dry air is required, it is necessary to multiply the corrected sample $x(CO_2)$ by the equilibrator pressure P_{eq} (the pressure at the time of equilibration):

$$p(\mathrm{CO_2})_{T_\mathrm{E},\mathrm{dry}} = x(\mathrm{CO_2}) \cdot P_{\mathrm{eq}} \tag{6}$$

where T_E is the temperature measured in the equilibrator.

8.2 Correction for water vapor pressure

Air in the equilibrator—like air at the sea surface—is assumed to be at 100% humidity. The partial pressure of CO_2 measured in dried equilibrator air must therefore be reduced by a factor which accounts for the increase in concentration of CO_2 in the air resulting from the removal of the water vapor.

Thus

$$p(\mathrm{CO_2})_{T_\mathrm{E},\mathrm{wet}} = x(\mathrm{CO_2})\left[P_{\mathrm{eq}} - VP(\mathrm{H_2O})\right] \tag{7}$$

where $VP(H_2O)$ is the water vapor pressure over a sea water sample of a given salinity at the temperature of equilibration[12]—see Chapter 5.

8.3 Calculation of $f(CO_2)$ from $p(CO_2)$

If the $p(CO_2)$ of the sea water is to be used to calculate—or compared with—the other parameters of the CO_2 system, it is necessary to calculate the fugacity, $f(CO_2)$—see SOP 24:

$$f(\mathrm{CO_2})_{T_\mathrm{E}} = p(\mathrm{CO_2})_{T_\mathrm{E},\mathrm{wet}} \cdot \exp\left[\frac{\left(B(\mathrm{CO_2})_{T_\mathrm{E}} + 2 \cdot \delta(\mathrm{CO_2})_{T_\mathrm{E}}\right) p_{\mathrm{atm}}}{R \cdot T_\mathrm{E}}\right] \tag{8}$$

where p_{atm} is the atmospheric pressure and B and δ are defined in SOP 24. The term $(x_C)^2$ is approximately equal to 1.

8.4 Correction of $f(CO_2)$ to sea surface temperature

The $f(CO_2)$ measured in the equilibrator is appropriate to the temperature of the water in the equilibrator. To use this as information about gas exchange at the sea surface, it is necessary to correct the value obtained to the measured sea surface temperature:

$$f(\mathrm{CO_2})_{T_\mathrm{S},\mathrm{wet}} = f(\mathrm{CO_2})_{T_\mathrm{S},\mathrm{wet}} \cdot \exp\left[0.0423(T_\mathrm{S} - T_\mathrm{E})\right] \tag{9}$$

[12] Equation (7) assumes that the water vapor behaves ideally.

where T_S is the sea surface temperature—typically the bulk temperature of the mixed layer[13]—and T_E is the temperature measured in the equilibrator[14].

8.5 Example calculations

8.5.1 Calibration data

The calibrated $x(CO_2)$ values for 4 standards are:

305.00, 370.00, 405.00 and 500.00 × 10^{-6}.

The measured $x(CO_2)$ values at time t_0 are:

12:05 = 305.06 × 10^{-6},
12:10 = 370.10 × 10^{-6},
12:15 = 405.21 × 10^{-6},
12:20 = 500.33 × 10^{-6}.

The measured $x(CO_2)$ values at time t_1 are:

15:05 = 305.56 × 10^{-6},
15:10 = 370.60 × 10^{-6},
15:15 = 405.71 × 10^{-6},
15:20 = 500.83 × 10^{-6}.

The interpolated $x(CO_2)$ values at 13:00 are:

$$305.06 + (305.56 - 305.06) \cdot \left(\frac{55}{180}\right) = 305.21 \times 10^{-6},$$

$$370.10 + (370.60 - 370.10) \cdot \left(\frac{50}{180}\right) = 370.24 \times 10^{-6},$$

$$405.21 + (405.71 - 405.21) \cdot \left(\frac{45}{180}\right) = 405.34 \times 10^{-6},$$

$$500.33 + (500.83 - 500.33) \cdot \left(\frac{40}{180}\right) = 500.44 \times 10^{-6}.$$

8.5.2 Correction of nominal sample value

The nominal equilibrator air $x(CO_2)$ was 378.45 × 10^{-6} at 13:00.

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[13] There is still some discussion as to whether the appropriate choice of sea surface temperature that should be used to study air–sea exchange is that measured on the ship's underway system (typically the bulk temperature of the mixed layer), or whether a "skin temperature" should be determined and used (see Robertson and Watson, 1992).

[14] The factor of 0.0423 has been determined experimentally (Takahashi *et al.*, 1993). A more elaborate correction procedure is possible (see, *e.g.*, Copin-Montegut, 1988; Goyet *et al.,* 1993); however, it is unnecessary provided that $|T_S - T_E| < 1$ K, as is the case for most measurement systems.

$A = 0.1813$, $B = 0.99876$ from linear fit,

$y_s = 0.99876 \cdot 378.45 + 0.1813 = 378.16 \times 10^{-6}$.

The final calibrated $x(CO_2)$ value is 378.16×10^{-6}.

8.5.3 Conversion to $p(CO_2)$

The calibrated $x(CO_2)$ value was 378.16×10^{-6} at P_{eq} = 101.802 kPa (1.0047 atm).

Thus

$$p(CO_2)_{TE,\ dry} = (378.16 \times 10^{-6})(101802) = 38.498 \text{ Pa}$$
$$= 379.94\ \mu\text{atm}.$$

8.5.4 Correction to 100% humidity

The water in the equilibrator has $S = 35$ and $T_E = 298.15$ K (25.00°C).

Thus

$$p_\sigma(H_2O) = 3.1106 \text{ kPa (Chapter 5)}$$
$$= 0.0307 \text{ atm}$$

and from equation (7)

$$p(CO_2)_{TE,\ wet} = 378.16 \cdot (1.0047 - 0.0307)$$
$$= 368.33\ \mu\text{atm}.$$

8.5.5 Calculation of $f(CO_2)$

The equilibrator pressure is P_{eq} = 101.802 kPa and T_E = 298.15 K (25.0°C), then

$$B(CO_2)_{TE} = -123.20 \text{ cm}^3 \text{ mol}^{-1},$$
$$\delta(CO_2)_{TE} = 22.52 \text{ cm}^3 \text{ mol}^{-1}.$$

So, from equation (8),

$$f(CO_2)_{T_E,wet} = 368.33 \cdot \exp\left[\frac{\left(-123.20\times10^{-6} + 2(22.52\times10^{-6})\right)\times 101802}{8.314472 \times 298.15}\right]$$
$$= 367.15\,\mu\text{atm}.$$

8.5.6 Correction to sea surface temperature

The sea surface temperature, T_S = 297.85 K (24.70°C). Thus from equation (9),

$$f(CO_2)_{T_S,wet} = 367.17 \cdot \exp[0.0423 \cdot (297.85 - 298.15)]$$
$$= 362.52\ \mu\text{atm}.$$

9. Quality assurance

9.1 For general principles of analytical quality control see Chapter 3

9.2 Specific applications of analytical quality control

9.2.1 Stability of the response of the infrared analyzer

The performance of the infrared analyzer can be monitored by means of control charts (SOP 22) which give a visual indication of any significant change in the response of the instrument to CO_2. The offset between the cells should remain near zero. The nominal $x(CO_2)$ values of standards should remain fairly stable.

9.2.2 Reproducibility of equilibrated samples

An estimate of the reproducibility of the instrument can be obtained in areas where the rate of change is slow. For marine air samples, this should extend over wide areas; for water it is most striking in the central gyres. The standard deviation of the measurement can be calculated over the period that either ambient air or air from the equilibrator is being measured. The standard deviation should be monitored carefully; it should be less than 0.3 μatm for ambient air and less than 1 μatm for air from the equilibrator.

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Annexe

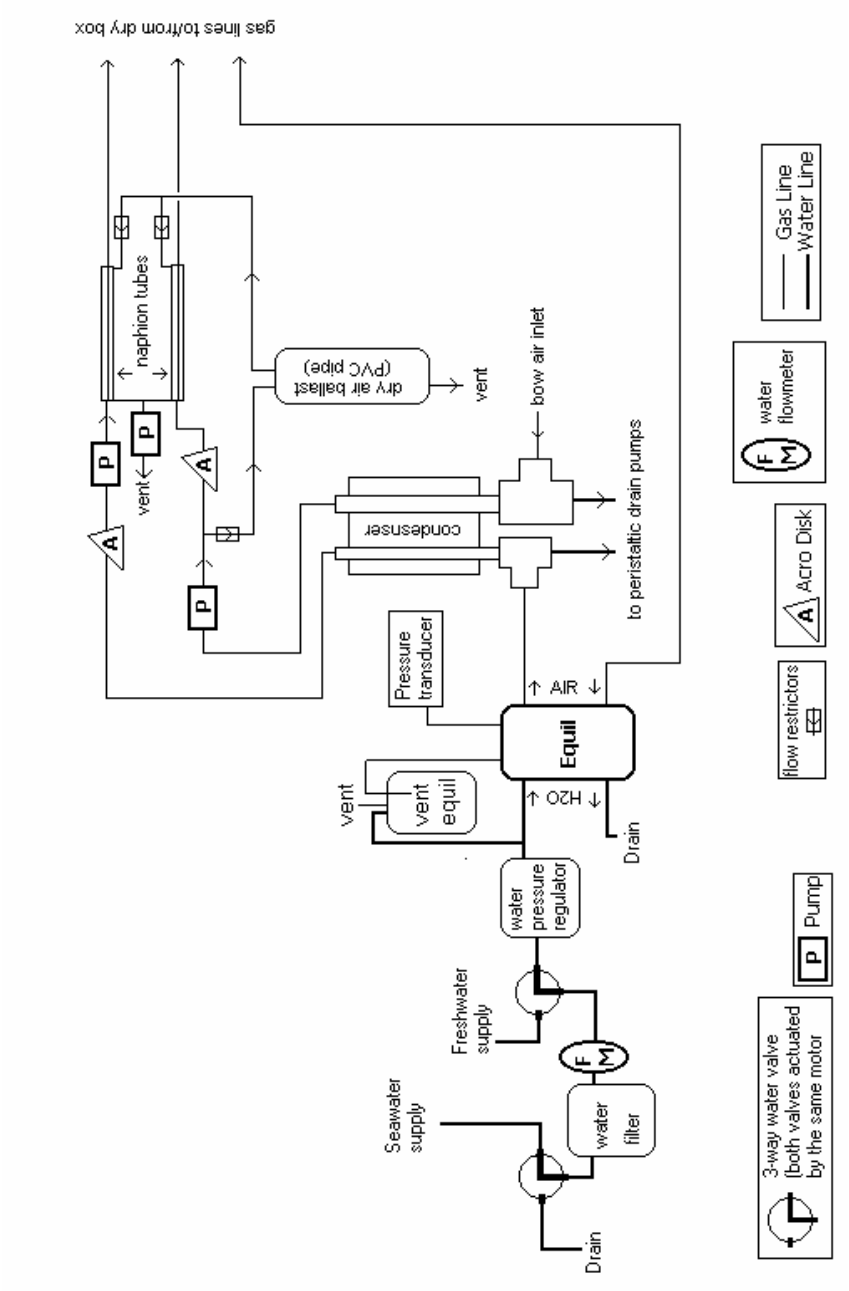

Fig. 1 Schematic showing the layout of the analytical system described here (based on system designed by Craig Neill, Bjerknes Center for Climate Research, Norway).

SOP 6a

Determination of the pH of sea water using a glass /reference electrode cell

1. Scope and field of application

This procedure describes a method for the potentiometric determination of the pH of sea water on the total hydrogen ion concentration pH scale. The total hydrogen ion concentration, $[H^+]$, is expressed as moles per kilogram of sea water.

2. Definition

The total hydrogen ion concentration of sea water includes the contribution of the medium ion sulfate and is defined as

$$\begin{aligned}[H^+] &= [H^+]_F(1 + S_T / K_S) \\ &\approx [H^+]_F + [HSO_4^-]\end{aligned} \quad (1)$$

where $[H^+]_F$ is the *free* concentration of hydrogen ion in sea water, S_T is the total sulfate concentration $([HSO_4^-]+[SO_4^{2-}])$ and K_S is the acid dissociation constant for HSO_4^-. The pH is then defined as the negative of the base 10 logarithm of the hydrogen ion concentration:

$$\mathrm{pH} = -\log_{10}\left(\frac{[H^+]}{\text{mol kg-soln}^{-1}}\right). \quad (2)$$

3. Principle

Values of pH are determined experimentally from sequential measurements of the e.m.f. (E) of the cell

reference electrode	concentrated KCl solution	test solution	glass $[H^+]$ electrode

in a standard buffer (S) of known (defined) pH and in the sea water sample (X).

The operational pH is defined by the expression

$$\mathrm{pH(X)} = \mathrm{pH(S)} + \frac{E_S - E_X}{RT \ln 10 / F} \quad . \tag{3}$$

Residual liquid junction error is minimized by matching the composition of the standard buffer to the sea water sample, *i.e.*, by making the buffer up in synthetic sea water.

Values of pH(S) have been assigned to various standard buffers in synthetic sea water. These are based on careful laboratory measurements made using cells without liquid junction.

4. Apparatus

4.1 pH cell

A combination glass/reference electrode is typically the most convenient cell to use; however, measurement quality can often be improved by using separate glass and reference electrodes.

4.2 Voltmeter with high input impedance

The e.m.f. of the glass/reference electrode cell can be measured with a pH meter or other voltmeter with a high input impedance ($>10^{13}$ Ω). If a pH meter with a sensitivity of ± 0.1 mV is used to measure the e.m.f., the sensitivity in determining the pH is ± 0.002 pH units. The use of a 5½ digit voltmeter with a high input impedance[1] can improve the sensitivity to better than ± 0.001 pH units. (The accuracy of the measurement is dependent upon the reliability of the assignment of pH(S) values to the calibration buffers used.)

4.3 Closed measurement container

It is necessary to measure the pH on a sample that has not had the opportunity to exchange CO_2 with the atmosphere so as to ensure reliable pH results.

4.4 Thermometer (accurate to ± 0.05°C)

The temperature should be known or controlled to within 0.1°C during the measurement.

[1] An external circuit based on a high input impedance operational amplifier (*e.g.*, an FET electrometer amplifier) configured as a voltage follower (unity gain amplifier) can be used to achieve this.

5. Reagents

5.1 Synthetic sea water

- Reagent grade NaCl (dried in an oven at 110°C),
- Reagent grade Na_2SO_4 (dried in an oven at 110°C),
- Reagent grade KCl (dried in an oven at 110°C),
- Calibrated solution of reagent grade $MgCl_2$,[2]
- Calibrated solution of reagent grade $CaCl_2$,[2]
- Deionized water.

5.2 Buffer substances

- Calibrated solution of HCl prepared from redistilled reagent grade HCl. Its concentration should be known to within 0.1%[3].
- 2-amino-2-hydroxymethyl-1,3-propanediol ("TRIS"), crushed and dried in a desiccator at room temperature over phosphorus (V) oxide before use.
- 2-aminopyridine, recrystallized from a benzene–petroleum ether mixture, crushed and dried in a desiccator at room temperature over phosphorus (V) oxide before use.

6. Sampling

It is essential that the samples analyzed are collected, poisoned, and stored according to the procedures detailed in SOP 1. Care should be taken to avoid the exchange of CO_2 with the atmosphere both during sampling and during subsequent manipulation.

7. Procedure

7.1 Preparation of buffers in synthetic sea water

The compositions of a TRIS/HCl buffer and of a 2-aminopyridine/HCl buffer in synthetic sea water with a salinity of 35 are given in Table 1. This recipe is based on synthetic sea water (see Chapter 5, Table 4) in which 0.04 mol/kg-H_2O of NaCl has been replaced with HCl, and contains a total of 0.08 mol/kg-H_2O of the desired base. The simplest way to prepare this buffer accurately is first to weigh out the hydrochloric acid and then to scale the amounts of the other constituents to match the exact amount of HCl that was weighed out. Such buffers can be stored for a number of weeks, in a sealed, almost full, container.

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[2] Solutions of $MgCl_2$ and $CaCl_2$ can be analyzed either by measuring the density of the stock solution, by titrating with a calibrated silver nitrate solution (*e.g.*, using K_2CrO_4 as an indicator) or by gravimetric precipitation of chloride.

[3] Solutions of HCl can be analyzed accurately by coulometric titration, by a careful titration against a standard base (*e.g.*, TRIS—NIST 723) or by gravimetric precipitation of chloride.

Table 1 Composition of a buffer solution for pH in synthetic sea water of salinity 35 (weights based on 1000 g of H_2O).

Constituent	Moles	Weight (g)[a]
NaCl	0.38762[b]	22.6446
KCl	0.01058	0.7884
$MgCl_2$	0.05474	–
$CaCl_2$	0.01075	–
Na_2SO_4	0.02927	4.1563
HCl	0.04000	–
One of:		
2-amino-2-hydroxymethyl-1,3-propanediol (TRIS)	0.08000	9.6837
2-aminopyridine	0.08000	7.5231
Total weight of solution containing:		
2-amino-2-hydroxymethyl-1,3-propanediol (TRIS)	–	1044.09
2-aminopyridine	–	1041.93

[a] Weight in air at sea level (*i.e.*, not corrected to mass). If a weight is not given, the component is added as the appropriate amount of a calibrated solution.

[b] m(NaCl) = 0.42762 – 0.04 mol/kg-H_2O, *i.e.*, replacing NaCl with HCl.

To compute the composition for a buffer with a salinity different from 35[4], first compute the composition of the basic artificial sea water—containing no base or HCl and with the full amount of NaCl—corresponding to the new salinity, S:

$$m_S = m_{35} \times \frac{25.5695S}{1000 - 1.0019S}, \tag{4}$$

then adjust the m(NaCl) down by 0.04 mol/kg-H_2O and add 0.08 mol/kg-H_2O of base.

7.2 Confirm response of pH cell[5]

Before a pH cell (a glass electrode/reference electrode pair) is used to measure pH, it should be tested to ensure that it is performing properly, *i.e.*, that it has an ideal Nernst response.

Bring both buffers (TRIS and 2-aminopyridine) to the same known temperature (*e.g.*, 25°C). Measure and record the e.m.f. of the pH cell in each buffer. The difference in the e.m.f. is used to check the response of the pH cell (see

[4] The magnitude of the error involved in using a salinity 35 buffer for most oceanic measurements (*i.e.*, in the salinity range 33–37) is probably less than 0.005 in pH. For a more complete discussion of this error see Whitfield *et al.* (1985) and Butler *et al.* (1985).

[5] Some investigators make use of the titration curve obtained from titrating a sodium chloride solution with HCl (see SOP 3) to confirm that the electrode pair has the theoretical response (RT/F). However, the value of the slope and the value of $E°$ obtained by fitting experimental results in this fashion are highly correlated and thus not particularly reliable. It is better to verify the response of the electrode pair used with suitable buffers, as is done here.

section 8.1). If the response is not theoretical (within the experimental uncertainty), the electrodes should be rejected. E.m.f. readings obtained with a well-behaved pH cell should be stable with time (drift < 0.05 mV min^{-1})[6].

7.3 Measurement of pH

Bring the TRIS buffer and the sea water samples to be measured to the same known temperature (*e.g.*, 25°C). The e.m.f. of the pH cell is then measured, first in the TRIS buffer (E_S) and then in the sea water sample (E_X). Care should be taken to minimize any exposure of the sea water samples to the atmosphere so as to limit loss or gain of CO_2.

8. Calculation and expression of results

8.1 Calculation of response of pH cell

The defined pH values of the two buffers recommended for use in this procedure are:

2-amino-2-hydroxy-1,3-propanediol (TRIS)

$$\begin{aligned}\mathrm{pH(S)} = {} & (11911.08 - 18.2499S - 0.039336S^2)\frac{1}{T/\mathrm{K}} \\ & - 366.27059 + 0.53993607S + 0.00016329S^2 \\ & + (64.52243 - 0.084041S)\ln(T/\mathrm{K}) - 0.11149858(T/\mathrm{K}).\end{aligned} \quad (5)$$

2-aminopyridine (AMP)

$$\begin{aligned}\mathrm{pH(S)} = {} & (111.35 + 5.44875S)\frac{1}{T/\mathrm{K}} + 41.6775 - 0.015683S \\ & - 6.20815\ \ln(T/\mathrm{K}) - \log_{10}(1 - 0.00106S).\end{aligned} \quad (6)$$

The electrode response, s, can then be calculated:

$$s = \frac{E_{\mathrm{AMP}} - E_{\mathrm{TRIS}}}{\mathrm{pH(S)_{TRIS}} - \mathrm{pH(S)_{AMP}}} \quad (7)$$

and compared with the ideal Nernst value: $RT\ \ln 10/F$. If it is more than about 0.3% different, the pH cell should be replaced.

8.2 Calculation of pH

Values of pH are calculated from the expression

$$\mathrm{pH(X)} = \mathrm{pH(S)} + \frac{E_S - E_X}{RT\ln 10/F} \quad (8)$$

[6] This is an upper limit to the acceptable level of drift. An ideal level is as much as an order of magnitude lower, *e.g.*, < 0.3 mV h^{-1}.

where pH(S), the pH of TRIS buffer (Table 1) on the total hydrogen ion scale (expressed in mol kg-soln^{-1}) is given by equation (5).

8.3 Example calculation

Input data:

$$\begin{aligned} t &= 25°C \text{ (}i.e.\text{, } T = 298.15 \text{ K)}, \\ S &= 35, \\ E_{TRIS} &= -0.0724 \text{ V}, \\ E_{AMP} &= 0.0049 \text{ V}, \\ E_X &= -0.0670 \text{ V}. \end{aligned}$$

Hence

$$\begin{aligned} \text{pH(S)}_{TRIS} &= 8.0936, \\ \text{pH(S)}_{AMP} &= 6.7866, \\ RT \ln 10/F &= 0.05916 \text{ V /pH unit}. \end{aligned}$$

Thus

$$s = \frac{0.0049 - (-0.0724)}{8.0936 - 6.7866} = 0.05914 \text{ V / pH unit}$$

and, using equation (8),

$$\text{pH(X)} = 8.0936 + \frac{-0.0724 - (-0.0670)}{0.05916} = 8.0023 .$$

9. Quality assurance

9.1 For general principles of analytical quality control see Chapter 3

9.2 Specific applications of analytical quality control

9.2.1 Ideality of pH cell behavior

The measured electrode response, s, should be compared with ideal Nernst behavior on a regular basis (see section 7.2). If the value is more than 0.3% from theoretical, try cleaning the glass electrode of surface deposits and measuring again. If the discrepancy persists, the electrode should be replaced.

The value of E_S in TRIS buffer, when measured at a constant temperature (*e.g.*, 25°C), should remain stable to within a few mV. A sudden change in E_S is indicative of potential problems. Similarly, the e.m.f. of a well-behaved pH cell immersed in a thermostated buffer should be stable (drift < 0.05 mV min^{-1}).

9.2.2 Precision

A precision of 0.003 pH units (1 SD) is possible with care. Plot the results of duplicate analyses on a range control chart (SOP 22).

9.2.3 Bias

The bias of potentiometric pH measurements depends on the care with which the buffer was prepared, especially with regard to the ratio between the TRIS and the HCl, and on the accuracy with which the values of pH(S) were originally assigned. This latter value has been estimated as being within 0.004 pH units.

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SOP 6b

Determination of the pH of sea water using the indicator dye *m*-cresol purple

1. Scope and field of application

This procedure describes a method for the spectrophotometric determination of the pH of sea water on the total hydrogen ion concentration pH scale. The total hydrogen ion concentration, $[H^+]$, is expressed as moles per kilogram of sea water.

2. Definition

The total hydrogen ion concentration of sea water includes the contribution of the medium ion sulfate and is defined as

$$\begin{aligned}[H^+] &= [H^+]_F(1 + S_T / K_S) \\ &\approx [H^+]_F + [HSO_4^-] \end{aligned} \quad (1)$$

where $[H^+]_F$ is the *free* concentration of hydrogen ion in sea water, S_T is the total sulfate concentration $([HSO_4^-] + [SO_4^{2-}])$ and K_S is the acid dissociation constant for HSO_4^-. The pH is then defined as the negative of the base 10 logarithm of the hydrogen ion concentration:

$$\mathrm{pH} = -\log_{10}\left(\frac{[H^+]}{\text{mol kg-soln}^{-1}}\right). \quad (2)$$

3. Principle

The values of pH are determined by adding an indicator dye to sea water. For the sulfonephthalein indicators such as *m*-cresol purple, the reaction of interest at sea water pH is the second dissociation

$$HI^-(aq) = H^+(aq) + I^{2-}(aq) \quad (3)$$

where I represents the indicator dye, which is present at a low level in a sea water sample. The total hydrogen ion concentration of the sample can then be determined:

$$\mathrm{pH} = \mathrm{p}K(\mathrm{HI}^-) + \log_{10}\frac{[\mathrm{I}^{2-}]}{[\mathrm{HI}^-]}. \quad (4)$$

The principle of this approach uses the fact that the different forms of the indicator have substantially different absorption spectra. Thus the information contained in the composite spectrum can be used to estimate $[I^{2-}]/[HI^-]$.

At an individual wavelength, λ, the measured absorbance in a cell with a path length, l, is given by the Beer–Lambert law as

$$\frac{A_\lambda}{l} = \varepsilon_\lambda(\mathrm{HI}^-)[\mathrm{HI}^-] + \varepsilon_\lambda(\mathrm{I}^{2-})[\mathrm{I}^{2-}] + B_\lambda + e \quad (5)$$

where B_λ corresponds to the background absorbance of the sample and e is an error term due to instrumental noise. Provided that the values of the extinction coefficients: $\varepsilon_\lambda(HI^-)$ and $\varepsilon_\lambda(HI^{2-})$ have been measured as a function of wavelength, absorbance measurements made at two or more wavelengths can be used to estimate the ratio $[I^{2-}]/[HI^-]$.

In the case that only two wavelengths are used, and provided that the background can be eliminated effectively by a subtractive procedure, (5) can be rearranged to give (assuming no instrumental error)

$$\frac{[\mathrm{I}^{2-}]}{[\mathrm{HI}^-]} = \frac{A_1/A_2 - \varepsilon_1(\mathrm{HI}^-)/\varepsilon_2(\mathrm{HI}^-)}{\varepsilon_1(\mathrm{I}^{2-})/\varepsilon_2(\mathrm{HI}^-) - (A_1/A_2)\varepsilon_2(\mathrm{I}^{2-})/\varepsilon_2(\mathrm{HI}^-)} \quad (6)$$

where the numbers 1 and 2 refer to the wavelengths chosen. For the best sensitivity, the wavelengths corresponding to the absorbance maxima of the base (I^{2-}) and acid (HI^-) forms, respectively, are used. The various terms ε are the extinction coefficients of the specified species at wavelengths 1 and 2, respectively.

4. Apparatus

4.1 Flexible drawing tube

Approximately 40 cm long, sized to fit snugly over cell port. Silicone rubber is suitable for this (see Footnote 1 in SOP 1).

4.2 Spectrophotometric cells

These should be made of optical glass with a 10 cm path-length, two ports and polytetrafluoroethylene (Teflon®) stoppers. A sufficient number of cells are needed to collect all the samples that will be analyzed from a particular cast (see section 6).

4.3 Micropipette

A micropipette is used to add the dye to the cell. It should be of ~ 0.1 cm^3 capacity with a narrow Teflon® tube attached to act as a nozzle.

4.4 High-quality spectrophotometer

For work of the highest sensitivity and precision, a double-beam spectrophotometer is desirable. However, good results can be obtained with a high-quality single-beam instrument.

4.5 Temperature-control system for spectrophotometer cell

Commercially manufactured, thermostated spectrophotometer compartments that can accommodate 10 cm cells are rarely available and one will probably have to be custom-made. The temperature should be regulated to within 0.1°C.

4.6 System to warm samples to measurement temperature

Although it is possible to warm up the cells containing samples in Ziploc® bags in a thermostat bath, this is inconvenient. It is much better to build a custom-made thermostated compartment that can hold approximately 12 cells at once without getting them wet.

4.7 Thermostat bath (± 0.05°C)

A thermostat bath is used to regulate the temperature of the cell compartment and the temperature of the system described in section 4.6.

5. Reagents

5.1 Solution of *m*-cresol purple

A concentrated (at least 2 mmol dm^{-3}) dye solution of known pH adjusted to be in the range 7.9 ± 0.1 pH units—chosen to match pH measurements from an oceanic profile—is required; this implies that for *m*-cresol purple $A_1/A_2 \approx 1.6$.[1]

6. Sampling

Draw the sample—using the drawing tube—directly from the Niskin bottle (or other water sampler) into the optical cell. After flushing with several hundred cm^3 of sea water—a flushing time of 15–20 seconds—seal the cell with the Teflon® caps ensuring that there is no headspace. Since the pH samples must be analyzed immediately, there is no long-term storage or preservation protocol. However, while awaiting analysis, store the samples in the dark at room temperature.

[1] The absorbance ratio of a concentrated dye solution can be measured using a cell with a short path length (0.5 mm).

7. Procedure

7.1 Warm sample cell to 25.0°C (± 0.1°C)

This is done by placing a number of cells in a thermostated compartment (see section 4.6) for a few hours.

7.2 Measure absorbances for the cell + sea water

Clean and dry the exterior of the cell; place the cell in the thermostated sample compartment of the spectrophotometer. Measure and record the absorbances at three wavelengths: a non-absorbing wavelength (730 nm for *m*-cresol purple) and at the wavelengths corresponding to the absorption maxima of the base (I^{2-}) and acid (HI^{-}) forms of the dye respectively (578 and 434 nm).

7.3 Inject dye into cell

Remove one of the cell caps, add approximately 0.05–0.1 cm^3 of concentrated dye (~2 mmol dm^{-3}) to the sample, replace the cap and shake the cell to mix the sea water and dye. The amount of dye required is that which will produce absorbance values of between 0.4 and 1.0 at each of the two absorbance peaks.

7.4 Measure absorbances of cell + sea water + dye

Return the cell to the spectrophotometer and again measure the absorbances at the three wavelengths used in section 7.2. Cells should be positioned to maintain consistent alignment(s) between baseline and indicator absorbance measurements.

8. Calculation and expression of results

8.1 Correction of measured absorbances

At each of the three wavelengths, subtract the absorbances measured for the background measurement (without dye) from the corresponding absorbances measured for the system containing dye.

In addition, the absorbance measured at a non-absorbing wavelength is used to monitor and correct for any baseline shift due to error in repositioning the cell, instrumental shifts, *etc.*[2]. This assumes that the magnitude of any observed baseline shift is identical across the visible spectrum. To do this, subtract the measured shift from the background-corrected absorbances at wavelengths 1 and 2 to obtain the final corrected absorbance value at each wavelength.

These final absorbance values, corrected for background absorbances *and* any observed baseline shifts, are used to calculate A_1/A_2, the absorbance ratio which describes the extent of protonation of the dye.

[2] The difference between the baseline absorbance (sea water only) and the absorbance of the sample + dye at 730 nm should be no greater than ± 0.001; if this value is exceeded, the cell should be removed and the optical windows cleaned before the absorbances are measured again.

8.2 Calculation of the pH of the sea water + dye

The pH of the sea water and dye in the cell is computed from

$$\mathrm{pH} = \mathrm{p}K_2 + \log_{10}\left(\frac{A_1/A_2 - \varepsilon_1(\mathrm{HI}^-)/\varepsilon_2(\mathrm{HI}^-)}{\varepsilon_1(\mathrm{I}^{2-})/\varepsilon_1(\mathrm{HI}^-) - (A_1/A_2)\varepsilon_2(\mathrm{I}^{2-})/\varepsilon_2(\mathrm{HI}^-)}\right) \quad (7)$$

where $\mathrm{p}K_2$ is the acid dissociation constant for the species HI^- (expressed on the total hydrogen ion concentration scale in mol kg-soln^{-1}), and A_1 and A_2 are the corrected absorbances measured at the wavelengths corresponding to the absorbance maxima of the base and acid forms, respectively. The various extinction coefficient terms ε correspond to values measured for the specified species at wavelengths 1 and 2, respectively (Table 1).

Table 1 Extinction coefficient ratios for *m*-cresol purple.

$\varepsilon_1(\mathrm{HI}^-)/\varepsilon_2(\mathrm{HI}^-)$	0.00691
$\varepsilon_1(\mathrm{I}^{2-})/\varepsilon_2(\mathrm{HI}^-)$	2.2220
$\varepsilon_2(\mathrm{I}^{2-})/\varepsilon_2(\mathrm{HI}^-)$	0.1331

$\lambda_1 = 578$ nm; $\lambda_2 = 434$ nm.

The equilibrium constant K_2 is a function of salinity and temperature and has been determined by careful laboratory measurements[3]. For *m*-cresol purple,

$$\mathrm{p}K_2 = \frac{1245.69}{(T/\mathrm{K})} + 3.8275 + 0.0021\,1(35 - S) \quad (8)$$

where $293 \le T/\mathrm{K} \le 303$ and $30 \le S \le 37$.

8.3 Correction for pH change resulting from addition of the dye

The addition of indicator dye to the sea water sample will perturb the pH (another acid–base system has been added!). Although care is taken to minimize this (by adjusting the dye solution pH), it is desirable to correct for the addition of dye to obtain the best pH measurements.

Although, in principle, the pH perturbation could be calculated from a knowledge of the equilibrium chemistry of the sample and the dye, it is simpler to evaluate the magnitude of the correction empirically. A pair of additions of dye is made to each of a series of sea water samples with different pHs, and the change in the measured ratio (A_1/A_2) with the second addition of indicator solution is determined as a function of the measured value (A_1/A_2) determined after the first addition of dye using a least-squares procedure (SOP 23):

$$\frac{\Delta(A_1/A_2)}{V} = a + b(A_1/A_2) \quad (9)$$

[3] Although DelValls and Dickson (1998) have suggested that this $\mathrm{p}K_2$ may be in error because of an error in calibrating TRIS buffer, it seems that there may be a compensating error that largely mitigates the proposed correction. The $\mathrm{p}K_2$ given here is that from Clayton and Byrne (1993).

where V is the volume of dye added at each addition. The final, corrected, absorbance ratio is

$$(A_1 / A_2)_{\text{corr}} = (A_1 / A_2) - V[a + b(A_1 / A_2)]\,. \tag{10}$$

8.4 Example calculation

$$\begin{aligned} t &= 25°\text{C}, \\ S &= 35, \\ \text{p}K_2 &= 8.0056, \end{aligned}$$

and for indicator stock solution with $A_1/A_2 = 1.6$,

$$\frac{\Delta(A_1 / A_2)}{V} = 0.125 - 0.147(A_1 / A_2)\,.$$

Measured absorbances:

Sea water: $A_{434} = 0.02433$; $A_{578} = 0.01936$; $A_{730} = 0.08365$
Dye + sea water: $A_{434} = 0.45123$; $A_{578} = 0.84574$; $A_{730} = 0.08298$

After addition of dye,

$$A_1 / A_2 = \frac{0.84574 - 0.01936 - (0.08298 - 0.08365)}{0.45123 - 0.02433 - (0.08298 - 0.08365)} = 1.93430.$$

Corrected to zero dye addition ($V = 0.08$ cm^3),

$$\begin{aligned} (A_1 / A_2)_{\text{corr}} &= 1.93430 - 0.08[0.125 - 0.147(1.93430)] \\ &= 1.94705 \end{aligned} \tag{11}$$

and thus

$$\text{pH} = 8.0056 + \log_{10}\left(\frac{1.94705 - 0.00691}{2.2220 - 1.94705 \times 0.1331}\right) = 8.0005.$$

9. Quality assurance

9.1 For general principles of analytical quality control see Chapter 3

9.2 Specific applications of analytical quality control

9.2.1 Spectrophotometer performance

The spectrophotometric performance of the instrument used can be confirmed using reference materials that are available from the U.S. National Institute for Standards and Technology (NIST). SRM 2034 is a holmium oxide solution in a sealed cuvette that allows the wavelength accuracy of the spectrophotometer to be determined; SRM 930d is a set of absorbance filters that allows the

absorbance measurement accuracy to be verified. Property control charts of these measurements should be maintained, and the spectrophotometer adjusted if it goes out of tolerance. (Nevertheless, the procedure detailed here is fairly insensitive to minor changes in spectrophotometer performance.)

A more important concern is that the spectrometer have a high stability. This can be confirmed by making a series of repeated measurements on a system of constant absorbance (*e.g.*, SRM 930d or a thermostated buffer solution containing indicator dye) and computing the standard deviation at the wavelengths of interest.

9.2.2 Precision

A precision of better than 0.001 pH units (1 SD) is possible with care—particularly in regard to the sample handling. The results of duplicate analyses should be plotted on a range control chart (SOP 22).

9.2.3 Bias

The bias of spectrophotometric pH measurements depends on the accuracy with which the various extinction coefficient ratios were determined, and on the accuracy of the values assigned to the values of pK_2. A significant advantage of spectrophotometric measurements is that, if more accurate information becomes available for these parameters at a later time, the pH results obtained can be adjusted without any degradation in precision provided that the original data are retained. At present, the likely bias is estimated to be less than 0.005 pH units.

10. Bibliography

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Dickson, A.G. 1993. The measurement of sea water pH. *Marine Chem.* **44**: 131–142.

SOP 7

Determination of dissolved organic carbon and total dissolved nitrogen in sea water

1. Scope and field of application

This procedure describes a method for the determination of dissolved organic carbon (DOC) and total dissolved nitrogen (TDN) in sea water, expressed as micromoles of carbon (nitrogen) per liter of sea water. The method is suitable for the assay of oceanic levels of dissolved organic carbon (< 400 μmol L^{-1}) and total dissolved nitrogen (< 50 μmol L^{-1}). The instrument discussed and procedure described are those specific to the instrument employed in the Hansell Laboratory at the University of Miami. Instruments produced by other manufacturers should be evaluated for suitability.

2. Definition

The dissolved organic carbon content of sea water is defined as:

> *The concentration of carbon remaining in a sea water sample after all particulate carbon has been removed by filtration and all inorganic carbon has been removed by acidification and sparging.*

The total dissolved nitrogen content of sea water is defined as:

> *The concentration of nitrogen remaining in a sea water sample after all particulate nitrogen has been removed by filtration.*

3. Principle

A filtered and acidified water sample is sparged with oxygen to remove inorganic carbon. The water is then injected onto a combustion column packed with platinum-coated alumina beads held at 680°C. Non-purgeable organic carbon compounds are combusted and converted to CO_2, which is detected by a non-dispersive infrared detector (NDIR). Non-purgeable dissolved nitrogen compounds are combusted and converted to NO which, when mixed with ozone, chemiluminesces for detection by a photomultiplier.

4. Apparatus

- Shimadzu TOC-V_{CSH} with ASI-V auto sampler and TNM-1 Total Nitrogen detector (or equivalent).

5. Reagents

5.1 Compressed gas

Ultra High Purity (UHP 99.995%) oxygen is used as the carrier gas for the Shimadzu TOC-V_{CSH}. High quality carrier gas is required to obtain low background levels in the detector. Oxygen is used to ensure complete combustion of all organic material.

5.2 Combustion column catalyst

The carrier gas passes through a column packed with 2 mm platinum-coated alumina beads (Shimadzu P/N 017-42801-01) held at 680°C.

5.3 Platinum gauze

Pure platinum wire gauze (52 mesh woven from 0.1 mm diameter wire) is roughly formed into cubes (≈ 0.5 cm to a side) and several (3–5) are placed on top of the combustion column bed. The platinum gauze improves analytical reproducibility and retains injected salt.

5.4 Acidification of sample

Trace-impurity analyzed concentrated hydrochloric acid is used to acidify samples prior to analysis. Approximately 0.1% by volume of the concentrated acid is added to each sample prior to analysis to lower the pH of the sample to pH < 2. At this pH and with sparging, all inorganic carbon species are converted to CO_2 and removed from the sample. Automated acidification by the TOC-V_{CSH} is not used, as with time the blank using this acid solution increases. When the sample is acidified manually with acid freshly taken from a sealed bottle, the increase of the blank has not been observed.

6. Sampling

Proper sampling techniques and handling are essential to good quality data. Care must be taken to minimize contamination of the sample. Sampling from the rosette should be done using clean silicone tubing. Gloves should be worn during sampling. It is recommended that anyone sampling from the rosette prior to collection of the samples (*e.g.*, gases) also wear gloves. If that it not possible, every effort must be made not to touch the sample nipple (the path of the water stream, from Niskin to sample bottle, must be kept very clean). Grease (whether mechanical grease from ship operations or sealing grease, as employed for some gas sampling) should never be allowed to come in contact with the sample nipple.

6.1 Sample preparation

Prior to sampling, 60 ml High Density Polyethylene (HDPE) bottles are cleaned, first by rinsing with distilled water, followed by a 4-hour soak in 10% hydrochloric acid, and then copiously rinsed with distilled water, inverted onto a clean surface and allowed to air dry.

All tubing and the polycarbonate inline filter holder should be acid washed and rinsed with copious quantities of distilled water prior to use. Tubing should be silicone; under no circumstances should Tygon® tubing be used as it is a source of contamination.

GF/F filters should be combusted at 450°C for at least 4 hours prior to use and stored in a sealed glass container.

6.2 Sample collection

Whether or not a sample is filtered prior to analysis depends on the goal of the measurement. If DOC(N) is the variable of interest, then all samples must be filtered. However, the handling of water required for filtration can introduce contaminants, so in some cases filtration may be bypassed. In oligotrophic waters, for example, where particulate organic carbon concentrations may be a very small fraction of the total organic carbon, filtering may not be necessary. Since the particles are generally small and homogeneously distributed in a sample, the analysis of unfiltered water results in a good measure of total organic carbon (TOC). Likewise, samples collected at depths > 250 m may be left unfiltered as water from these depths normally has low particulate organic carbon loads (< 1 μmol L^{-1}).

In high productivity areas, a substantial portion of the total carbon may be present in particulate form, and many of those particles may be large and so not homogeneously and representatively assessed in the DOC analyzer. In those situations, samples collected between the surface and 250 m are filtered through a precombusted GF/F filter. For consistency when sampling in both oligotrophic and eutrophic environments as part of a study, prefiltering is recommended for all upper layer waters.

The GF/F filters are housed in a polycarbonate inline filter holder connected to the Niskin bottle sample nipple with silicone tubing, with collection of filtrate into a precleaned 60 ml HDPE bottle. HDPE sample bottles should be labeled with sample-specific information, such as the cruise designation, cast number, and Niskin bottle number. The filter holder, with filter in place, must be well flushed with sample prior to collection into the bottles. The sample bottles should be rinsed three times with sample prior to filling. Bottles should be filled to between 75 and 90%, or 45 to 55 ml into the 60 ml bottle. This volume provides room for expansion of the water on freezing. The sample bottles are then capped tightly and frozen upright.

7. Procedure

Water samples are collected from the rosette. Water taken from the surface to 250 m is filtered using precombusted (450°C) GF/F inline filters as they are being collected from the Niskin bottle. At depths > 250 m, the samples are collected without filtration. After collection, samples are frozen upright in 60 ml acid-cleaned HDPE bottles, and remain cold until analysis. Prior to analysis, samples are returned to room temperature and acidified to pH < 2 with concentrated hydrochloric acid. Analysis is performed using a Shimadzu TOC-V_{CSH} Total Organic Carbon Analyzer with the TNM-1 Total Nitrogen detector.

Instrument conditions are as follows:

Combustion temperature	680°C
Carrier gas	UHP Oxygen
Carrier flow rate	150 ml min^{-1}
Ozone generation gas	Zero Air from Whatman TOC Gas Generator
Ozone flow rate	500 ml min^{-1}
Sample sparge time	2.0 min
Minimum number of injections	3
Maximum number of injections	5
Number of washes	2
Standard deviation maximum	0.1000
CV maximum	2.00%
Injection volume	100 μl

Each detector functions independently with respect to the acceptance values above. If DOC meets the required specifications, but TDN does not, the instrument will continue making injections until either the criteria are met or the maximum number of injections has been reached. The same is true for the situation where TDN has met the criteria and the DOC has not.

The DOC system is calibrated using potassium hydrogen phthalate and the TDN system using potassium nitrate, both in Milli-Q® water. System performance is verified daily using Consensus Reference Water (www.rsmas.miami.edu/groups/biogeochem/CRM.html). This reference water is deep Sargasso Sea water (DSR) that has been acidified and sealed in 10 ml ampoules, the concentrations of which (of DOC and TDN) have been determined by the consensus of up to six expert and independent laboratories. Low Carbon Water (LCW) that has gone through the same acidification, sealing process, and consensus verification program as the DSR, and has an agreed upon carbon concentration of 1–2 μmolC L^{-1}, is also analyzed and used to determine the instrument blank. After verifying proper operation of the TOC/TN instrument, samples are placed on an auto sampler for analysis. The run starts with a QW (Q Water) blank and a reference seawater analysis. Then six samples are analyzed, followed by another QW blank and reference sea water. This sequence is repeated until all samples for that run are analyzed. The run ends with a QW blank, reference water, and a QW blank that had not been acidified. This last blank verifies that the hydrochloric acid used to acidify the samples is not contaminated. QW blanks and reference water samples are used to evaluate

system performance during the analytical run. If a problem is detected with the blanks or reference waters, the samples are reanalyzed.

8. Calculation and expression of results

The Shimadzu TOC-V_{CSH} is calibrated for carbon using a 4- to 5-point analysis of potassium hydrogen phthalate in Milli-Q® water. The instrument determines the concentration in parts per million (ppm), and the concentration of the sample in μM (micromolar or micromoles per liter), corrected for the instrument blank, is calculated as

$$[(\text{Sample (ppm)} - \text{LCW (ppm)}) \times 83.33] + \text{LCW value } (\mu\text{M})$$

where Sample and LCW are the concentrations determined by the TOC-V_{CSH}, 83.33 is a conversion factor converting ppm to μM and LCW is the carbon concentration of the Low Carbon Water CRM. Subtracting the LCW (ppm) from the sample removes both instrument blank and carbon content of the LCW. The carbon content of the LCW is added again (final term in equation) to calculate the correct sample concentration.

For total dissolved nitrogen, the instrument is calibrated using a similar method to that used for calibrating total carbon. The standard is potassium nitrate in Milli-Q® water. Again, the instrument is calibrated in ppm and the following calculation is used:

$$\text{Sample (ppm)} \times 71.43$$

where Sample is the concentration determined by the TOC-V_{CSH} and 71.43 is a conversion factor from ppm to μM. An instrument blank has not been detected for the nitrogen system. Dissolved organic nitrogen (DON) is calculated by subtracting inorganic nitrogen (NO_2, NO_3, *etc.*) from the total dissolved nitrogen determined by the TOC-V_{CSH}.

9. Quality assurance

On a daily basis, CRM is analyzed to verify system performance. If the value of the CRM does not fall within the expected range, samples are not analyzed until the expected performance has been established.

The QW blanks and reference seawater samples analyzed with the samples are used for quality assurance and quality control (QA/QC). By evaluating the performance of these reference waters, instrument drift and performance can be evaluated. If a problem is detected with either drift or performance, the samples are reanalyzed.

SOP 11

Gravimetric calibration of the volume of a gas loop using water

1. Scope and field of application

This procedure describes how to calibrate the volume of a length of stainless steel tubing coiled as a loop based on the procedures of Wilke *et al.* (1993). Typically, two loops are installed onto an 8-port chromatography valve to calibrate the coulometer used in the determination of total dissolved inorganic carbon in sea water (SOP 2). This procedure is capable of achieving a reproducibility of about 0.01% (1 relative standard deviation). A procedure is also detailed for computing the volume of the loop, in the valve assembly, at temperatures different from the calibration temperature.

2. Principle

The loop is weighed empty and full of water and its volume at the calibration temperature is computed from the mass of water contained. The volume at another temperature can then be calculated by allowing for the thermal expansion of the tubing.

3. Apparatus

- Length of 316 stainless steel tubing $^1/_8$ inch (~ 0.3 cm) outside diameter, electropolished on the inside, and coiled as a loop. The ends of the tubing must be cut perfectly square[1]. Typically, two calibration loops have lengths designed to deliver a volume of pure CO_2 that brackets the anticipated CO_2 content of the sea water samples. If the sea water sample size is approximately 29 ml, then a typical carbon yield (S = 35, C_T = 2000 μmol kg^{-1}) is about 700 μg C. Ideal nominal loop volumes would then be 1.25 and 1.75 ml yielding about 500 and 800 μg C, respectively.
- 8-port chromatography valve (*e.g.*, 8UWP, Valco Instruments Co. Inc. (VICI®)),
- Analytical balance, capacity 300 g, sensitivity 0.1 mg,
- Constant temperature bath capable of maintaining 25 ± 0.1°C,
- 100 ml syringe and clean Teflon® tubing to connect the syringe to the loop/valve assembly,
- Helium leak detector (*e.g.*, Gow-Mac Instrument Co., Bethlehem, PA, U.S.A.) or an alternative method for ensuring a proper seal between the loops and the chromatography valve.

[1] The square ends are needed to ensure that the tubing fits properly into the valve ports.

4. Reagents

- Helium supply,
- Ultra-pure water (*e.g.*, distilled and then deionized) degassed by sparging with He at > 200 ml min^{-1} for 30 minutes,
- Dry compressed N_2 gas,
- Methanol (analytical grade).

5. Procedure

5.1 Clean the loop and valve assembly prior to weighing. It is essential that they be scrupulously clean before the measurement and that they remain that way. Rinse the exterior of the loop and flush the interior of the loop repeatedly with deionized water, then with methanol. Dry the loop overnight by flushing with N_2 gas. Use gloves or tongs to handle the loop at all times to maintain cleanliness.

5.2 Carefully connect the loops to the ports of the chromatography valve using either Hastalloy (ZF2HC, VICI®) or gold plated (ZF2GP, VICI®) ferrules.

5.3 Leak test the loop/valve assembly by pressurizing the system to ~ 250 kPa with helium and checking for leaks using the helium leak detector.

5.4 Place the valve along with loose port plugs (ZC2, VICI®) into an open Ziploc freezer bag and dry in a vacuum oven at < 95 kPa at ambient temperature until a constant weight can be determined. Reseal the bag as you remove it from the oven to minimize moisture contamination.

5.5 Determine the dry weight by quickly removing the valve from the Ziploc and weighing on the balance. Take the average of five weights as the "dry weight" of the assembly.

5.6 Once the dry weight is determined, secure the ports for the second loop using the port plugs and attach the syringe and tubing to the remaining two ports.

5.7 Place the container of ultra-pure water and the valve assembly double bagged in Ziplocs® (valve assembly must be kept scrupulously dry) into the constant temperature bath for 1 hour until thermally equilibrated.

5.8 Flush and fill the loop with ultra-pure degassed water using the syringe, then manually switch the valve as smoothly and quickly as possible to isolate the fluid path. The temperature of the water should be controlled.

5.9 Remove the valve from the bath, disconnect tubing and flush non-isolated valve pathways with N_2, flush with two 50 ml methanol rinses, then purge with N_2 for 30–45 minutes at 200 ml min^{-1}. Ensure that all exposed parts are dry.

5.10 Weigh the valve assembly five times to determine the "full weight".

5.11 Remove port plugs and rinse with methanol, dry with N_2, turn valve to original position and return valve and plugs to vacuum oven.

5.12 Weigh the dried valve assembly at ½-hour intervals until a constant weight is obtained. If the difference between the dry weight and the final weight is < 0.0007 g, then the calibration result is considered valid.

6. Calculation and expression of results

6.1 The volume (V) of water, in milliliters, is calculated by correcting the mass of water (M_a), determined as the difference between the full weight and the dry weight, to the weight under vacuum (buoyancy correction) and dividing the result by the density (d) of water[2] at 25°C:

$$V = \left[M_a \cdot (0.0012/d - 0.0012/8.000) + M_a\right]/d \quad (1)$$

where 0.0012 g cm^{-3} is the density of moist air at standard temperature and pressure and 8.000 g cm^{-3} is the density of stainless steel weights in air.

6.2 The thermal expansion of the tubing being used must be taken into account in order to convert the volume measured at one temperature (t_1) to an alternate temperature (t_2). For 316 stainless steel, the coefficient of linear expansion (α_l) is about 1.73 × 10^{-5} K^{-1} (Weast, 1975). The coefficient of volumetric expansion,

$$\alpha_v = (1+\alpha_l)^3 - 1 \approx 3 \cdot \alpha_l, \quad (2)$$

is used to calculate the volume at the alternate temperature,

$$V(t_2) = V(t_1)\left[1 + \alpha_V (t_2 - t_1)\right]. \quad (3)$$

7. Quality assurance

The following points should be noted:

- The weights for the stainless steel tubing (dry) obtained at each measurement should agree with each other to ± 1 mg. This confirms that the tubing is being cleaned and dried adequately before each weighing.
- Measurements of the volume of the stainless steel tubing made on different days should agree with each other when corrected to a standard temperature.
- The ratio of measured loop volumes from a pair of loops should agree with the ratio of the amounts of CO_2 gas delivered, as determined by the coulometer.

8. Bibliography

Weast, R.F. 1975. CRC Handbook of Chemistry and Physics, 56th edition, Chemical Rubber Company.

Wilke, R.J., Wallace, D.W.R. and Johnson, K.M. 1993. Water-based, gravimetric method for the determination of gas sample loop volume. *Anal. Chem.* **65**: 2403–2406.

[2] The formula given for the water density in Chapter 5 is for air-saturated water. However, the error induced by using this formula with helium-sparged water is negligible.

SOP 12

Gravimetric calibration of volume delivered using water

1. Scope and field of application

This procedure describes how to calibrate the volume of water delivered by a volumetric pipette—or similar device such as a Knudsen style pipette, a syringe or a piston burette. This is expressed as the volume delivered at a standard temperature (20.0°C). This procedure is capable of achieving a reproducibility of better than 0.01% (1 relative standard deviation).

2. Principle

The mass of water delivered by the device at a measured calibration temperature is used to compute the volume of water delivered at that temperature. The volume that would be delivered at the standard temperature (20°C) can be calculated by taking account of the volumetric expansion of the dispenser. The volume of liquid delivered at any desired temperature can be calculated in a similar fashion.

3. Apparatus

- Analytical balance capable of weighing the quantity of water delivered with a resolution of 1 part in 10^5 while having sufficient capacity to weigh the water together with the glass container used to collect it,
- Clean dry glass containers with suitable closures[1],
- Thermometer accurate to ± 0.1°C,
- Timer.

4. Reagents

- Deionized water.

[1] If the container and water will be weighed shortly after delivery, then an ungreased ground glass stopper, or even a screw cap, is suitable. If it will be some time before the water delivered is weighed, as when samples are delivered on board ship, it is essential that the closure chosen be both air- and water-tight.

5. Procedure

5.1 Weigh the clean, dry, empty container together with the associated closure.

5.2 Fill the clean pipette or other apparatus being calibrated with deionized water. Allow the temperature of the pipette and water to reach an equilibrium value. Note this temperature.

5.3 Allow the water to drain into the pre-weighed container for a controlled time (60 seconds).

5.4 Close the container and reweigh it.

6. Calculation and expression of results

6.1 Volume of water delivered at the calibration temperature

Compute the weight of the water delivered from the difference between weights of the filled and empty container:

$$w(\mathrm{H_2O}) = w(\text{filled container}) - w(\text{empty container})\,. \tag{1}$$

Compute the mass of water contained, correcting for air buoyancy (see SOP 21):

$$m(\mathrm{H_2O}) = w(\mathrm{H_2O})\left(\frac{1-\rho(\text{air})/\rho(\text{weights})}{1-\rho(\text{air})/\rho(\text{sample})}\right). \tag{2}$$

The volume dispensed at the noted temperature (t) is

$$V(t) = m(\mathrm{H_2O})/\rho(\mathrm{H_2O},\ t). \tag{3}$$

The density of air-saturated water in the temperature range 5 to 40°C is given by the expression (Jones and Harris, 1992)

$$\begin{aligned}\rho_{\mathrm{W}}/(\mathrm{kg\ m^{-3}}) = {} & 999.84847 + 6.337563\times10^{-2}\,(t/°\mathrm{C}) \\ & - 8.523829\times10^{-3}\,(t/°\mathrm{C})^2 + 6.943248\times10^{-5}\,(t/°\mathrm{C})^3 \\ & - 3.821216\times10^{-7}\,(t/°\mathrm{C})^4\end{aligned} \tag{4}$$

where t is the temperature on ITS 90[2]. To achieve an accuracy of 1 part in 10^4, t must be known to within 0.5°C.

6.2 Volume that would be delivered at an alternate temperature

To convert the volume dispensed at one temperature (t_1) to the volume that would be delivered at a standard or alternate temperature (t_2), we need to take account of

[2] The International Practical Temperature Scale of 1968 (IPTS 68) has been superceded by the International Temperature Scale of 1990 (ITS 90). A simple equation can be used to relate the two over the oceanographic temperature range 0 to 40°C (Jones and Harris, 1992):

$$t_{90} = 0.0002 + 0.99975\ t_{68}.$$

The small difference in temperature scales is typically not important to the calibration of glassware for the procedures in this Guide.

the thermal expansion of the dispenser being used. For Pyrex-like glasses (Corning 7740, Kimble KG-33, Schott Duran, Wheaton 200, *etc.*), the coefficient of linear expansion α_l is 32.5×10^{-7} K^{-1}; for glasses such as Kimble KG-35, α_l is about 55×10^{-7} K^{-1}.

The coefficient of volumetric expansion,

$$\alpha_V = (1+\alpha_l)^3 - 1 \approx 3\alpha_l \,, \tag{5}$$

is used to calculate the corrected volume at the alternate temperature,

$$V(t_2) = V(t_1)\left[1 + \alpha_V (t_2 - t_1)\right]. \tag{6}$$

This correction is negligible for all except the most precise work unless $t_2 - t_1$ exceeds 10°C.

6.3 Example calculation

6.3.1 The following data were used for this calculation:

$$\begin{aligned} w(\mathrm{H_2O}) &= 30.0000 \text{ g}, \\ \text{calibration temperature} &= 23.0°\text{C}, \\ \rho\,(\mathrm{H_2O},\, 23.0°\text{C}) &= 0.997535 \text{ g cm}^{-3}, \\ \alpha_l &= 32.5 \times 10^{-7} \text{ K}^{-1}, \end{aligned}$$

weighing conditions:

$$\begin{aligned} \rho\,(\text{air}^3) &= 0.0012 \text{ g cm}^{-3}, \\ \rho\,(\text{weights}) &= 8.0 \text{ g cm}^{-3}. \end{aligned}$$

6.3.2 Correct weight of water to mass:

$$\begin{aligned} m(\mathrm{H_2O}) &= 30.0000 \times \frac{1 - 0.0012/8.0}{1 - 0.0012/0.997541} \\ &= 30.0316 \text{ g}\,. \end{aligned}$$

6.3.3 Compute volume of water delivered at the calibration temperature of 23.0°C:

$$\begin{aligned} V(23.0°\text{C}) &= 30.0316/0.997535 \\ &= 30.1058 \text{ cm}^3. \end{aligned}$$

6.3.4 Compute volume that would be dispensed at the standard temperature of 20.0°C, *i.e.*, the standard calibrated volume:

$$\begin{aligned} V(20.0°\text{C}) &= 30.1058\left[1 + 3(32.5 \times 10^{-7})(20.0 - 23.0)\right] \\ &= 30.105 \text{ cm}^3. \end{aligned}$$

[3] This value is appropriate to measurements of moderate accuracy made at sea level pressure (1 atm) and at normal laboratory temperatures (~ 20°C). For a more accurate value, see SOP 21 equation (1).

6.3.5 Compute volume that is dispensed at 25°C.

$$V(25.0°\text{C}) = 30.1049\left[1 + 3(32.5 \times 10^{-7})(25.0 - 20.0)\right]$$
$$= 30.106\ \text{cm}^3.$$

7. Quality assurance

To ensure that the volume dispensed is in control, the amount dispensed should be measured regularly and a property control chart maintained of the volume corrected to 20°C (see SOP 22).

8. Bibliography

Jones, F.E. and Harris, G.L. 1992. ITS-90 density of water formulation for volumetric standards calibration. *J. Res. Natl. Inst. Stand. Technol.* **97**: 335–340.

SOP 13

Gravimetric calibration of volume contained using water

1. Scope and field of application

This procedure describes how to calibrate the volume of solution contained by a volumetric flask or other container capable of being filled to a reproducible mark. This is expressed as the volume contained at a standard temperature (20.0°C). This procedure is capable of achieving a reproducibility of better than 0.01% (1 relative standard deviation).

2. Principle

The mass of water contained by the flask at a measured calibration temperature is used to compute the volume of water contained at that temperature. The volume that would be contained at the standard temperature (20°C) can be calculated by taking account of the volumetric expansion of the flask. The volume of liquid contained at any desired temperature can be calculated in a similar fashion.

3. Apparatus

- Analytical balance capable of weighing the quantity of water contained with a sensitivity of 1 part in 10^5 while having the capacity to weigh the water together with the container being calibrated,
- Thermometer accurate to ± 0.1°C.

4. Reagents

- Deionized water.

5. Procedure

5.1 Weigh the clean dry empty container together with the associated closure.

5.2 Fill the container being calibrated to the mark with deionized water, allowing the temperature of the container and contained water to reach an equilibrium value. Note this temperature.

5.3 Close the container and reweigh it.

6. Calculation and expression of results

6.1 Volume of the water contained at the calibration temperature

Compute the weight of the water contained from the difference between weights of the filled and empty container:

$$w(\mathrm{H_2O}) = w(\text{filled container}) - w(\text{empty container}) . \quad (1)$$

Compute the mass of water contained, correcting for air buoyancy (see SOP 21):

$$m(\mathrm{H_2O}) = w(\mathrm{H_2O}) \left(\frac{1 - \rho(\text{air})/\rho(\text{weights})}{1 - \rho(\text{air})/\rho(\text{sample})} \right). \quad (2)$$

The volume contained at the noted temperature (t) is

$$V(t) = m(\mathrm{H_2O}) / \rho(\mathrm{H_2O},\ t) . \quad (3)$$

The density of air-saturated water in the temperature range 5 to 40°C is given by the expression (Jones and Harris, 1992)

$$\begin{aligned} \rho_{\mathrm{W}} / (\mathrm{kg\ m^{-3}}) = {} & 999.84847 + 6.337563 \times 10^{-2} (t/°\mathrm{C}) \\ & - 8.523829 \times 10^{-3} (t/°\mathrm{C})^2 + 6.943248 \times 10^{-5} (t/°\mathrm{C})^3 \\ & - 3.821216 \times 10^{-7} (t/°\mathrm{C})^4 \end{aligned} \quad (4)$$

where t is the temperature on ITS 90[1]. To achieve an accuracy of 1 part in 10^4, t must be known to within 0.5°C.

6.2 Volume that would be contained at an alternate temperature

To convert the volume contained at one temperature (t_1) to a standard or alternate temperature (t_2), we need to take account of the thermal expansion of the container being used. For Pyrex-like glasses (Corning 7740, Kimble KG-33, Schott Duran, Wheaton 200, *etc.*) the coefficient of linear expansion α_l is $32.5 \times 10^{-7}\ \mathrm{K^{-1}}$; for glasses such as Kimble KG-35, α_l is about $55 \times 10^{-7}\ \mathrm{K^{-1}}$.

The coefficient of volumetric expansion,

$$\alpha_V = (1 + \alpha_l)^3 - 1 \approx 3\alpha_l , \quad (5)$$

is used to calculate the corrected volume at the alternate temperature,

$$V(t_2) = V(t_1)\left[1 + \alpha_V (t_2 - t_1)\right] . \quad (6)$$

This correction is negligible for all except the most precise work; unless $t_2 - t_1$ exceeds 10°C or if plastic ware is used.

---

[1] The International Practical Temperature Scale of 1968 (IPTS 68) has been superceded by the International Temperature Scale of 1990 (ITS 90). A simple equation can be used to relate the two over the oceanographic temperature range 0 to 40°C (Jones and Harris, 1992):

$$t_{90} = 0.0002 + 0.99975\ t_{68}.$$

The small difference in temperature scales is typically not important to the calibration of glassware for the procedures in this Guide.

6.3 Example calculation

6.3.1 The following data were used for this calculation:

$$\begin{aligned} w(\mathrm{H_2O}) &= 996.55\ \mathrm{g}, \\ \text{calibration temperature} &= 23.0°\mathrm{C}, \\ \rho\,(\mathrm{H_2O},\ 23.0°\mathrm{C}) &= 0.997535\ \mathrm{g\ cm^{-3}}, \\ \alpha_l &= 32.5 \times 10^{-7}\ \mathrm{K^{-1}}, \end{aligned}$$

weighing conditions:

$$\begin{aligned} \rho\,(\text{air}) &= 0.0012\ \mathrm{g\ cm^{-3}},^{2} \\ \rho\,(\text{weights}) &= 8.0\ \mathrm{g\ cm^{-3}}. \end{aligned}$$

6.3.2 Correct weight of water to mass:

$$\begin{aligned} m(\mathrm{H_2O}) &= 996.55 \times \frac{1 - 0.0012/8.0}{1 - 0.0012/0.997535} \\ &= 997.60\ \mathrm{g}\,. \end{aligned}$$

6.3.3 Compute volume of water contained at the calibration temperature of 23.0°C:

$$\begin{aligned} V(23.0\ °\mathrm{C}) &= 997.60/0.997535 \\ &= 1000.07\ \mathrm{cm^3}\,. \end{aligned}$$

6.3.4 Compute volume that would be contained at the standard temperature of 20.0°C, *i.e.*, the standard calibrated volume:

$$\begin{aligned} V(20.0\ °\mathrm{C}) &= 1000.07\left[1 + 3(32.5 \times 10^{-7})(20.0 - 23.0)\right] \\ &= 1000.04\ \mathrm{cm^3}\,. \end{aligned}$$

6.3.5 Compute volume that would be contained at 25°C.

$$\begin{aligned} V(25.0\ °\mathrm{C}) &= 1000.04\left[1 + 3(32.5 \times 10^{-7})(25.0 - 20.0)\right] \\ &= 1000.09\ \mathrm{cm^3}\,. \end{aligned}$$

7. Quality assurance

To ensure that the volume contained is in control, the amount contained should be measured regularly and a property control chart maintained of the volume corrected to 20°C (see SOP 22).

8. Bibliography

Jones, F.E. and Harris, G.L. 1992. ITS-90 density of water formulation for volumetric standards calibration. *J. Res. Natl. Inst. Stand. Technol.* **97**: 335–340.

[2] This value is appropriate to measurements of moderate accuracy made at sea level pressure (1 atm) and at normal laboratory temperatures (~ 20°C). For a more accurate value see SOP 21, Equation (1).

SOP 14

Procedure for preparing sodium carbonate solutions for the calibration of coulometric C_T measurements

1. Scope and field of application

This procedure describes the preparation of a set of aqueous sodium carbonate solutions which are to be used for the calibration of the determination of total dissolved inorganic carbon by extraction/coulometry. Such solutions provide an alternative to the use of gas loops for the calibration of this apparatus.

2. Principle

Six different standard solutions are prepared which contain carefully weighed amounts of pure sodium carbonate, such that the concentrations are at approximately 500 μmol dm^{-3} intervals from 0–2500 μmol dm^{-3}. Care is taken during the preparation and use of these solutions to minimize contamination by atmospheric carbon dioxide.

3. Apparatus

- 6×1 dm^3 calibrated volumetric flasks (SOP 13),
- Balance capable of weighing the sodium carbonate to $\pm$ 1 μg.

4. Reagents

- High purity sodium carbonate, > 99.95% (If you wish to prepare high purity sodium carbonate yourself, follow the procedure given in IUPAC, 1969.),
- Deionized water (If desired, carbon dioxide can be removed by boiling and allowing to cool in a stream of nitrogen.),
- Cylinder of N_2 gas.

5. Procedure

5.1 Preparation of solutions

Dry the sodium carbonate to constant weight in an oven at 280°C for > 2 hours and store it in a desiccator over phosphorus pentoxide until it is used.

The following procedure is carried out for each solution prepared:

- Weigh out the necessary amount of salt in a small container, such as a plastic vial, which has been treated to reduce static charge (*e.g.*, with an anti-static strip).
- Flush the clean dry flask with nitrogen for 5 minutes.
- Fill the flask ¾ full with deionized water, filling from the bottom of the flask through a piece of tubing.
- Using a funnel, transfer the sodium carbonate from the vial to the flask. Rinse the vial and the funnel into the flask to ensure quantitative transfer of the sodium carbonate into the flask.
- Adjust the volume of solution contained in the flask to the calibration mark.
- Make sure that the headspace is filled with nitrogen gas and then close the flask with a lightly greased stopper. Once it is closed, shake it gently to dissolve all the sodium carbonate and to mix the solution.

These solutions will last for at least 1 week, provided that the headspace is kept filled with nitrogen and that the flasks are resealed after each use.

5.2 Calculation of concentrations of solutions

First correct the weight of Na_2CO_3 for air buoyancy effects (SOP 21):

$$m(\mathrm{Na_2CO_3}) = w(\mathrm{Na_2CO_3})\left(\frac{1-\rho(\mathrm{air})/\rho(\mathrm{weights})}{1-\rho(\mathrm{air})/\rho(\mathrm{Na_2CO_3})}\right). \qquad (1)$$

Then combine this with information on the calibrated volume of the flask, V(flask) (SOP 13) and on the purity of the sodium carbonate (if known):

$$\frac{c(\mathrm{Na_2CO_3})}{\mathrm{mol\ dm^{-3}}} = \frac{m(\mathrm{Na_2CO_3})/\mathrm{g}}{105.988}\cdot\frac{1}{V(\mathrm{flask})/\mathrm{dm^3}}\cdot\mathrm{purity}. \qquad (2)$$

5.3 Example calculation

$w(\mathrm{Na_2CO_3})$ = 0.21230 g,
V(flask) = 1.0001 $\mathrm{dm^3}$,
ρ(weights) = 8.0 g $\mathrm{cm^{-3}}$,
$\rho(\mathrm{Na_2CO_3})$ = 2.532 g $\mathrm{cm^{-3}}$,
purity of Na_2CO_3 = 99.95%.

Thus

$$m(\mathrm{Na_2CO_3}) = 0.21230\left(\frac{1-0.0012/8.0}{1-0.0012/2.532}\right)$$
$$= 0.21237\ \mathrm{g}$$

and

$$c(\mathrm{Na_2CO_3}) = \frac{0.21237}{105.988}\cdot\frac{1}{1.0001}\cdot 0.9995$$
$$= 2002.5\ \mu\mathrm{mol\ dm^{-3}}.$$

6. Quality assurance

The set of six calibration standards are used in a linear regression procedure (SOP 23) to calibrate the extraction/coulometric system for measurement of total dissolved inorganic carbon. If the relative standard error of the slope obtained is too high (> 0.15%), the data should be examined to ascertain the source of error. If necessary, additional standard solutions should be prepared. Furthermore, if the value of the intercept—the background level of carbon dioxide in the deionized water—is too high (> 15 μmol dm^{-3}), the solutions should be rejected and made again with freshly boiled deionized water.

7. Bibliography

IUPAC. 1969. Sodium carbonate and sulphamic acid as acid-base primary standards. *Pure Appl. Chem.* **18**: 445–455.

SOP 21

Applying air buoyancy corrections

1. Scope and field of application

The effect of air buoyancy is, if uncorrected, frequently the largest source of error in mass measurements. This procedure provides equations to be used to correct for the buoyant effect of air. An air buoyancy correction should be made in all high accuracy mass determinations.

2. Principle

The upthrust due to air buoyancy acts both on the sample being weighed and on the counter-balancing weights. If these are of different densities and hence of different volumes, it will be necessary to allow for the resulting difference in air buoyancy to obtain an accurate determination of mass.

3. Requirements

3.1 Knowledge of the air density at the time of weighing

For the most accurate measurements, the air density is computed from a knowledge of pressure, temperature, and relative humidity. Tolerances for the various measurements are given in Table 1.

Table 1 Tolerances for various physical parameters.

Variable	Uncertainty in computed air density	
	± 0.1%	**± 1.0%**
Relative humidity (%)	± 11.3%	–
Air temperature (°C)	± 0.29 K	± 2.9 K
Air pressure (kPa)	± 0.10 kPa	± 1.0 kPa

- Barometer accurate to ± 0.05 kPa,
- Thermometer accurate to ± 0.1°C,
- Hygrometer accurate to 10%.

An error of 1% in air density results in an error of approximately 1 part in 10^5 in the mass corrected for air buoyancy. Although meteorological variability can result in variations of up to 3% in air density, the change of pressure (and hence of air density) with altitude can be much more significant. For measurements of moderate accuracy, made at sea level and at normal laboratory temperatures, an air density of 0.0012 g cm^{-3} is often adequate.

3.2 Knowledge of the apparent mass scale used to calibrate the balance

There are two apparent mass scales in common use. The older one is based on the use of brass weights adjusted to a density of 8.4 g cm^{-3}, the more recent one on the use of stainless steel weights adjusted to a density[1] of 8.0 g cm^{-3}.

3.3 Knowledge of the density of the sample

The density of the sample being weighed is needed for this calculation.

4. Procedure

4.1 Computation of air density

The density of air in g cm^{-3} can be computed from measurements of pressure, temperature, and relative humidity (Jones, 1978):

$$\rho(\text{air}) = \frac{3.4848\,(p - 0.0037960U \cdot e_S)}{273.15 + t} \times 10^{-3} \qquad (1)$$

where

p = air pressure (kPa),
U = relative humidity (%),
t = temperature (°C),
e_S = saturation vapor pressure (kPa),

$$e_S = 1.7526 \times 10^8 \exp\left[-5315.56/(t + 273.15)\right]. \qquad (2)$$

4.2 Computation of mass from weight

The mass, m, of a sample of weight, w, and density, ρ(sample), is computed from the expression

[1] Strictly, these densities apply only at 20°C. The conversion factor from the "apparent mass" obtained by using these values to "true" mass is defined by the expression

$$Q = \frac{\rho(\text{weights})(D_{20} - 0.0012)}{D_{20}[\rho(\text{weights}) - 0.0012]}$$

where D_{20} is the apparent mass scale to which the weights are adjusted. This factor may be considered as unity for most purposes.

$$m = w\left(\frac{1-\rho(\text{air})/\rho(\text{weights})}{1-\rho(\text{air})/\rho(\text{sample})}\right) \quad (3)$$

(see Annexe for the derivation).

5. Example calculation

The following data were used for this calculation[2]:

$$\begin{aligned} \text{weight of sample, } w &= 100.00000 \text{ g}, \\ \text{density of sample, } \rho\,(\text{sample}) &= 1.0000 \text{ g cm}^{-3}. \end{aligned}$$

Weighing conditions:

$$\begin{aligned} p &= 101.325 \text{ kPa (1 atm)}, \\ U &= 30.0\%, \\ t &= 20.00°\text{C}, \\ \rho\,(\text{weights}) &= 8.0000 \text{ g cm}^{-3}. \end{aligned}$$

5.1 Computation of air density

$$\begin{aligned} e_S &= 2.338 \text{ kPa}, \\ \rho\,(\text{air}) &= 0.0012013 \text{ g cm}^{-3}. \end{aligned}$$

5.2 Computation of mass

$$m = 100.10524 \text{ g}.$$

6. Bibliography

Dean, J.A. 1985. Lange's Handbook of Chemistry. McGraw-Hill Book Company, New York, 1792 pp.

Jones, F.E. 1978. The air density equation and the transfer of the mass unit. *J. Res. Natl. Bureau Stand.* **83**: 419–428.

Schoonover, R.M. and Jones, F.E. 1981. Air buoyancy correction in high-accuracy weighing on analytical balances. *Anal. Chem.* **53**: 900–902.

Taylor, J.K. and Oppermann, H.V. 1986. Handbook for the quality assurance of metrological measurements. National Bureau of Standards Handbook 145.

Woodward, C. and Redman, H.N. 1973. High-precision Titrimetry. The Society for Analytical Chemistry, London, 63 pp.

[2] The seemingly excessive number of decimal places is provided here so that users of this procedure can check their computation scheme.

Annexe

Derivation of the expression for buoyancy correction

An expression for the buoyancy correction can be derived from a consideration of the forces shown in Figure 1. Although the majority of balances nowadays are single-pan, the principles remain the same, the difference being that the forces are compared sequentially using a force sensor rather than simultaneously using a lever. At balance, the opposing forces are equal:

$$m_1 g - V_1 \rho(\text{air}) g = m_2 g - V_2 \rho(\text{air}) g \tag{4}$$

where g is the acceleration due to gravity and $\rho(\text{air})$ is the density of the air at the temperature, pressure, and humidity of the weighing operation. Note that m_2 is the "weight" of a sample whose true mass is m_1.

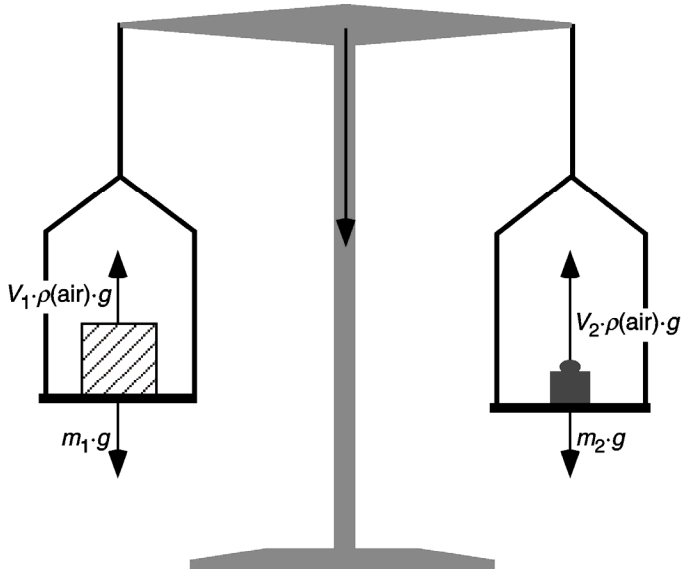

Fig. 1 Forces on sample (1) and weights (2) when weighing in air.

As

$$V = m/\rho\,, \tag{5}$$

we can rewrite equation (4) as

$$m_1 - m_1 \rho(\text{air})/\rho_1 = m_2 - m_2 \rho(\text{air})/\rho_2\,. \tag{6}$$

This equation can be rearranged to obtain the expression

$$m_1 = m_2 \frac{1 - \rho(\text{air})/\rho_2}{1 - \rho(\text{air})/\rho_1}. \tag{7}$$

Equation (7) is the basis of the expression used for air buoyancy correction (Schoonover and Jones, 1981; Taylor and Oppermann, 1986):

$$m = w \frac{1 - \rho(\text{air})/\rho(\text{weights})}{1 - \rho(\text{air})/\rho(\text{sample})} \tag{8}$$

where w is the "weight" of the sample in air and m is the true mass.

Equation (6) can also be rearranged to give

$$m_1 = m_2 + m_2 \rho(\text{air}) \left(\frac{m_1}{m_2} \frac{1}{\rho_1} - \frac{1}{\rho_2} \right). \tag{9}$$

As $m_1 \approx m_2$, equation (9) is almost identical to the commonly quoted expression for buoyancy correction,

$$m = w + w\rho(\text{air}) \left[\frac{1}{\rho(\text{sample})} - \frac{1}{\rho(\text{weights})} \right] \tag{10}$$

(Woodward and Redman, 1973; Dean, 1985). An approximate value of 0.0012 g cm^{-3} for $\rho(\text{air})$ is often used with this expression; this is appropriate to measurements of moderate accuracy made at sea level pressures and at normal laboratory temperatures.

SOP 22

Preparation of control charts

1. Scope and field of application

This procedure details the preparation and use of property ($\bar{X}$) and range (R) control charts. The $\bar{X}$ chart is used to demonstrate whether a measurement mean is in control; the R chart is used to demonstrate whether measurement variability is in control. Such charts are basic tools for the quality assurance of analytical measurements. They can be used to document measurement uncertainty and to monitor a variety of aspects of a measurement process, such as blank levels or instrument sensitivity.

2. Principle

The construction of a control chart is based on statistical principles, specifically on the normal distribution. The control limits are based on considerations of probability; thus decisions that a system is in control are supported. Similarly, the control limits can be used to warn of potential problems and reveal the need for corrective action. Control charts should be kept in real time so that such corrective action is taken promptly.

3. Procedure

3.1 Statistical calculations

SOP 23 of this Guide provides all the necessary information to carry out the statistical calculations needed in this SOP.

3.2 The $\bar{X}$ chart

Values obtained for repetitive measurements of a control sample are plotted sequentially to evaluate the stability of the measurement process (see Figure 1). Such control samples must be very similar to the test samples of interest, otherwise it is not possible to draw conclusions about the performance of the system on test samples from this information.

The results from at least 12 measurements—with never more than one measurement made on the same day—are used to compute estimates of the mean and standard deviation of the data in accordance with the standard expressions (SOP 23).

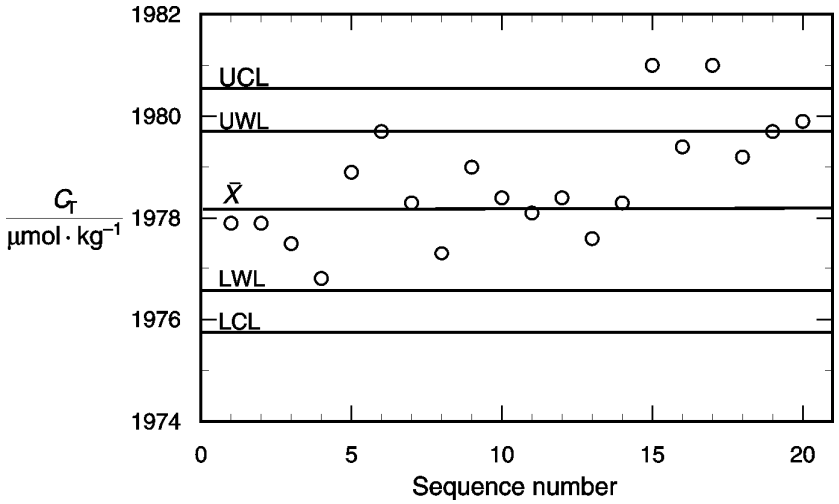

Fig. 1 Example of a property control chart showing a trend in the data with time; control limits were calculated from the first 12 points. This chart indicates that the measurement process is not in control.

The central line is the mean value, $\bar{x}$, the control limits are based on the sample standard deviation, s:

$$\begin{aligned} &\text{upper control limit} && \text{UCL} = \bar{x} + 3\,s, \\ &\text{upper warning limit} && \text{UWL} = \bar{x} + 2\,s, \\ &\text{lower warning limit} && \text{LWL} = \bar{x} - 2\,s, \\ &\text{lower control limit} && \text{LCL} = \bar{x} - 3\,s. \end{aligned}$$

When so set, approximately 95% of the plotted points should fall between the warning limits (UWL and LWL) and rarely should any fall outside the control limits (UCL and LCL).

3.3 The R chart

The absolute differences (R) of duplicate measurements are plotted sequentially to evaluate the precision of the measurement process (see Figure 2). The average range $\bar{R}$ is related to the short-term standard deviation (or repeatability, s_R) of the measurement process (SOP 23). At least 12 measurements should be used to compute $\bar{R}$. The control limits for duplicate measurements are:

$$\begin{aligned} \text{UCL} &= 3.267\ \bar{R}, \\ \text{UWL} &= 2.512\ \bar{R}, \\ \text{LWL} &= 0, \\ \text{LCL} &= 0. \end{aligned}$$

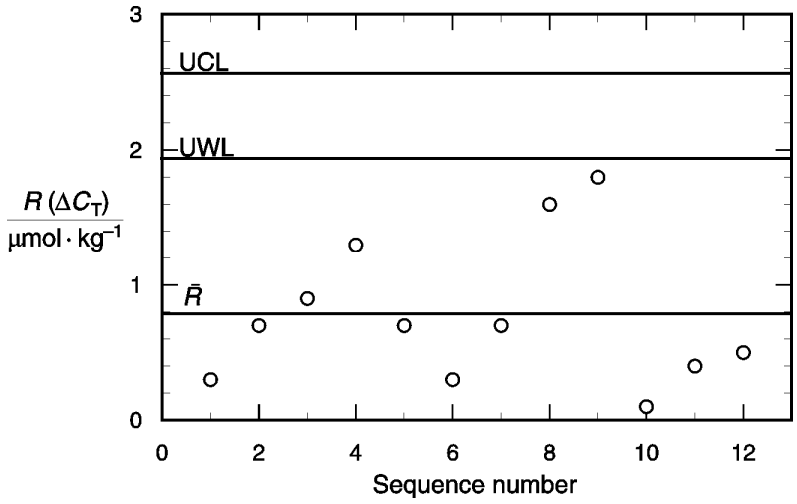

Fig. 2 Example of a range control chart; control limits were calculated using all the data shown. The measurement precision is in control.

3.4 Updating control charts

After additional control data have been accumulated—at least as much as was used originally—the control limits may be updated. A *t* test is made to assess whether $\bar{x}$ for the second set of data is significantly different from that for the first (SOP 23). If not, all the data may be used to compute a new estimate of $\bar{x}$, otherwise only the second set of data should be used to revise the control chart.

The value of the sample standard deviation, *s*, should also be calculated for the second set of data. It should be compared with the estimate from the first set of data, using the *F* test (SOP 23) to decide whether to pool it with the first, or use it separately in setting new control limits.

If the values of *R* show no significant trends and if $\bar{R}$ has not changed significantly, all of the values of *R* should be combined to obtain an updated estimate of $\bar{R}$ from which updated control limits can be computed. Judgement of the significance of changes in $\bar{R}$ is best decided by computing the corresponding values of the short-term standard deviation (the repeatability) and conducting an *F* test.

3.5 Interpretation of control chart data

Points plotted on a control chart should be randomly distributed within the warning limits when the system is in a state of statistical control. If a plotted point lies outside of the warning limits, a second set of measurements should be made. If this point also lies outside the warning limits, corrective action is required and demonstrated attainment of control is necessary before measurements may be reported with confidence. Barring blunders, one point outside of the control limits is reason for corrective action. The nature of the corrective action to be taken will depend, in either case, on the kind of measurement made. If the *X* point is outside the limits but the *R* point is not, a source of bias should be sought and eliminated. If the *R* point is outside of limits, *X* probably will be as well. Sources of

extraordinary random error should be sought and eliminated before any possible bias can be detected.

Control charts may be used to evaluate the uncertainty of measurement in some cases. When an appropriate control chart is maintained, a $\bar{X}$ chart may be used to evaluate bias and to document the standard deviation of the measurement process. Then the values of s on which the control limits are based may be used in calculating confidence limits for measurement values.

4. Bibliography

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SOP 23

Statistical techniques used in quality assessment

1. Scope and field of application

This procedure describes various statistical calculations used in quality assessment. Calculations are detailed which allow the computation of the mean and standard deviation of a set of values, the computation of a standard deviation from a set of duplicate measurements, the computation of the confidence interval for a mean, the examination of the values of two means or of two standard deviations to assess if they are significantly different at some chosen level of probability, and the computation of the least-squares estimates of the slope and intercept of a straight line.

2. Principle

These calculations are based on statistical principles, specifically on the normal distribution. More details of the relevant statistical background are given in the bibliography.

3. Procedure

3.1 Estimation of the mean and standard deviation from a series of measurements

Given n measurements,

$$x_1, x_2, x_3, \ldots, x_n,$$

the mean, $\bar{x}$, is given by

$$\bar{x} = \frac{1}{n}\sum_{i=1}^{n} x_i \qquad (1)$$

and an estimate of the standard deviation, s, is given by

$$s = \left(\frac{\sum_{i=1}^{n} (x_i - \bar{x})^2}{n-1} \right)^{1/2} . \qquad (2)$$

3.2 Estimation of the standard deviation from the difference of sets of duplicate measurements

Given k differences of duplicate measurements,

$$d_1, d_2, d_3, \ldots, d_k ,$$

an estimate of the standard deviation, s, is given by

$$s_R = \left(\frac{\sum_{i=1}^{k} d_i^2}{2k} \right)^{1/2} . \qquad (3)$$

This is a measure of the short-term standard deviation, or repeatability of measurements[1].

3.3 Confidence interval for a mean

The formula for use is

$$\bar{x} \pm \frac{ts}{\sqrt{n}} \qquad (4)$$

where

$\bar{x}$ = sample mean,
n = number of measurements on which the mean is based,
s = estimate of the standard deviation[2],
t = Student's t value, *i.e.*, the probability factor for the desired confidence limit and the number of degrees of freedom associated with s. (For numerical values, see Table 1 in the Annexe to this procedure.)

3.4 Comparing values of two means

Case 1. No reason to believe that the standard deviations differ.

Step 1: Choose α, the desired probability level (*i.e.*, the significance level) of the test.

Step 2: Calculate a pooled standard deviation from the two estimates to obtain a better estimate of the standard deviation:

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[1] The International Organization for Standardization (ISO) applies two descriptions of precision: (1) the *reproducibility*, the closeness of agreement between individual results obtained with the same method but under different conditions (*e.g.*, in different laboratories) and (2) the *repeatability*, the closeness of agreement between successive results obtained with the same method and under the same conditions.

[2] If $\bar{x}$ and s are based on the same data set, the number of degrees of freedom, df = n – 1. However, if s is based on additional evidence, such as a system under statistical control (judged by a control chart), then the degrees of freedom on which the estimate of s is based may be used to determine t. In such a case, one can calculate a confidence interval for even a single measurement.

$$s_{\mathrm{p}} = \left(\frac{\nu_{\mathrm{A}} s_{\mathrm{A}}^2 + \nu_{\mathrm{B}} s_{\mathrm{B}}^2}{\nu_{\mathrm{A}} + \nu_{\mathrm{B}}} \right)^{1/2} \tag{5}$$

where ν_{A} and ν_{B} are the number of degrees of freedom associated with s_{A} and s_{B}, respectively. s_{p} will thus be based on $\nu_{\mathrm{A}} + \nu_{\mathrm{B}}$ degrees of freedom.

Step 3: Calculate the uncertainty, U, of the differences

$$U = t s_{\mathrm{p}} \left(\frac{1}{n_{\mathrm{A}}} + \frac{1}{n_{\mathrm{B}}} \right)^{1/2} \tag{6}$$

where t is the appropriate Student's t value.

Step 4: Compare $\Delta = \left| \bar{x}_{\mathrm{A}} - \bar{x}_{\mathrm{B}} \right|$ with U. If $\Delta \leq U$, there is no reason to believe that the means disagree.

Case 2. The standard deviations differ significantly (see section 3.5).

Step 1: Choose α, the significance level of the test.

Step 2: Compute the estimated variance of each mean using the individual estimates of the standard deviations,

$$V_{\mathrm{A}} = s_{\mathrm{A}}^2 / n_{\mathrm{A}}, \qquad V_{\mathrm{B}} = s_{\mathrm{B}}^2 / n_{\mathrm{B}} \,. \tag{7}$$

Step 3: Compute the effective number of degrees of freedom[3] :

$$f^* = \frac{\left(V_{\mathrm{A}} + V_{\mathrm{B}} \right)^2}{\dfrac{V_{\mathrm{A}}^2}{n_{\mathrm{A}} + 1} + \dfrac{V_{\mathrm{B}}^2}{n_{\mathrm{B}} + 1}} - 2 \,. \tag{8}$$

Step 4: Calculate the uncertainty, U, of the differences

$$U = t^* \sqrt{V_{\mathrm{A}} + V_{\mathrm{B}}} \tag{9}$$

where t^* is the effective value of t based on f^* degrees of freedom and the chosen significance level, α (Table 1 in the Annexe).

Step 5: Compare $\Delta = \left| \bar{x}_{\mathrm{A}} - \bar{x}_{\mathrm{A}} \right|$ with U. If $\Delta \leq U$, there is no reason to believe that the means disagree.

3.5 Comparing estimates of a standard deviation (*F* test)

This test may be used to decide whether there is sufficient reason to believe that two estimates of a standard deviation are significantly different. It consists of

[3] A number of expressions exist in the literature for this calculation, with some authors even arguing that such a pooling of the variances is inappropriate. The expression used here comes from Taylor (1987).

calculating the ratio of the variances and comparing it with tabulated values. Unless the computed ratio is larger than the tabulated value, there is no reason to believe that the respective standard deviations are significantly different.

The F ratio is calculated as

$$F = \frac{s_L^2}{s_S^2} \tag{10}$$

where s_L is the larger value and s_S is the smaller of the two estimates under consideration. The critical value of F will depend on the significance level chosen and on the degrees of freedom associated with s_L and s_S (see Table 2 in the Annexe).

3.6 Computation of least-squares estimates

For the linear model,

$$y_i = \beta_0 + \beta_1 x_i + \varepsilon_i \tag{11}$$

where x is essentially without error (for data with errors in x and y—see York, 1966) and the error ε_i is normally distributed with a constant variance, least-squares estimates of the coefficients, β_0 and β_1, are given by the expressions

$$\beta_1 = \frac{\sum_i (x_i - \bar{x})(y_i - \bar{y})}{\sum_i (x_i - \bar{x})^2}, \tag{12}$$

$$\beta_0 = \bar{y} - \beta_1 \bar{x} . \tag{13}$$

An estimate of the experimental error variance is then given by

$$s^2 = \frac{\sum_i (y_i - \beta_0 - \beta_1 x_i)^2}{n - 2} \tag{14}$$

and estimates of the standard errors of the coefficients by

$$\text{S.E.}(\beta_0) = s\left(\frac{1}{n} + \frac{\bar{x}^2}{\sum_i (x_i - \bar{x})^2}\right)^{1/2}, \tag{15}$$

$$\text{S.E.}(\beta_1) = \frac{s}{\left(\sum_i (x_i - \bar{x})^2\right)^{1/2}} . \tag{16}$$

4. Example calculations

4.1 Estimation of the mean and standard deviation from a series of measurements

Given the following 9 measurements:

1977.67, 1977.98, 1977.29, 1978.60, 1979.48,
1979.14, 1979.33, 1979.95, 1979.99,

the mean is 1978.83 and the standard deviation is 0.99.

4.2 Estimation of the standard deviation from the difference of sets of duplicate measurements

Given 10 pairs of measurements:

1976.8, 1979.3, 1978.9, 1979.6, 1979.6, 1979.8
1978.3, 1978.6, 1981.2, 1979.8, 1977.6, 1977.8
1976.2, 1976.8, 1978.6, 1977.0, 1976.6, 1978.9
1978.3, 1978.9,

the standard deviation calculated using

$$s_R = \left(\frac{\sum_{i=1} d_i^2}{2k} \right)^{1/2}$$

is 0.93.

4.3 Confidence interval for a mean

The 95% confidence interval for the mean calculated in section 4.1 is

$$1978.83 \pm \frac{(2.306)(0.99)}{\sqrt{9}} = 1978.83 \pm 0.76$$

4.4 Comparing values for two means

Case 1. No reason to believe that the standard deviations differ.

$$\overline{x}_A = 1978.78, \quad s_A = 0.93, \quad n_A = 9$$
$$\overline{x}_B = 1981.74, \quad s_B = 0.87, \quad n_B = 18$$

Step 1: Require 95% confidence in decision.

Step 2: Pooled standard deviation:

$$s_{\mathrm{p}} = \left(\frac{8(0.93)^2 + 17(0.87)^2}{8+17} \right)^{1/2}$$
$$= 0.89.$$

Step 3: Calculate U:

$$U = 2.060(0.89)\left(\frac{1}{9} + \frac{1}{18} \right)^{1/2}$$
$$= 0.75.$$

Step 4: As Δ (= 1981.74 – 1978.78 = 2.96) is larger than U, the means disagree at the 95% confidence level.

Case 2. The standard deviations differ significantly.

$$\bar{x}_{\mathrm{A}} = 1978.78, \quad s_{\mathrm{A}} = 0.93, \quad n_{\mathrm{A}} = 9$$
$$\bar{x}_{\mathrm{B}} = 1981.74, \quad s_{\mathrm{B}} = 2.75, \quad n_{\mathrm{B}} = 16$$

Step 1: Require 95% confidence in decision.

Step 2: Compute the estimated variance of each mean:

$$V_{\mathrm{A}} = (0.93)^2 / 9 = 0.0961$$
$$V_{\mathrm{B}} = (2.75)^2 / 16 = 0.4727.$$

Step 3: Compute the effective number of degrees of freedom:

$$f^* = \left[\frac{(0.0961 + 0.4727)^2}{(0.0961)^2/(9+1) + (0.4727)^2/(16+1)} \right] - 2 \approx 21.$$

Step 4: Calculate U:

$$U = 2.08(0.0961 + 0.4727)^{1/2} = 1.57 .$$

Step 5: As Δ (= 1981.74 – 1978.78 = 2.96) is larger than U, the means disagree at the 95% confidence level.

4.5 Comparing estimates of a standard deviation

$$\bar{x}_{\mathrm{A}} = 1978.78, \quad s_{\mathrm{A}} = 0.93, \quad n_{\mathrm{A}} = 9$$
$$\bar{x}_{\mathrm{B}} = 1975.35, \quad s_{\mathrm{B}} = 1.71, \quad n_{\mathrm{B}} = 12$$

Calculate F:

$$F = \frac{(1.71)^2}{(0.93)^2} = 3.38 .$$

The tabulated value of F—with 8 degrees of freedom in the numerator and 11 degrees of freedom in the denominator—is 3.7. As the computed value is smaller than the tabulated value, there is no reason to believe that the two standard deviations are significantly different.

4.6 Computation of least-squares estimates

Given 6 pairs of measurements of x and y:

0.0	1892
498.8	66537
1001.9	130818
1500.8	195216
2002.5	260068
2497.1	323456

Linear regression gives

$$\beta_0 = 2017.77,$$
$$\beta_1 = 128.765.$$

The error estimates are

$$s = 221.77,$$
$$\text{S.E.}(\beta_0) = 160.55,$$
$$\text{S.E.}(\beta_1) = 0.106.$$

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Annexe

Table 1 Student's *t* values for 95% and 99% confidence intervals.

Probability level for two-sided confidence interval		
df[4]	**95%**	**99%**
1	12.706	63.657
2	4.303	9.925
3	3.182	5.841
4	2.776	4.604
5	2.571	4.032
6	2.447	3.707
7	2.365	3.499
8	2.306	3.355
9	2.262	3.250
10	2.228	3.169
11	2.201	3.106
12	2.179	3.055
13	2.160	3.012
14	2.145	2.977
15	2.131	2.947
16	2.120	2.921
17	2.110	2.898
18	2.101	2.878
19	2.093	2.861
20	2.086	2.845
25	2.060	2.787
40	2.021	2.704
60	2.000	2.660
∞	1.960	2.576

[4] degrees of freedom ($n - 1$)

Table 2 Critical values for the *F* test for use in a two-tailed test of equality of standard deviation at 95% level of confidence.

df_D	df_N									
	1	2	4	6	8	10	15	20	30	40
1	648	800	900	937	957	969	983	993	1001	1006
2	38.5	39.0	39.2	39.3	39.4	39.4	39.4	39.4	39.5	39.5
4	12.2	10.6	9.6	9.2	9.0	8.8	8.7	8.6	8.5	8.4
6	8.8	7.3	6.2	5.8	5.6	5.5	5.3	5.2	5.1	5.0
8	7.6	6.1	5.0	4.6	4.4	4.3	4.1	4.0	3.9	3.8
10	6.9	5.5	4.5	4.1	3.8	3.7	3.5	3.4	3.3	3.3
15	6.2	4.8	3.8	3.4	3.2	3.1	2.9	2.8	2.6	2.6
20	5.9	4.5	3.5	3.1	2.9	2.8	2.6	2.5	2.4	2.3
30	5.6	4.2	3.2	2.9	2.6	2.5	2.3	2.2	2.1	2.0
40	5.4	4.0	3.1	2.7	2.5	2.4	2.2	2.1	1.9	1.9
60	5.3	3.9	3.0	2.6	2.4	2.3	2.1	1.9	1.8	1.7
120	5.2	3.8	2.9	2.5	2.3	2.2	1.9	1.8	1.7	1.6
∞	5.0	3.7	2.8	2.4	2.2	2.1	1.8	1.7	1.6	1.5

df_D — degrees of freedom of the variance in the denominator.
df_N — degrees of freedom of the variance in the numerator.

SOP 24

Calculation of the fugacity of carbon dioxide in pure carbon dioxide gas or in air

1. Scope and field of application

This procedure describes a method for the calculation of the fugacity of carbon dioxide in pure carbon dioxide gas or in air. The fugacity, $f(CO_2)$, is expressed either in Pascals or in atmospheres[1].

2. Definition

The chemical potential (μ_B) of an individual component of a vapor phase can be expressed in terms of its fugacity (f_B). This is defined by the equation

$$RT \ln f_B = \mu_B - \lim_{p \to 0} [\mu_B - RT \ln(x_B p / p^\circ)] \quad (1)$$

where x_B is the mole fraction of B in the gaseous mixture and thus $x_B p$ is the partial pressure of B (p_B) in the vapor phase and p° is a standard pressure (typically 101325 Pa, *i.e.*, 1 atm). The term

$$\lim_{p \to 0} [\mu_B - RT \ln(x_B p / p^\circ)] \quad (2)$$

is thus a standard chemical potential, $\mu_B^\circ(T)$.

3. Principle

The vapor phase fugacity of either a pure gas (x_B = 1) or of a component in a mixture of gases can be calculated from the equation

$$f_B = x_B p \exp\left(\frac{1}{RT} \int_0^p (V_B - RT/p')\, dp' \right). \quad (3)$$

[1] 1 atm = 101325 Pa.

V_B is obtained from

$$V_B = \left(\frac{\partial V}{\partial n_B} \right)_{T,p}, \tag{4}$$

where V is given by an equation of state for the vapor,

$$V = f(T, p). \tag{5}$$

3.1 The ideal gas equation

The simplest equation of state is the expression for a perfect gas mixture,

$$V = \frac{RT}{p} \sum\nolimits_B n_B . \tag{6}$$

The integral in equation (3) is then equal to zero and

$$f_B = x_B p . \tag{7}$$

3.2 The virial equation

More generally, the equation of state can be represented by a virial expression,

$$\frac{pV_B}{RT} = 1 + \frac{B(T)}{V_B} + \frac{C(T)}{V_B^2} + \ldots \tag{8}$$

This equation, truncated after the second virial coefficient, is usually adequate to represent p–V–T properties at pressures up to a few atmospheres. It also has the advantage that the coefficient, $B(T)$, can be related to the intermolecular potential energy function of the molecules concerned.

In a mixture of gases,

$$B(T) = \sum_l \sum_m x_l x_m B_{lm}(T) \tag{9}$$

where $B_{lm} = B_{ml}$. The total volume can then be written as

$$V = \sum_k n_k V_k = \sum_k n_k \frac{RT}{p} + \frac{\sum_l \sum_m n_l n_m B_{lm}(T)}{\sum_k n_k} . \tag{10}$$

The partial molar volume of an individual component is

$$V_B = \frac{RT}{p} - \frac{\sum_l \sum_m n_l n_m B_{lm}(T)}{\left(\sum_k n_k \right)^2} + \frac{2 \sum_m n_m B_{Bm}(T)}{\sum_k n_k} \tag{11}$$

and thus

$$V_{\mathrm{B}} = \frac{RT}{p} + \sum_{l}\sum_{m} x_l x_m [2B_{\mathrm{B}m}(T) - B_{lm}(T)]p \,. \tag{12}$$

The fugacity is then given by

$$f_{\mathrm{B}} = x_{\mathrm{B}} p \exp\left(\frac{\sum_{l}\sum_{m} x_l x_m \left(2B_{Bm}(T) - B_{lm}(T)\right) p}{RT} \right). \tag{13}$$

For a pure gas, this reduces to

$$f_{\mathrm{B}} = p \exp\left(\frac{B_{\mathrm{BB}}(T)\, p}{RT} \right) \tag{14}$$

where $B_{\mathrm{BB}}(T)$ is the virial coefficient for the pure gas, B.

A further particular case of equation (13) is the expression for a component of a binary mixture,

$$f_{\mathrm{B}} = x_{\mathrm{B}} p \exp\left[\left(B_{\mathrm{BB}}(T) + 2x_C^2 \delta_{\mathrm{B-C}}(T) \right) \frac{p}{RT} \right] \tag{15}$$

where

$$\delta_{\mathrm{B-C}} = B_{\mathrm{BC}} - \tfrac{1}{2}(B_{\mathrm{BB}} + B_{\mathrm{CC}}) \,. \tag{16}$$

Many of the cross-virial coefficients for the practical computation of fugacity in vapor mixtures have never been measured experimentally. However, a number of empirical approaches can be used.

The simplest of these is the Lewis and Randall rule,

$$f_{\mathrm{B}} = x_{\mathrm{B}} f_{\mathrm{B}}^{*} \tag{17}$$

where f_{B}^{*} is the fugacity of pure component, *B*, at the same temperature and total pressure as the mixture (equation 14).

An alternate method of predicting $B(T)$, based on statistical–mechanical arguments, is to use the expression

$$B(T) = 2\pi L \int_{0}^{\infty} \left[1 - \exp\left(-u(r)/kT \right) \right] r^2 \, dr \tag{18}$$

where L is the Avogadro constant and k the Bolzmann constant. Here, $u(r)$—the pair-interaction energy—is assumed to depend only on the separation, r, of the centers of mass of two molecules.

4. Calculation and expression of results

4.1 Virial coefficient of pure carbon dioxide gas

The first virial coefficient of CO_2, $B(CO_2, T)$, is given by the expression (Weiss, 1974) which is based on values reported by Levelt Sengers *et al.* (1971):

$$\frac{B(\mathrm{CO_2},T)}{\mathrm{cm^3\ mol^{-1}}} = -1636.75 + 12.0408\left(\frac{T}{\mathrm{K}}\right) - 3.27957\times10^{-2}\left(\frac{T}{\mathrm{K}}\right)^2 + 3.16528\times10^{-5}\left(\frac{T}{\mathrm{K}}\right)^3 \qquad (19)$$

where $265 < T/\mathrm{K} < 320$.

This expression can then be used in equation (14) to calculate the fugacity of pure CO_2 provided that the pressure and temperature of the CO_2 are known.

4.2 Virial coefficient of carbon dioxide in air

In addition, Weiss used the Lennard–Jones (6–12) potential to estimate $u(r)$ and hence calculate values for δ_{BC} for the binary mixture: CO_2–air. He found that the temperature dependence of this parameter is represented by the equation

$$\frac{\delta(\mathrm{CO_2-air})}{\mathrm{cm^3\ mol^{-1}}} = 57.7 - 0.118\left(\frac{T}{\mathrm{K}}\right) \qquad (20)$$

where $273 < T/\mathrm{K} < 313$.

This expression can then be used in equation (15), together with equation (19), to calculate the fugacity of CO_2 in air.

4.3 Example calculations

4.3.1 Fugacity of pure CO_2

$$T = 298.15\ \mathrm{K},$$
$$p = 101.325\ \mathrm{kPa}\ \ (1\ \mathrm{atm}).$$

Then,

$$B(\mathrm{T}) = -123.2\ \mathrm{cm^3\ mol^{-1}},$$
$$f(\mathrm{CO_2}) = 101325\exp\left(\frac{-123.2\times10^{-6}\times101325}{8.31447\times298.15}\right) = 100.816\ \mathrm{kPa}$$

or

$$f(\mathrm{CO_2}) = 100.816/101.325 = 0.99498\ \mathrm{atm}.$$

4.3.2 Fugacity of CO_2 in air

$$T = 298.15\ \text{K},$$
$$p = 101.325\ \text{kPa}\ \ (1\ \text{atm}),$$
$$x(\text{CO}_2) = 350 \times 10^{-6}.$$

Then,

$$B(T) = -123.2\ \text{cm}^3\ \text{mol}^{-1},$$
$$\delta(\text{CO}_2\text{–air}) = 22.5\ \text{cm}^3\ \text{mol}^{-1},$$
$$f(\text{CO}_2) = (350 \times 10^{-6})(101325) \times \exp\left\{\frac{\left[-123.2 \times 10^{-6} + 2(1 - 350 \times 10^{-6})^2 (22.5 \times 10^{-6})\right] \times 101325}{8.31447 \times 298.15}\right\}$$
$$= 35.35\ \text{Pa}\ \ (348.9 \times 10^{-6}\ \ \text{atm}).$$

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